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# THERMOPHYSICAL PROPERTIES OF NITROGEN TRIFLUORIDE FROM 66 TO 500 K AT PRESSURES TO 500 BAR

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Air Force Weapons Laboratory (AFSC), Kirtland Air Force Base, NM 87117 Project Order No. 79-64

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# THERMOPHYSICAL PROPERTIES OF NITROGEN TRIFLUORIDE FROM 66 TO 500 K AT PRESSURES TO 500 BAR Robert D. Goodwin and Lloyd A. Weber

Density and specific heat data for nitrogen trifluoride have been measured in the approximate ranges 90 < T < 320 K, 0.07 <  $\rho/\rho_{C}$  < 3, at pressures up to 300 bar. These include vapor pressures, some orthobaric densities away from the critical region, and specific heats in the single and two phase regions. A nonanalytic equation of state is used to tabulate thermophysical properties along isobars. The tables include: compressibility factors, densities, enthalpies, entropies, heats of vaporization, isochores, isotherms, Joule-Thomson inversion, orthobaric densities, specific heats, speeds of sound, and vapor pressures. The data also are represented by an analytic equation of state and comparisons are made between some results from the two equations.

Key Words: Compressibility factors; densities; enthalpies; entropies; equation of state; heats of vaporization; isobars; isochores; isotherms; Joule-Thomson inversion; nitrogen trifluoride; orthobaric densities; specific heats; speeds of sound; vapor pressures.

#### 1. INTRODUCTION

The purpose of this work has been to perform P-p-T and heat capacity measurements needed to develop equations of state, and then to report both the equations and tables of thermodynamic properties, including the computer programs.

The triple-point temperature was reported at 66.36 K by Pierce and Pace in 1954 [15]. In 1955 they reported vapor pressures and specific heats of the liquid up to the normal boiling point, and the heat of vaporization at the normal boiling point, (11587  $\pm$  22 J/mol) at 144.093 K, corrected for the icepoint 273.15 K, and molecular weight on the C<sup>12</sup> scale) [16]. In 1956 Jarry and Miller reported vapor pressures up to their observed critical-point at 233.9  $\pm$  0.1 K, as well as densities of the saturated liquid from 78 to 170 K [11]. Some P-p-T compressibility data were reported privately by E. A. Burns (1975) [1], and by E. M. Van der Waal and R. E. Anderson (1977) [1]. The range is 273 < T < 344 K, 21 < P < 200 atm, 0.14 <  $\rho/\rho_{C}$  < 1.48.

Thermodynamic functions for ideal gas states appeared in the JANAF Thermochemical Tables in 1969 [2]. Thermodynamic properties over the P-p-T surface were computed by Seshadri, et al. in 1970 by use of some of the above

data and a Martin-Hou equation of state in which all parameters were estimated from simple physical properties [18].

At the start of present work, apparently no experimental compressibility data existed below 273 K. There were no experimental densities for saturated liquid above 170 K in the all-important critical region, and no such densities whatsoever for the saturated vapor. No virial equation of state was found for low-density gas. No saturated liquid specific heat data existed above the normal boiling point and there were no data at all for the single-phase fluid.

The present report includes results of experimental and computational work. The PVT compressibility measurements are described in a manuscript by Goodwin [7] for the range 90 to 320 K at pressures to 300 bar. Table 5 presents a comparison of these data with the nonanalytic equation of state. Specific heat measurements, for the saturated and compressed liquid up to 300 K, are described in a manuscript by Weber [22].

In the following we at first give a full description of development of the nonanalytic equation of state and of the computation of thermodynamic properties tabulated in this report. The specific heat measurements are described where appropriate, and the analytic, BWR-type of equation of state [10] is described in Sections 3.5 and 5.5. Finally, some comparisons are made between experimental and calculated data from the two equations of state, and also between calculated thermodynamic properties from the two equations.

In present work, we have derived second virial coefficients from 200 through 320 K. Vapor pressures have been measured from 160 K (2.75 bar) up to the critical point at 234 K (44.607 bar), and data have been derived via thermal loops from the triple- to the normal boiling-point (144 K). Some orthobaric densities have been derived at temperatures well below the critical. Apparent gravitational effects in our P-p-T data near the critical point preclude accurate extrapolation of experimental isochores to the vapor pressure curve in the critical region.

We have formulated the vapor pressures and orthobaric densities from the triple- to the critical-point, and then have developed the highly constrained, nonanalytic equation of state via our P-p-T data. This equation has the valuable property for thermodynamic computations that it is structured to be consistent with the known behavior of specific heats about the critical point. We also have fit an analytic 32-term Benedict-Webb-Rubin (BWR) equation, useful for many applications, to the P-p-T and specific heat data.

We subsequently formulate the available, ideal gas specific heats. We derive heats of vaporization via thermal loops from the triple- to the boiling-point, and via the Clapeyron equation up to the critical temperature, and formulate these data, to obtain enthalpies, entropies, and specific heats of the saturated liquid, and finally a complete thermodynamic network over the  $P-\rho-T$  surface. We then compare results from the analytic and nonanalytic equations.

The commercially purified NF $_3$  for the PVT work is 99.925 percent pure, and 99.90 percent for the specific heat measurements. Apparatus and the data-reduction programs for PVT work are the same as modified by G. C. Straty in prior work on ethylene [19]. The sample cell is 12.5 cm high, with a volume of about 28.5 cm $^3$ . It is connected to a pressure transducer via a very small stainless steel capillary tube, brought out through the walls of the cryostat at a height within about 5 cm above the top of the cell (to avoid corrections for hydrostatic pressures in the former, vertical capillary). The transducer was maintained at 330 K.

Symbols and units for this report are in Appendix A, and fixed-point values in Appendix B. Computer programs are in Appendices C and D. The density-temperature phase diagram is outlined in fig. 1, where the upper left corner shows the qualitative behavior of freezing liquid densities. Explanations for table headings are in Appendix E.

#### 2. PHYSICAL PROPERTIES

# 2.1 Fixed-Point Values

These values are listed in Appendix B.

- (a) The Triple Point. The temperature used is from Pierce and Pace by subtracting 0.01 K for the ice-point [15]. This choice was made before our subsequent redetermination yielded a value 0.1 K higher [22]. The pressure is from our vapor-pressure eq. (1). The liquid density is assigned as a fitting parameter in eq. (2). The vapor density from eq. (3) is based on data derived from the vapor-pressure and virial equations.
- (b) The Boiling Point. The temperature of 144.0935 K is from the vapor-pressure eq. (1) at a pressure of 1 atm = 1.01325 bar, as compared with 144.10 K reported by Jarry and Miller [11]. The liquid and vapor densities are from eqs. (2) and (3).
- (c) The Critical Point. The temperature, 234.0 K, is selected for fitting estimated orthobaric densities and P- $\rho$ -T data, as compared with 233.9  $\pm$  0.1 K

observed directly by Jarry and Miller [11]. The density, 7.92 mol/L, has been selected by the condition that, at the critical point, the slope of the critical isochore (from the equation of state) be equal to the slope of the vapor-pressure equation,  $\partial P/\partial T = dP_{\sigma}/dT$ . The critical pressure is from the vapor-pressure eq. (1).

# 2.2 Vapor Pressures and Melting Pressures

(a) Vapor Pressures. Vapor pressures from the triple- to the boiling-point have been estimated via thermal loops as described in refs. [3,4], and in Program Ziegler, Appendix C. This computation yields also densities of the saturated vapor, and heats of vaporization. Information used includes the ideal gas specific heats, eq. (7); the virial eq. (4); specific heats of the saturated liquid [16]; and the heat of vaporization at the normal boiling point [16]. Vapor pressure above the boiling point have been measured directly, as reported in table 1. The data are formulated by use of the argument  $x \equiv T/T_C$ ,

$$ln(P) = a + b/x + c \cdot x + d \cdot x^2 + e \cdot x^3 + f \cdot x (1 - x)^{\epsilon}$$
, (1)

where P is in bar,  $\varepsilon = 1.75$ , and

a = 20.3154 17602 d = 20.1621 94616

b = - 8.3620 69370 e = - 6.9186 62727

c = -21.3989 86401 f = 3.6777 99376

Under heading ID in table 1 is given the source of data for each line, as specified at the top of this table. Heading DPS/DT is for calculated slopes of the vapor-pressure curve in bar/K. The calculated critical-point pressure (at 234.0 K) is 44.60713 bar, and the critical-point slope is 1.24509 bar/K. Data from other sources are given for comparison at the bottom of table 1. From about 2 bar up to the critical point, the vapor pressures of Jarry and Miller exceed ours by several percent. They used a 1000 psi Bourdon gage accurate to 0.25 percent of full scale, whereas we used a piston-type, oil dead-weight gage.

The last column of table 1 gives the experimental residual,

$$\ln(P/P_t)/\ln(P_c/P_t) - (1 - T_t/T)/(1 - T_t/T_c)$$
,

which has been used in the past to develop the extended, nonanalytic vapor-pressure equation.

At the normal boiling point (144.0935 K) the vapor-pressure slope from eq. (1) is  $dP_{\sigma}/dT = 0.070882$  bar/K. The Clapeyron equation, with orthobaric

densities from eqs. (2) and (3) below, yields a derived heat of vaporization,  $Q_{vap} = 11.583 \text{ kJ/mol}$ , as compared with the experimental value 11.587 + .022 kJ/mol of Pierce and Pace [16], (adjusted to the  $C^{12}$  molecular weight scale).

(b) Melting Pressures. No data have been found for pressure vs. temperature at the liquid-solid equilibrium of NF<sub>3</sub>, i.e., the melting line. This boundary is used here in the tables of functions along isobars merely as a low-temperature limit for the tabulations, and for convenience we have substituted the reduced Simon equation for methane,  $P = P_t + P_o \cdot [(T/T_t)^{\varepsilon} - 1]$ , with  $P_o = 1909.40$  bar,  $\varepsilon = 1.85$ , and  $P_t$ ,  $T_t$  for NF<sub>3</sub>.

# 2.3 The Orthobaric Densities

We have used the present nonanalytic equation of state (which incorporates the vapor-pressure equation) to describe pressure vs. T along experimental pseudo-isochores. For a given density (isochore) it is necessary merely to find the coexistence temperature,  $T_{\sigma}(\rho)$ , by iteration for a best "fit" of these data [5], as follows from eq. (6) below for a fixed density (and assuming values of non-linear parameters from preliminary work) -

$$[P - P_{\sigma}(T_{\sigma}) - \rho R^{*} \cdot (T - T_{\sigma})]/(\rho^{2} R^{*} T_{c}) = B \cdot \Phi(\rho, T, T_{\sigma}) + C \cdot \Psi(\rho, T, T_{\sigma}),$$

wherein B and C are least-squares coefficients for a given density. At densities in the range roughly  $\rho_{\rm C}$   $\pm$  30 percent, the results are unacceptable, but their qualitative behavior suggests gravitational effects on the P-p-T data in the critical region, by comparison with published studies of this effect [14,20,23]. The critical density of NF<sub>3</sub>, 0.562 g/cm<sup>3</sup>, is large relative to that of many simple substances, e.g., 0.16 g/cm<sup>3</sup> for methane.

The behavior of orthobaric densities about the critical point is well known to be described by a term  $|T-T_c|^{\epsilon}$  where traditionally the exponent was  $\epsilon=1/3$ , and more recently  $\epsilon=0.35$  [17]. In the following representations of the orthobaric densities we use  $\epsilon=1/3$ , and a minimum of coefficients by use of data well-removed from the critical temperature.

(a) Saturated Liquid Densities. In table 2 our derived densities are identified by ID =  $900^+$ , wherein the last two digits are the sequence number of the experimental pseudo-isochore run. The extensive data set of Jarry and Miller from 78 to 170 K at ID = 6 is included with a low weighting. Our calculated densities are roughly 0.4 percent greater than theirs. As the accuracy in each set is believed to be  $\pm$  0.1 percent, the reader of this report

must assume an uncertainty of 0.2 percent about the mean. Our densities are essential for our equation of state in the compressed liquid region. In table 2 the heading X is for  $x(T) \equiv (T_c - T)/(T_c - T_t)$ , and DDS/DT is for slope of the saturated liquid curve in (mol/L)/K. We represent these densities by use of the further reduced variable,  $y(\rho) \equiv (\rho - \rho_c)/(\rho_t - \rho_c)$ ,

$$y = x + (x^{\epsilon} - x) f(T), f(T) \equiv a + b \cdot exp[2 \cdot (1 - T_c/T)],$$
 (2)

where  $\varepsilon = 1/3$ , and

$$a = 0.754377410$$
,  $b = 0.027975083$ .

The experimental residual,  $(y-x)/(x^{\varepsilon}-x)$ , in the last column of table 2 was used to develop a functional form for f(T).

(b) Saturated Vapor Densities. In table 3 our densities derived via thermal loops are identified by ID = 43, and results via isochores, the vapor-pressure equation and the equation of state by ID =  $900^+$ . Our recent formulation yields a compressibility factor for saturated vapor which approaches unity at low densities, by use of the vapor-pressure equation [4]. Let  $A_0 \equiv (Z_c-1)$  where  $Z_c$  is value of the compressibility factor at the critical point, and define the variables,

$$\pi(T) \equiv P_{\sigma}(T)/P_{C}, \quad x(T) \equiv T/T_{C}, \quad u(T) \equiv 1 - x$$

The saturated vapor densities,  $d_q = P_{\sigma}(T)/[Z_{\sigma}(T) R T]$ , then are described by

$$Z_{\sigma}(T) = 1 + A_{\sigma} \cdot \pi \cdot x^{-2} \cdot f(x) , \quad f(x) = 1 + a \cdot u^{\varepsilon} + b \cdot u + c \cdot u^{2}, \quad (3)$$

with

$$\varepsilon = 1/3$$
 b = 0.3800 17523  
a = -0.7109 56694 c = 1.6228 47586

The seventh and eighth columns of table 3 give experimental and calculated values of the compressibility factor for saturated vapor. The next-to-last column gives the experimental values,  $F(Z) \equiv (Z-1) \cdot x^2/[A_0 \cdot \pi]$ , used to develop a functional form for f(x). Very small inaccuracies in low-density data yield large relative errors in the experimental values of (Z-1). The last column of table 3 gives the slope of the saturated vapor densities curve in (mol/L)/K.

# 2.4 Second Virial Coefficients

The truncated virial equation of state (for gas at densities roughly below  $\rho_{\text{C}}/5)$  may be arranged to

$$(Z - 1)/\rho = B(x) + C(x) \cdot \rho + \dots$$
 (4)

in which we use reduced variables  $x = T/T_c$ ,  $\rho = d/d_c$ . With P- $\rho$ -T data along seven isotherms from 200 thru 320 K we have obtained values for the second and third virial coefficients, B(x) and C(x), by least squares. Results for C(x) are not highly regular, but for B(x) they are formulated as follows,

$$B(x) = B_1 + B_2/x + B_3/x^3 , (5)$$

$$B_1 = 0.4938 \ 2731$$
  $B_3 = -0.3898 \ 3811$   $B_2 = -1.3097 \ 2686$ 

In table 4, column B(T) is the second virial coefficient in cm $^3$ /mol, whereas B $^*$  is the dimensionless value B(x) in eq. (4). This equation with C(x) = 0 was used for the thermal loop computations [3,6] to obtain the density at any given (P,T), and to obtain  $\Delta H$  and  $\Delta S$  by integration along isotherms from ideal gas states up to the derived, saturated vapor boundary at temperatures up to the normal boiling point.

#### 2.5 The Nonanalytic Equation of State

This isochoric equation is modified from those described earlier [3,4,5,6]. It is constrained to a given liquid-vapor coexistence boundary, and yields a maximum in isochoric specific heats at the critical point. It is adjusted to our compressibility data in table 5. Data of Burns and of Van der Waal are not used for the adjustment.

At the critical point the derivatives  $\partial \rho/\partial T$  and  $\partial \rho/\partial P$  become infinite for any pure fluid. The slightest error in experimental pressures due to gravitational effects therefore will correspond to gross deviations of density in the critical region, as is well known. In present work, P- $\rho$ -T data in the critical region are given a low weighting, where density deviations are several percent.

The form of this nonanalytic equation is

$$P - P_{\sigma}(\rho) = \rho R^* \cdot [T - T_{\sigma}(\rho)] + \rho^2 R^* T_{c} \cdot F(\rho, T) , \qquad (6)$$

$$F(\rho,T) \equiv B(\rho) \cdot \phi(\rho,T) + C(\rho) \cdot \Psi(\rho,T) , \qquad (6a)$$

in which, for any given density (isochore), the liquid-vapor coexistence temperature,  $T\sigma(\rho)$ , is obtained by iteration from eqs. (2) and (3) for the

orthobaric densities, and the vapor pressure,  $P_{\sigma}[T_{\sigma}(\rho)]$ , thus is a function of density. The temperature-dependent functions in eq. (6a) are

$$\phi(\rho,T) \equiv x^{1/2} \cdot \ln[T/T_{\sigma}(\rho)] , \qquad (6b)$$

$$\Psi(\rho,T) \equiv \psi(\rho,T) - \psi_{\sigma}(\rho) , \qquad (6c)$$

where  $\psi_{\sigma}(\rho)$  is obtained from  $\psi(\rho,T)$  merely by replacing T with  $T_{\sigma}(\rho)$ ,

$$\psi(\rho,T) \equiv \delta \cdot f_1(T) + (1 - \delta) \cdot f_2(\rho,T) , \qquad (6d)$$

$$f_1(T) \equiv \exp[\varepsilon \cdot (1 - x)]$$
, (6e)

$$f_2(\rho,T) = 1 - (\omega - \omega^{\eta}/\eta)/(1 - 1/\eta)$$
 (6f)

The parameter,  $0 \le \delta \le 1$ , in eq. (6d) is for relative weighting of the analytic and nonanalytic parts, and --

$$\omega(\rho,T) \equiv [1 - \theta(\rho)/T]$$
, (6g)

where  $\theta(\rho)$  is a locus of temperatures inside the coexistence envelope

$$\theta(\rho) \equiv T_{\sigma}(\rho) \cdot \exp[-\alpha \cdot f(\rho)]$$
, (6h)

$$f(\rho) \equiv |\rho - 1|^3/(\rho_t - 1)^3$$
, (6i)

and  $\rho_t$  is reduced density of liquid at the triple point. The density-dependent coefficients in eq. (6a) are

$$B(\rho) \equiv B_1 + B_2 \cdot \rho + B_3 \cdot \rho^2$$
, (6j)

$$C(\rho) \equiv (C_1 + C_2 \rho) \cdot (\rho - 1) \cdot \exp(-\gamma \cdot \rho^m) . \qquad (6k)$$

Parameters and least-squares coefficients of (6) for NF<sub>3</sub> are  $\alpha = 1, \gamma = 1, \delta = 1/2, \varepsilon = 1, \eta = 1.10, m = 1,$ 

$$B_1 = 0.5519 9813 920$$
  $C_1 = 0.7406 7409 894$ 

$$B_2 = 0.1326 8809 584$$
  $C_2 = 0.2937 5371 520$ 

 $B_3 = 0.2060 8495 802$ 

The overall "fit" of present P- $\rho$ -T data is not sensitive to small relative changes in the non-linear parameters, excepting  $\eta = 1.10$ , which value was not explored. Table 6 gives behavior of coefficients  $B(\rho)$ ,  $C(\rho)$ .

In present work the assigned critical density was varied to obtain a critical isochore (from the equation of state) having a slope at the critical point equal to that of the vapor-pressure equation,  $\partial P/\partial T = dP_{\sigma}/dT$ . Following this, these two slopes at the critical point were constrained to equality via the least-squares program [9,12]. This procedure leads to a critical isotherm free of negative slopes,  $(\partial P/\partial \rho)_{T_C}$ , as shown in table 7. The sign of the curvatures of isochores,  $\partial^2 P/\partial T^2$ , at the coexistence boundary

The sign of the curvatures of isochores,  $\partial^2 P/\partial T^2$ , at the coexistence boundary  $[T = T_{\sigma}(\rho)]$ , is determined uniquely by the sign of  $C(\rho)$  because  $\partial^2 \Phi/\partial T^2 = 0$  on this boundary. The present compressed liquid isochores for NF<sub>3</sub> have positive curvatures  $\partial^2 P/\partial T^2$  up to the highest densities (lowest temperatures) measured experimentally, in contrast to experience with other, simple cryogenic fluids. This behavior is obtained from the equation of state via the positive values of  $C(\rho)$  at high densities as seen in table 6.

# 2.6 The Ideal Gas Functions

We have formulated specific heats  $C_p^0(T)$  for NF3 from the JANAF tables [2] as follows, using  $x \equiv T/100$ ,

$$C_p^0(T)/R = 4 + \exp(-\epsilon/x) \cdot \sum_{i=1}^5 A_i \cdot x^{1-i}$$
, (7)

where,

Table 8 shows the "fit" of data used. The calculated values of  $(H^0-H^0_0)$  and of  $S^0$  are obtained by numerical integrations, starting at T = 300 K. Table 9 gives interpolated values at integral temperatures.

# 2.7 The Heats of Vaporization

Table 10 shows the "fit" of data used for NF3. Those below the boiling-point at ID = 39 we derived via thermal loops as described above, and those at ID = 40 are via the Clapeyron equation. Unpublished, estimated data from the Aerojet Company [1] are given last for comparison, ID = 23. The formulation of these data uses argument  $x(T) \equiv (T_C - T)/(T_C - T_T)$ ,

$$Q_{vap}/Q_{t} = x + (x^{\varepsilon} - x) \cdot [a + b \cdot x + c \cdot x^{2}],$$
 (8)

where  $\varepsilon = 0.38$ , and

 $Q_t = 14.548 \text{ kJ/mol}$  b = 0.2695 36103a = 0.9982 47122 c = -0.4050 10672

The experimental residual in the last column of table 10 is

$$[Q_{\text{vap}}/Q_{t} - x]/(x^{\varepsilon} - x)$$
 .

# 2.8 Specific Heats of Saturated Liquid

Specific heats,  $C_{\sigma}(T)$ , along the saturated liquid path, are needed as a base to compute specific heats in compressed liquid states. The techniques described here were developed before the measured data of Weber [22] were available, and they were used to produce the values given in tables 14 and 15. Starting with the ideal gas functions  $S^{O}(T)$ , we have used the equation of state and the heats of vaporization to tabulate  $S_{\sigma}(T)$  for the saturated liquid at 35 temperatures from the triple- to the critical point. These are represented in J/mol/K with an rms relative deviation of 0.002 percent by use of  $x(T) \equiv T/T_{\sigma}$ ,  $u(T) \equiv (1-x)$ ,

$$S_{\sigma}(T) - S_{c} = A_{1} \cdot u^{\varepsilon} + A_{2} \cdot ln(x) + \sum_{i=3}^{7} A_{i} \cdot u^{i-2}$$
, (9)

where  $\varepsilon = 0.33$ , and

 $S_{C} = 197.03182 \text{ J/mo1/K}$   $A_{4} = -16.4628 7979$   $A_{1} = -27.0414 1165$   $A_{5} = 241.1959 696$   $A_{2} = 168.4875 348$   $A_{6} = -288.5828 349$  $A_{3} = 117.5913 487$   $A_{7} = 230.9162 107$ 

The specific heats for saturated liquid follow from the relation  $C_{\sigma}(T) = T \cdot dS_{\sigma}/dT$ , in J/mol/K,

$$C_{\sigma}(T) = -\epsilon \cdot A_{1} \cdot x \cdot u^{\epsilon-1} + A_{2} - x \cdot \sum_{i=3}^{7} (i-2) \cdot A_{i} \cdot u^{i-3}$$
 (10)

Calculated values for  $C_{\sigma}(T)$  appear in the eighth column of page two of table 14.

#### 2.9 Specific Heats at Constant Volume

The specific heat at constant volume,  $C_V(\rho,T)$ , may be calculated from the equation of state and the ideal gas properties by methods outlined in Secion 3. Recently, new experimental data for specific heats have been published by one of us [22]. Since this quantity is a measure of the temperature variation of the state properties (E,H,S) a comparison between calculated and experimental values is useful for estimating uncertainties. Such a comparison with the nonanalytic and with the analytic equation of state is given in fig. 3 and in table 17.

# 2.10 The Analytic Equation of State

For many purposes it is convenient to use an analytic equation of state to represent the properties of a substance. Here we have used the 32 term BWR equation reported by Jacobsen [10], which has the form,

$$P = \rho RT + \rho^{2}(A_{1}T + A_{2}T^{1/2} + A_{3} + A_{4}/T + A_{5}/T^{2})$$

$$+ \rho^{3}(A_{6}T + A_{7} + A_{8}/T, + A_{9}/T^{2})$$

$$+ \rho^{4}(A_{10}T + A_{11} + A_{12}/T)$$

$$+ \rho^{5}(A_{13})$$

$$+ \rho^{6}(A_{14}/T + A_{15}/T^{2})$$

$$+ \rho^{7}(A_{16}/T)$$

$$+ \rho^{8}(A_{17}/T + A_{18}/T^{2})$$

$$+ \rho^{9}(A_{19}/T^{2})$$

$$+ \rho^{9}(A_{20}/T^{2} + A_{21}/T^{3})$$

$$+ \rho^{5}(A_{22}/T^{2} + A_{23}/T^{4})$$

$$+ \rho^{7}(A_{24}/T^{2} + A_{25}/T^{3})$$

$$+ \rho^{9}(A_{26}/T^{2} + A_{27}/T^{4})$$

$$+ \rho^{11}(A_{28}/T^{2} + A_{29}/T^{3})$$

$$+ \rho^{13}(A_{30}/T^{2} + A_{31}/T^{3} + A_{32}/T^{4})]$$

The parameters are given in table 16 and a listing of the program and subroutines used is given in Appendix D. From the listing it is seen that all of the thermodynamic properties may be calculated quickly and conveniently in closed form as functions of the density and temperature. Since the equation is explicit in pressure, the density must be found by iteration. The FUNCTION FINDD in the appendix is used for this purpose. This equation of state, with 32 adjustable parameters, is much more flexible than the nonanalytic equation; therefore, a large body of precise data is necessary to insure proper behavior. In addition it should not be extrapolated far beyond the bounds of the data, particularly in the direction of higher densities. On the other hand, since the derived properties can be expressed directly in terms of the parameters, other data such

as the specific heats may be included in the fitting process by making use of multiproperty fitting techniques such as described by Hust and McCarty [9].

In applying the equation to NF $_3$  we used the 225 P-p-T data of Goodwin [7], 25 points on the saturation boundary calculated from the relations in Section 2.3 above, a few high density points in the compressed liquid between the triple point and 90 K calculated from the nonanalytic equation, 47 single phase specific heats,  $C_{_{\rm V}}$ , and 101 saturated liquid specific heats,  $C_{_{\rm O}}$ , from ref. [22]. We also included some calculated data which help to insure that the chemical potential is the same for the saturated liquid and vapor at a given temperature, in other words that  $\Delta H = T\Delta S$  across the two phase boundary. These data make use of the vapor pressure and orthobaric density equations in Sections 2.2 and 2.3. In addition the equation is constrained to the critical point, and the derivatives  $(\partial P/\partial \rho)_T$  and  $(\partial^2 P/\partial \rho^2)_T$  are constrained to be zero at the critical point.

This equation, like all analytical equations, does not fit the data well in the critical region. The average absolute deviation in density is 0.50 pct when all of the data are considered. If the deviations of the points in the range 235 - 240 K and  $\rho_{\rm C}$   $\pm$  28 percent are not counted, the average absolute deviation drops to 0.14 percent. The average absolute deviation from the C $_{\rm V}$  data is 0.97 pct and for the C $_{\rm G}$  data it is 1.42 pct, which are quite reasonable for this type equation. Some typical deviations are shown in figs. 2 and 3.

#### 3. COMPUTATIONAL METHODS

(Nonanalytic Equation of State)

The numerical values for E and H in this report are based on the assigned value, E = 0 at the liquid triple-point, obtained by use of the arbitrary value,  $E_0^0 = 12340.685$  J/mol, for ideal gas at T = 0. Specific heats of Pierce and Pace [16] could be integrated to give the solid at T = 0 as reference state.

#### 3.1 The Homogeneous Domain

The homogeneous domain of fig. 1 includes all regions which can be attained along isotherms starting at zero density without crossing the vapor-liquid "dome," and without passing very close to the critical point at  $T \ge T_c$ .

We start our computations with ideal gas thermodynamic functions at zero density, and then integrate along isotherms by use of the equation of state in the following relations,

$$\Delta E = \int [P - T \cdot (\partial P/\partial T)] \cdot d\rho/\rho^2 , \qquad (12)$$

$$\Delta C_{V} = -T \cdot \int (\partial^{2}P/\partial T^{2}) \cdot d\rho/\rho^{2} , \qquad (13)$$

$$\Delta S = R \cdot \ln[P^{O}/(\rho RT)] + \int [R - (\partial P/\partial T)/\rho] \cdot d\rho/\rho , \qquad (14)$$

Equation (14) is for use with initial entropies in hypothetical ideal gas states at  $P^{O} = 1$  atm. For all other initial states we use

$$\Delta S = -\int (\partial P/\partial T) \cdot d\rho/\rho^2 . \qquad (14a)$$

In each  $(\rho,T)$  state, reached by above integrations, we compute

$$H = E + P \cdot v , \qquad (15)$$

$$C_{p} = C_{v} + T \cdot (\partial P/\partial T)^{2}/(\partial P/\partial \rho)/\rho^{2} , \qquad (16)$$

$$W^2 = C_p \cdot (\partial P/\partial \rho)/C_v . \tag{17}$$

# 3.2 The Saturated Liquid

At temperatures from the triple point up to the critical point, we first obtain thermofunctions for the saturated vapor via eqs. (12) through (15). We then use eq. (8) for the heat of vaporization,  $Q_{\rm vap}$ , to compute

$$\Delta H = -Q, \quad \Delta S = \Delta H/T \quad , \tag{18}$$

such that the free energy of vaporization,  $\Delta F = \Delta H - T \cdot \Delta S$ , is zero. Having obtained H and S for the saturated liquid, we compute  $E = H - P \cdot v$ .

The single-phase specific heat,  $C_V(\rho,T)$ , at the saturated liquid boundary is obtained via eq. (10) for  $C_G(T)$  and the thermodynamic relation,

$$C_{V}(\rho,T) = C_{\sigma}(T) + T \cdot (\partial P/\partial T) \cdot (d\rho_{\ell}/dT)/\rho_{\ell}^{2} , \qquad (19)$$

where  $\rho_{\ell}$  is density of the saturated liquid. Values for  $C_p(\rho,T)$  and  $W(\rho,T)$  on this boundary follow from eqs. (16) and (17). For liquid at the boiling point we have obtained.

$$T_b$$
 = 144.0935 K,  $H_b$  = 5 538.1 J/mol,  $E_b$  = 5 533.4 J/mol,  $S_b$  = 147.694 J/mol/K.

#### 3.3 The Compressed Liquid

Starting with above values for E, S, and  $C_{\rm V}$  on the saturated liquid boundary, we use eqs. (12), (13), and (14a) to integrate along isotherms, and then obtain H,  $C_{\rm D}$ , and W via eqs. (15), (16), and (17).

#### 3.4 Subroutine THERMO

In Appendix C, we have prepared a Subroutine, THERMO, for convenience to the reader in computing properties at any random, (P,T) point. ENTRIES at the bottom of this subroutine are given for the two-phase boundaries, in which the independent variable is pressure. The present computational method of integration along isotherms cannot be used on or very near the critical isotherm to obtain  $C_V$ ,  $C_p$ , or W at supercritical densities or pressures, because the specific heats pass through infinity at the critical point.

### 3.5 Computations With the Analytic Equation

Calculation of the thermodynamic properties by means of the analytic equation is extremely simple. Relations (12-17) are used for this purpose. If, as indicated in Section 2.10, data are included to influence the equation to yield a constant chemical potential across the gas-liquid boundary, we can then perform the integrations indicated in eqs. (12-17) right through the two phase region in closed analytical form, without reference to heats of vaporization or vapor pressures. Examples illustrating these calculations are given in the program listing in the appendix.

#### 4. COMMENTS

It is well known that extremely accurate physical properties data are needed for thermodynamic properties computations. In present work we see inherent deficiencies in P-p-T data near the critical point due, we believe, to gravity. For this the only remedy apparently is specialized apparatus, because no simple computational procedure is available to make corrections [14].

The orthobaric densities in the critical region are especially important for the Clapeyron equation, and for the present highly-constrained equation of state. They should be measured directly by methods such as those used by Weber [21] or Haynes [8].

Heats of vaporization also always are needed over the widest practical temperature range, and it is obvious also, that a Burnett-type determination of virial coefficients is needed, especially for lower temperatures and densities than available in present work.

The above deficiencies lead to a diminished accuracy, but not to irregularities or inconsistencies with the present, nonanalytic equation of state, as seen by inspecting derivatives of the P- $\rho$ -T surface in tables 7, 11, 12, 14, and 15.

# 5. TABLES OF PHYSICAL AND THERMODYNAMIC PROPERTIES 5.1 Calculated P-p-T Isochores and Isotherms

Tables 11 and 12 give a selection of isochores and isotherms computed by equation of state (6). These are essential to examine behavior of the  $P(\rho,T)$  surface. They are a useful supplement to the isobars of table 15 for interpolating  $P-\rho-T$  values and their derivatives.

# 5.2 The Joule-Thomson Inversion Locus

Table 13 gives the P-p-T locus of the J.-T. inversion,  $(\partial T/\partial P)_H = 0$ , obtained from equation of state (6) under the condition  $T(\partial P/\partial T) = \rho(\partial P/\partial \rho)$ . This table has been computed to temperatures well above those of P-p-T data, to show a maximum in P-T coordinates. In this table under heading DI are given the initial densities used to start the iteration for density in heading MOL/L. We thus know that convergence is attained within present limits of DI  $\pm$  3.2 mol/L, Subroutine JTLOCUS.

# 5.3 Thermophysical Properties of the Saturated Liquid

Table 14 gives physical and thermodynamic properties of saturated liquid, computed by methods of Section 3, using eq. (6). Column headings are interpreted on the first page of this table.

# 5.4 Thermophysical Properties Along Selected Isobars

Table 15 gives physical and thermodynamic properties on isobars, computed by methods of Section 3, using eq. (6). Explanations for this table are given on the first page. This table is extrapolated below the minimum temperature (90 K), and above the maximum pressure ( $\sim$  300 bar) of P- $\rho$ -T data used for adjusting the equation of state.

# 5.5 Results From the Analytic Equation

The derived properties may be calculated from the analytic equation by making use of the subroutines given in Appendix D. A sample program is also included there to illustrate the proper method of utilizing the subroutines. Detailed calculated results are not tabulated in this report because of the space requirements. However, table 17 gives a comparison of several of the derived

properties calculated via the analytic and nonanalytic equations. Since the zero for enthalpy is arbitrary, the equations were adjusted to give the same value for the liquid at the triple point.

Table 17 compares properties computed via the nonanalytic eq. (6) with properties via the BWR-type eq. (11). At given pressures and temperatures, table 17 presents differences [eq. (6) minus eq. (11)] of density in percent; of enthalpy (J/mol); of entropy (J/mol/K); and of the specific heats,  $C_V$ ,  $C_P$ , in percent. These comparisons serve to indicate the uncertainties in the derived results.

Figure 2 presents a comparison of the deviations of experimental densities from calculated values obtained via the two equations of state: open circles for the nonanalytic equation and filled circles for the BWR-type equation. The greatest relative deviations of several percent, from each equation, occur in the critical region near  $\rho_{\rm C}$  = 7.92 mol/L, and T<sub>C</sub> = 234.0 K. This behavior has been encountered often in work on other fluids.

Figure 3 presents a comparison of the deviations of experimental single-phase specific heats [22] from calculated values via the two equations of state: open circles for the nonanalytic equation, and filled circles for the BWR-type equation.

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#### Appendix A. Symbols and Units

Subscripts c and t refer to critical and liquid triple points.

Subscripts g and  $\ell$  refer to saturated vapor and liquid. Subscript o refers to liquid-vapor coexistence. α, γ, δ, ε, η non-linear parameters in the equation of state  $B(\rho)$ ,  $C(\rho)$ density-dependent coefficients in the equation of state  $B^{*}(x)$ reduced second virial coefficient  $C_{v}(\rho,T)$ isochoric specific heat, (J/mol)/K  $C_{\mathbf{p}}(\rho,T)$ isobaric specific heat, (J/mol)/K molal heat capacity for saturated liquid, (J/mol)/K  $C_{\alpha}(T)$ d density, mol/L  $E(\rho,T)$ the internal energy, J/mol E 0 H 0 H 0 12,340.685 J/mol (arbitrary) enthalpy for ideal gas state at T = 0 $H(\rho,T)$ the enthalpy, J/mol J the joule, 1 N-m the liter,  $10^{-3}$  m<sup>3</sup> L 71.0019 grams of  $NF_3$  ( $C^{12}$  scale) mol pressure in bar, 1 bar =  $10^5$  N/m<sup>2</sup>, (1 atm = 1.01325 bar) Р the vapor pressure, bar  $P_{\sigma}(T)$  $P_{\sigma}(\rho)$  $P_{\alpha}[T_{\alpha}(\rho)]$ , vapor pressure as function of density  $\Phi(\rho,T)$ function in the equation of state  $\Psi(\rho,T)$ function in the equation of state R the gas constant, 8.3145 (J/mol)/K, 0.083145 (bar-L/mol)/KR \* (0.083145) •d<sub>c</sub>, bar/K, for the equation of state  $d/d_{C}$ , reduced density ρ  $S(\rho,T)$ the entropy, (J/mol)/K Τ temperature, K (IPTS 68)  $T_{\sigma}(\rho)$ liquid-vapor coexistence temperature, K θ(ρ) defined locus of temperatures, K  $[1-\theta(\rho)/T]$ , for the equation of state  $\omega(\rho,T)$  $T/T_{c}$ , for the equation of state x(T) $\times(T)$ variously defined for other equations  $x^{\alpha}(b)$  $T_{\sigma}(\rho)/T_{c}$ , reduced coexistence temperature  $P/(d \cdot R \cdot T)$ , the "compressibility factor"  $Z(P,\rho,T)$ 

Appendix B. Fixed-Point Values Used for NF3

	Triple Point	Boiling Point	Critical Point
Temperature, K	66.35	144.0935	234.0
Pressure, bar	1.85425·10 <sup>-6</sup>	1.01325	44.60713
Density, mol/L	_		
Vapor	3.3612·10 <sup>-7</sup>	8.782·10 <sup>-2</sup>	7.92
Liquid	26.320	21.662	7.92

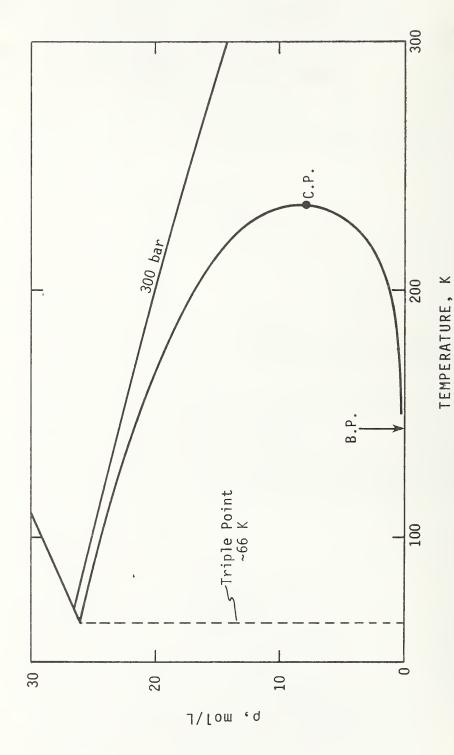


Figure 1. Density-Temperature Phase Diagram for Nitrogen Trifluoride.

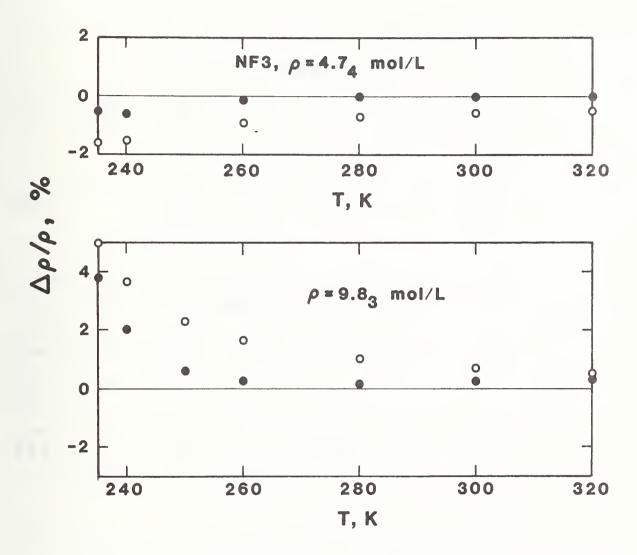


Figure 2. Comparisons of experimental with calculated densities: open circles for eq. (6); filled circles for eq. (11).

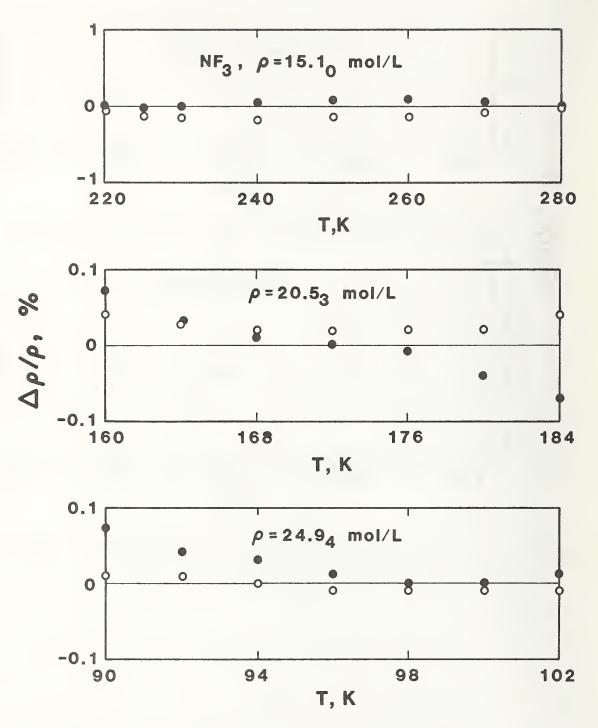


Figure 2, Continued. Comparisons of experimental with calculated densities: open circles for eq. (6); filled circles for eq. (11).

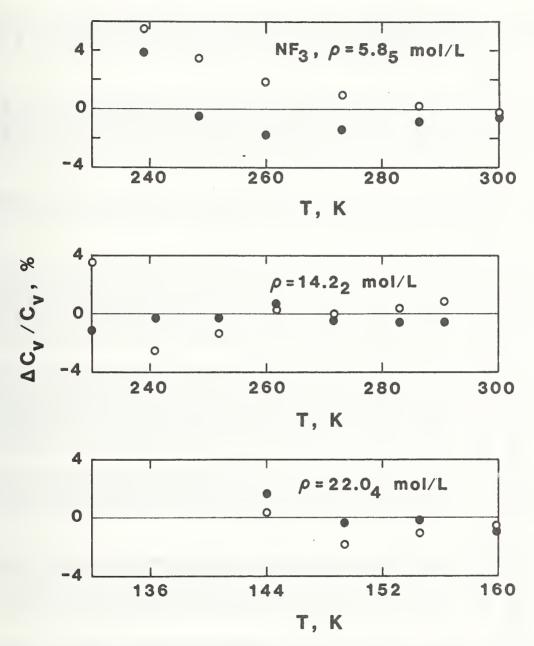


Figure 3. Comparisons of experimental with calculated specific heats: open circles for eq. (6); filled circles for eq. (11).

-6,918662727 -8.362069370 -21.398986401 20.162194616 = 66.350, TCRT = 234.000 = .18543E-05, PCRT = 44.607130, DPSDT = 1.24509 (3) PIERCE(1954), (6) JARRY(1956), (10) MENZEL(1933). (43) THERMALOOPS VIA NBS VIRIAL, (100+) NBS(1979). = 1.750 NF3 VAPOR PRESSURES, EPP 20,315417602 TTRP

3.677799376

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Table 1. Continued.

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Table 1. Continued.

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PS/D	176E-0	248E-0	338E-0	443E-0	568E-0	712E-0	914E-0	115E+0	143E+0	175E+0	211E+0	252E+0	297E+0	346E+0	399E+0	461E+0	525E+0	597E+0	672E+0	845E+0	947E+0	106E+0	120E+0	393E-0	205E-0	507E-0	138E-0	174E-0	.347E-02	441E-0	520E-0	437E+0	647E-0	682E-0	708E-0	720E-0		
Z	4	3	2	44	4	0	0	$\sim$	5	5	8	4.	0.	.3	• 0	æ	2.	9 •	9.	7	80	•2	2.	4.5	5	9.4	5	• 2	.11	σ	4	$\sim$	8	4	.3	.2		
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, BA	17709E+0	27086E+0	39725E+0	55770E+0	76404E+0	10189E+0	14064E+0	19090E+0	25919E+0	34187E+0	43833E+0	56246E+0	70036E+0	86572E+0	10518E+0	12656E+0	15205E+0	18032E+0	21202E+0	28647E+0	33265E+0	38365E+0	44087E+0	19998E-0	11999E-0	30664E-0	90659E-0	11732E-0	.25065E-01	33597E-0	0530E-0	54569E+0	89379E+0	6285E+0	10086E+0	10307E+0		
×	5262	453	5638	5815	989	6161	6365	6572	6780	6987	7196	7408	7617	7826	8035	8253	8463	8680	8889	313	9527	9735	2466	3412	3745	3963	4545	4318	• 45534	4643	707	5805	6087	6127	6157	6169		
	23.15	7.60	31.94	36.07	40.16	44.17	48.96	53.79	58.66	63°51	68.39	73.35	78.26	83.15	88.02	93.14	98.05	03.13	08.01	17.93	22.95	27.80	32.77	9.85	7.65	2.75	99,35	01.05	106.550	08.65	10.15	35.85	45.45	43.39	44.08	44.37	CT = .033	
	• 00	.00	• 00	• 00	• 00	• 00	• 00	• 0 0	• 00	• 00	• 00	• 0 0	• 0 0	• 00	• 00	• 0 0	• 00	• 00	• 0 0	• 0 0	• 0 0	• 0 0	• 00	• 00	• 0 0	• 0 0	• 00	• 0 0	000-0	• 00	• 0 0	• 00	• 00	• 00	• 00	• 00	54. RMSP	
10	9	9	٩	9	9	9	9	9	9	9	9	9	9	9	9	9	9	9	9	9	9	ی	9						10								11 Q.	

NF3 VAPOR PRESSURES, EPP = 1.750

NF3 SATLIQUID DENSITIES, EL = .333
(6) JARRY, (11) SESHADRI, (900) NBS V.P., ISOCHORES/EQNSTATE.

TTRP = 66.350, TCRT = 234.000, DTRP = 26.320, DCRT = 7.920
.754377410 .027975083 0.000000000

					-			
ID	WT	T.K	х	MOL/L	CALCD	PONT	005/01	RESID
935	1.000	89.012	.86483	25.013	25.055	17	05718	.72962
934	1.000	105.189	.76833	24.124	24.112	• 05	05942	•76116
933	1.000	123.055	.66177	23.022	23.025	01	06247	.75832
932	1.000	142.576	.54533			01		
931	1.000			21.762	21.764		06699	.76180
931	1.000	158.678	•44928	20.651	20.645	• 03	07232	.76628
		174.718	• 35361	19.438	19.426	• 06	08021	.77042
929	1.000	184.904	• 29285	18.555	18.574	10	08756	.76811
928	1.000	197.490	.21778	17.422	17.392	. 17	10140	.77798
927	1.000	207.954	•15536	16.234	16.237	02	12116	.77569
926	1.000	215.559	•11000 _	15.216	15.228	08	14673	.77619
924	1.000	221.420	• 07504	14.267	14.273	04	18296	.77835
6	.020	78.040	.93027	25.619	25.675	22	05585	.68877
6	.020	79.090	.92401	25.549	25.616	26	05597	.68148
6	• 0 2 0	79.430	.92198	25.520	25.597	30	05601	•67367
6	•020	81.670	•90862	25.380	25.471	36	05528	.67185
6	•020	87.220	.87551	25.070	25.157	<b></b> 35	<b></b> 05696	.69683
6	.020	87.650	.87295	24.999	25.133	53	05701	.66781
6	.020	92.210	.84575	24.788	24.871	33	05760	.71039
6	• 020	94.260	.83352	24.619	24.753	54	05787	.68818
6	.020	97.000	.81718	24.506	24.594	36	05824	.71563
6	.020	99.4.40	.80262	24.323	24.451	52	05858	.70129
6	.020	101.780	.78867	24.225	24.314	37	05892	.72060
6	.020	104.060	.77507	24.056	24.179	51	05925	.70989
6	.020	109.900	.74023	23.704	23.831	53	06015	.71530
6	.020	114.780	.71112	23.422	23.535	48	06096	.72397
6	.020	119.460	.68321	23.140	23.248	46	06179	.72885
6	.020	119.520	.68285	23.140	23.244	45	06180	.72991
6	.020	124.498	.65321	22.830	22.935	45	06275	.73275
6	.020	129.410	.62386	22.535	22.624	39	06377	.73897
6	.020	131.050	.61408	22.436	22.519	37	06413	.74114
6	.020	134.220	.59517	22.253	22.314	27	06485	.74715
6	.020	135.340	.58849	22.168	22.241	33	06512	.74497
6	.020	139.150	•56576	21.943	21.992	22	-,06607	.75145
6	.020	139.930	.56111	21.859	21.940	37	06627	.74490
6	.020	143.990	.53689	21.633	21.669	16	06738	.75540
6	.020	144.650	.53296	21.549	21.624	35	06757	.74775
6	.020	149.330	.50504	21.239	21.305	31	06899	.75111
6	.020	153.920	.47766	20.901	20.984	40	07054	.74930
6	.020	158.520	.45022	20.577	20.656	38	07226	.75156
6	.020	164.150	.41664	20.197	20.243	23	07464	.75873
6	.020	169.530	. 38455	19.802	19.834	16	07727	.76238
ID	WT	T,K	X	HOL/L	CALCD	PCNT	DDS/DT	RESID
925	0 - 0 0 0	226.509	.04468	13 • 227	13.197	•23	24950	.78591
923	0.000	230.872	.01866	11.986	11.809	1.49	42936	.82051
922	0.000	233.122	.00524	10.844	10.440	3.87	97199	.91258
915	0.000	233.662	.00202	10.188	9.746	4.53	-1.81660	•97532
11	0.000	170.000	•38175	19.646	19.798	77	07752	.74360
11	0.000	180.000	.32210	18.762	18.993	-1.22	08372	.73510
11	0.000	190.000	.26245	17.794	18.116	-1.78	09234	.72567
11	0.000	200.000	.20280	16.750	17.133	-2.23	10519	.72029
11	0.000	205.000	.17298	16.181	16.585	-2.43	- • 11437	.71837
11	0.000	210.000	•14316	15.528	15.984	-2.85	12669	.71144
11	0.000	215.000	.11333	14.815	15.309	-3.23	14427	.70531
11	0.000	220.000	.08351	14.065	14.525	-3.17	17188	.70830
11	0.000	225.000	• 05368	13.123	13.553	-3.17	22328	.70811
11	0.000	230.000	• 02386	11.696	12.155	-3.78	36776	.68688

	0/50	129F-0	.425E-06	175E-0	583E-0	64E-0	4005-0	171F-0	309E-0	23E-0	833E-0	126E-0	183E-0	257E-0	コールのよう	4525-0	235E-0	421E-0	560E-0	753E-0	107E+0	139E+0	193E+0	32 UE + U	72F+0	523E-0	126E-0	257E-0	462E-0	116E-U	1 / UE - U	3405-0	80E-0	579E-0	710E-0	94E-0	18E+0	58E+0	99E+0
	17	4595.4	41	7.2114	5.1138	.8011	<b>46789</b> で III II I	0 47770 1 11 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	3859	.2473	.1392	• 0523	9910	9418	90 no	000 000 000 000	7390	7207	7187	7266	7431	7591	7789	0707	4770	.9105	8051	.2366	.9875	1600	07.42	2016	7790	7861	7513	7437	7474	7731	9100
3 VIRIAL. 920	Q.	0000	1.00000	6666•	6666	9999	7666	2000	9982	9966	6466	9921	9884	9836	37.75	97.01	8587	7754	7272	6741	6107	5672	5158	4460	775	6966	9921	9836	9701	7626	1460	An on	7538	7213	6848	6433	5949	5362	4774
IA NBS NF OCRT = 7.	2	9999	69995	.0000	0001	.0000	2000	9000	9977	9966	9945	9918	9883	9837	2000	9/C	8588	7740	7265	6736	6114	5690	5213	70744	3853	9916	860	9786	9668	1768	1040	7820	320	9469	725	384	965	389	0 2 0
X = 2.00 MALOOPS V 185E-06, 7586F+01			.01	0	• 0	0	•	5 C	9 0	0	0	0	0	<u>ت</u>	<b>.</b>	<b>3</b> C		- 44	0	0	4.	P • 3	) · H	10		· ·	9	S	۳ I	•	0 0	ນຸ	5	00	40	~	. 2		7.
G = .333, EG) D), (43) TH ERI GAT = .33611	0.0140	337416-0	.12519E-05	60206E-0	23241E-0	74982E-0	20851E-U 54402E-0	11374F-0	23098E-0	43534E-0	76974E-0	12883E-0	20564E-0	31505E-0	45577E=0	20075E-U	55006E+0	10946E+0	14728E+0	19414E+0	25789E+0	30709E+0	3/21UE+U	403216+0	59490E+0	43534E-0	12883E-0	31505E-0	66753E-0	26 22 45 + 0	36321E+0	85416F+0	12586E+0	15222E+0	18426E+0	22406E+0	7526E+0	34556E+0	42200540
S, NF = 3, E(H/KULOOR(197) ES/EQNSTATE, = 234,000, D(3)	NO.	3744E-0	.12520E-05	0203E-0	23238E-0	74972E-0	24 55 7 F - 1	1377F-0	23108E-0	3555E-0	7009E-0	12887E-0	20567E-0	31502E-0	455575	20000540	5000E+0	10965E+0	4742E+0	9429E+0	5761E+0	30616E+0	5818E+U	4/029E+0	8275E+0	43764E-0	2963E-0	1666E-0	6979E-0	20032E+0	9453E+0	88417E+0	12960E+0	5805E+0	8762E+0	2578E+0	7450E+0	34388E+U	20005
I/VISWANETH P., ISOCHOR 350, TCRT =	+	6 . 36	70.000	5°00	0000		מים מים		05.00	10.00	15,00	20.00	25.00	30.00	20000		79.29	96.35	04.13	11,35	18.45	22.49	70°48	32.44	33.12	10.00	20.00	30.00	00-05	20.00	80.00	00.06	00.00	05.00	10.00	15.00	20.00	20.00	1. =
SATVAPOR ) SESHADR 10) NBS V.F P = 66.3	3	0 0	0.0	0 0	0 0	000	9 0	9 =	02	0 5	0 8	13	18	1 to	2 0	5 5 5	75	85	8	92	95	96.	9 0		000	• 0 0	• 0 0	• 0 0	000	9 0		000	• 00	• 00	• 00	00.	000	•	Z Z
(11) (900 TTRE	c	1 d	43	43	43	t 3	0 M	) M	43	43	43	m 1	. t	5 to 2	2 t	<b>t</b> C	0		0	0	CD (	0 0	<b>&gt;</b> ~	4 +	910	-	11	# :	## T	4 +	4 +-	#	11	11	<del>-1</del> :		ed 4	-1 + -1 +	10

Table 4. Second Virial Coefficients.

NF3 SECOND VIRIAL COEFFICIENTS, EV = 3.00
(40) NBS/RDG APRIL, 1979.

·49382731 -1·30972686 -·38983811

IO	WT	T,K	X	B(T)	8*	CALC	DIF	PCT
40	1.000	200.00	.855	-210.00	-1.663	-1.6 €3	000	02
40	1.000	220.00	.940	-173.00	-1.370	-1.368	002	13
40	1.000	240.00	1.026	-144.00	-1.140	-1.144	- 004	•35
40	1.000	260.00	1.111	-122.00	966	969	.003	.30
40	1.000	280.00	1.197	-105.00	832	828	003	40
40	1.000	300.00	1.282	-91.00	721	713	008	-1.12
40	1.000	320.00	1.368	-77.00	610	616	.007	1.06

 $NP = 7 \cdot RMSPCT = .63$ 

Table 5. Comparisons With P-p-T Data for  $NF_3$ .

NF3 PVT DATA VS. EQNSTATE.
(1) NBS VIRIAL, (100+) NBS(1979), (26) BURNS(1975), (27) VANDERWALL(1977).

ID	PN	WT	T,K	MOL/L	CALCD	D.PCT	P.BAR	CALCD	P.PCT
1	1	.839	160.000	.2000	.2001	07	2.483	2.482	.06
1	2	.690	170.000	.2000	.2003	16	2.661	2.657	• 15
1	3	.610	180.000	-2000	.2005	23	2.837	2.831	.21
1	4	• 567	190.000	.2000	.2005	27	3.012	3.004	.26
1	5	.544	200.000	.2000	.2006	29	3.186	3.177	.28
1	6	• 534	210.000	.2000	.2006	30	3.359	3.350	• 29
1	7	.532	220.000	.2000	.2006	30	3.532	3.522	.29
1	8	•535	230.000	.2000	.2006	30	3.704	3.693	.29
1	9	.543	240.000	.2000	.2006	28	3.876	3.865	.28
1	10	.554	250.000	.2000	.2005	27	4.047	4.036	.25
1	11	•568	260.000	.2000	-2005	25	4.218	4.207	. 25
1	12	.584	270.000	.2000	.2005	23	4.388	4.378	.23
1	13	.601	280.000	.2000	.2004	21	4.559	4.549	.21
1	14	.620	290.000	.2000	.2004	19	4.729	4.720	•19
1	15	. 540	300.000	.2000	.2003	17	4.899	4.891	.17
1	16	.661	310.000	.2000	.2003	15	5.069	5.061	.15
1	17	.683	320.000	.2000	.2003	14	5.238	5.231	.13

NP = 17, DNRMSPCT = .228, PMEANDIF = .008, PMEANPCT = .210

Table 5. Continued.

NF3 PVT DATA VS. EQNSTATE. (1) NBS VIRIAL, (100+) NBS (1979), (26) BURNS (1975), (27) VANDERWALL (1977). P.PCT ID PN WT T.K MOL/L CALCD D.PCT P.BAR CALCD . 745 .5500 601 18 8.119 8.109 .13 200.000 .5508 -.14 602 19 .5491 -.16 9.117 9.104 .717 220.000 .14 •5499 603 20 .5480 .12 . 755 240.000 .5487 +.13 10.094 10.082 .5470 604 21 .793 260.000 .5475 -.09 11.059 11.049 .09 12.006 605 22 .846 280.000 .5460 .5463 -.05 12.012 .05 .5449 606 23 .920 -.01 12.955 12.954 .01 300.000 •5450 .959 320.000 .5438 .02 13.891 607 24 13.894 -.02 •5437 101 25 . 15 14.276 14.292 -.11 .689 200.000 1.0965 1.0948 102 -681 220.000 1.0944 1.0931 16.476 16.492 -.09 26 .12 1.0922 103 27 .655 240.000 1.0907 18.595 18.617 -.12 . 14 20.695 1.0901 1.0880 -.17 104 28 .610 260.000 .19 20.660 105 .569 -.23 29 280.000 1.0879 1.0852 . 25 22.686 22.737 .540 .30 -.28 106 30 300.000 1.0856 1.0824 24.682 24.751 107 31 .532 320.000 1.0833 1.0797 • 33 26.657 26.739 -.31 501 32 .03 20.718 -.02 .791 220.000 1.4742 1.4737 20.712 502 1.4712 1.4703 33 .727 240.000 . 06 23.733 23.745 -.05 503 34 . 662 260.000 1.4682 1.4663 26.654 26.682 -.11 .13 . 18 -.16 504 35 .625 280.000 1.4651 1.4625 29.511 29.557 300.000 505 36 •593 1.4620 1.4585 32.382 -.21 .24 32.314 506 37 .578 320.000 1.4587 1.4547 .27 35.077 35.165 -.25 24.950 201 38 . 786 220.000 1.9429 1.9422 . 04 24.944 -.02 29.187 202 39 .663 240.000 1.9388 1.9371 .09 29.205 -.06 203 33.252 33.295 40 .588 260.000 1.9346 1.9314 .17 -.13 1.9303 204 41 .548 280.000 1.9257 . 24 37.205 37.277 -.19 2.05 42 .522 300.000 1.9260 1.9202 .30 41.071 41.176 -.26 206 43 .513 320.000 1.9215 1.9150 . 34 44.873 45.008 -.30 301 44 .779 220.000 2.5761 2.5798 -. 14 29.113 29.093 .07 45 302 .928 240.000 2.5702 2.5746 -.17 35.239 35.202 .10 2.5643 303 260.000 40.995 46 .810 2.5653 -.04 41.007 .03 .06 304 47 .701 280.000 2.5582 2.5566 46.579 46.601 -.05 2.5521 2.5486 52.014 52.072 305 .656 48 300.000 . 14 -.11 306 49 .646 320.000 2.5457 2.5411 .18 57.345 57.434 -.15 901 50 .538 225.000 3.0616 3.0744 -.42 33.244 33.189 .17 902 51 .610 230.000 3.0598 3.0717 -.39 35.186 35.125 -18 903 52 .752 240.000 3.0561 3.0654 -.30 38.937 38.874 .16 904 53 .989 3.0488 -.17 260.000 3.0538 46.127 46.077 -11 905 54 .814 280.000 3.0413 .02 3.0423 -.03 53.039 53.026 906 55 .747 300.000 3.0336 3.0321 . 05 59.770 59.794 -.04 907 56 .732 320.000 3.0258 3.0226 .10 66.361 66.418 -.09 .315 701 57 3.7207 -1.04 37.918 .35 230.000 3.6818 37.787 702 58 .407 240.000 3.6772 3.7072 -.81 42.715 42.562 .36 703 59 .526 260.000 3.6680 3.6881 -.55 51.843 51.676 .32 280.000 .26 704 60 . 522 3.6585 3.6721 -.37 60.600 60.444 705 68.975 . 21 61 .662 300.000 3.6487 3.6589 -.28 69.120 706 62 .672 320.000 3.6388 3.6467 -. 22 77.453 77.317 .18 .241 .37 1602 63 235.000 4.7629 4.8418 -1.63 43.763 43.599 1603 64 .259 240.000 4.7597 4.8329 -1.51 47.112 46.895 . 46 1604 65 . 355 260.000 4.7468 4.7929 -.96 59.867 59.570 .50

Table 5. Continued.

NF3 PVT DATA VS. EQNSTATE.
(1) NBS VIRIAL, (100+) NBS (1979), (26) BURNS (1975), (27) VANDERWALL (1977).

ID	PN	WT	T,K	MOL/L	CALCO	D.PCT	P.BAR	CALCD	P,PCT
1605	66	.411	280.000	4.7336	4.7673	71	72.099	71.768	• 46
1606	67	• 438	300.000	4.7200	4.7472	57	84-003	83.645	•43
1607	68	• 438	320.000	4.7062	4.7303	51	95.665	95.267	. 42
						• • •	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	3,7000	
1701	69	.174	235.000	5.7980	5.9458	-2.49	45.213	45.093	.27
1702	70	.214	240.000	5.7940	5.9102	-1.97	49.522	49.320	.41
1703	71	. 285	250.000	5.7858	5.8636	-1.33	57.839	57.561	. 48
1704	72	.332	260.000	5.7774	5.8374	-1.03	65.955	65.631	. 49
1705	73	.377	280.000	5.7603	5.8048	77	81.823	81.418	.50
1706	74	-385	300.000	5.7427	5.7812	67	97.339	96.845	.51
1707	75	• 376	320.000	5.7249	5.7611	63	112-575	111.976	•53
1006	76	•183	235.000	5.8266	5.9673	-2.36	45.229	45.118	• 25
1007	77	.189	236.000	5.8258	5.9627	-2.30	46.111	45.978	• 29
1008	78	.198	237.000	5.8250	5.9545	-2.18	46.982	46.832	• 32
1009	79	• 206	238.000	5.8242	5.9480	-2.08	47.849	47.682	• 35
1010	80	• 223	240.000	5.8225	5.9343	-1.88	49.562	49.371	• 39
1801	81	.095	235.000	6.7709	7.1222	-4.93	45.705	45.617	.19
1802	82	. 224	240.000	6.7660	6.8920	-1.83	50.886	50.734	•30
1803	83	• 362	250.000	6.7561	6.8189	92	60.986	60.787	• 33
1804	84	.429	260.000	6.7459	6.7913	67	70.930	70.696	• 33
1805	85	. 448	280.000	6.7248	6.7615	54	90.535	90.196	.38
1806	86	. 424	300.000	6.7032	6.7391	53	109.823	109.342	.44
1807	87	• 396	320.000	6.6816	6.7185	55	128.827	128.179	•51
1106	88	.093	235.000	7.0723	7.4403	-4.95	45.767	45.694	•16
1107	89	• 145	236.000	7.0713	7.2935	-3.05	46.867	46.781	-18
1108	90	.189	237.000	7.0702	7.2334	-2.26	47.957	47.863	.20
1109	91	.227	238.000	7.0692	7.1989	-1.80	49.042	48.942	• 20
1110	92	.289	240-000	7.0672	7.1614	-1.32	51.200	51.092	.21
1901	93	. 228	235.000	7.8341	7.9658	-1.65	45.860	45.837	• 05
1902	94	. 468	240.000	7.8284	7.7900	. 49	51.924	51.969	09
1903	95	• 450	250.000	7.8165	7.7787	.49	64.054	64.180	20
1904	96	.518	260.000	7.8041	7.7772	. 35	76.170	76.320	20
1905	97	.792	280.000	7.7783	7.7718	.08	100.313	100.380	07
1906	98	.807	300.000	7.7521	7.7589	09	124.237	124.135	. 08
1907	99	.618	320.000	7.7265	7.7424	21	147.908	147.591	.21
1206	100	• 333	235.000	8.1094	8.0267	1.03	45.871	45.886	03
1207	101	• 255	236.000	8.1082	7.9928	1.44	47.124	47.168	09
1208	102	.234	237.000	8.1070	7.9810	1.58	48.377	48.450	15
1209	103	.230	238.000	8.1058	7.9784	1.60	49.633	49.732	20
1210	104	• 240	240.000	8.1034	7.9861	1.47	52.156	52.298	27
0.4.2	405	. 0.5	275 000	0 4470	0 0557	70	LC 977	45.888	02
812	105	• 405	235.000 240.000	8.1178	8.0553 7.9984	.78 1.42	45.877 52.171	52.308	26
813	106 107	• 247 • 300	250.000	8.0995	8.0208	• 98	64.869	65.139	41
815	108	.371	260.000	8.0865	8.0328	.67	77.616	77.926	40
019	100	•011	2001000	0 0 0 0 0 0	010020	* 01			3 7 0
2001	109	.116	235.000	8.8533	8.5174	3.94	45.964	46.036	16
2002	110	.135	240.000	8.8467	8.5847	3.05	52.900	53.250	66
2003	111	.185	250.000	8.8328	8.6693	1.89	67.181	67.802	92
2004	112	.235	260.000	8.8181	8.7049	1.30	81.664	82.387	88
2005	113	.348	280.000	8.7874	8.7271	.69	110.761	111.471	64

NF3 PVT DATA VS. EQNSTATE.
(1) NBS VIRIAL, (100+) NBS(1979), (26) BURNS(1975), (27) VANDERWALL(1977).

			1200111101		12070011		,		
ID	PN	нт	T.K	MOL/L	CALCD	D.PCT	P,BAR	CALCD	P,PCT
2006	114	.492	300.000	8.7566	8.7250	• 36	139.781	140.328	
2007	115	•659	320.000	8.7274	8.7123	•17	168.575	168-922	21
		0000	020000	00,2.1	34,120		1000	2000,22	~
1306	116	.075	235.000	9.1988	8.6529	6.31	45.991	46.131	30
1307	117	.085	236.000	9.1974	8.7270	5.39	47.415	47.642	48
1308	118	. 094	237.000	9.1961	8.7763	4.78	48.861	49.162	61
1309	119	.101	238.000	9.1947	8.8138	4.32	50.322	50.687	72
1310	120	.115	240.000	9.1919	8.8683	3.65	53.280	53.748	87
2101	121	.093	235.000	9.8670	9-4001	4.97	46.201	46.433	50
2102	122	•113	240.000	9.8594	9.5120	3.65	54.265	54.911	-1.18
2103	123	• 154	250.000	9.8431	9.6230	2.29	71.122	72 • 176	-1.46
2104	124	•185	260.000	9.8257	9.6618	1.70	88.303	89.590	-1.44
2105	125	. 254	280.000	9.7896	9.6893	1.04	123.064	124.487	-1.14
2106	126	.320	300.000	9.7545	9.6867	.70	157.853	159.254	88
2107	127	.378	320.000	9.7225	9.6734	•51	192.477	193.815	69
1406	128	.102		10.1860	9.7594	4.37	46.369	46.677	
1407	129	-107	236.000	10.1845	9.7836	4.10	48.040	48.445	
1408	130	•109	237.000	10.1829	9.7948	3.96	49.721	50.225	-1.00
1409	131	•113		10.1813	9.8158	3.72	51.431	52.013	-1.12
1410	132	.122	240.080	10.1781	9.8517	3.31	54.895	55.611	-1.29
2201	133	•169		10.8444		2.30	47.155	47.551	83
2505	134	•178		10.8355		2.04	56.817	57.540	-1.26
2203	135	.221		10.8162		1.41	76.900	77.940	-1.33
2204	136	. 276		10.7956		1.00	97.443	98.578	-1.15
2205	137	• 392		10.7536		• 55	138.974	140.049	77
2206	138	•507		10.7147		• 32	180.597	181.489	49
2207	139	•600	320.000	10.6808	10.6598	• 20	222.095	222.798	32
0700		74.0				~-			
2302	140	• 342		11.9859		• 75	50.886	51.342	89
2303	141	. 360		11.9749		.70	62.985	63.600	97
2304	142	. 441		11.9512		• 52	87.811	88.542	83
2305	143	•538		11.9263		• 37	113.040	113.755	- 63
2306	144	•702		11.8777		•19	163.880 214.798	164.450	35
2307 2308	145 146	•772 •742		11.8362 11.8013		•11 •08	265.560	215.240	21 16
2300	140	• 1 4 4	320.000	11.0013	11.4919	• 00	200,000	200.990	- 10
2502	147	.861	230.000	13.2274	13.21/.8	•10	46.808	46.937	27
2503	148	.917		13.2141		.08	62.040	62.176	22
2504	149	.758		13.2000		-04	77.517	77.600	11
2505	150	•653		13.1701		01	108.794	108.752	• 04
2506	151	•625		13.1402		05	140.289	140.109	•13
2507	152	•686		13.0874		06	203.455	203.144	•15
2508	153	.886		13.0455		02	266.595	266.433	.06
		• • • • •		2000 177	2000401	• • •	20000	2000 100	
2401	154	•510	225.000	14.2667	14.2796	09	44.567	44.336	•52
2402	155	.424		14.2510		14	63.201	62.767	•69
2403	156	.408		14.2166		17	100.744	100.030	•71
2404	157	.417		14.1813		19	138.506	137.541	.70
2405	158	-450		14.1490		18	176.323	175.220	• 63
2406	159	.503	270.000			16	214-187	213.061	•53
2407	160	•590	280.000	14.0968	14.1141	12	252.025	251.038	• 39
2408	161	.720	290.000	14.0755	14.0868	08	289.818	289.095	• 25

NF3 PVT DATA VS. EQNSTATE.
(1) NBS VIRIAL, (100+) NBS (1979), (26) BURNS (1975), (27) VANDERWALL (1977).

ID	PN	WT	T,K	MOL/L	CALCD	D.PCT	P,BAR	CALCD	P,PCT
2602	162	.488	220.000	15.2155	15.2259	07	45.983	45.683	•66
2603	163	. 405	225.000	15.1969		12	68.294	67.680	.91
2604	164	.402	230.000	15.1770					
	_					14	90.556	89.757	.89
2605	165	•412	240.000		15.1606	16	135.155	134.019	.85
2606	166	. 454	250.000	15.0989	15.1223	15	179.742	178.462	•72
2607	167	•530	260.000	15.0677	15.0869	13	224.367	223.158	•54
2608	168	. 664	270.000	15.0415	15.0541	08	268.965	268.074	.33
2609	169	.914	280.000		15.0230	03	313.449	313.116	.11
				1740101	1740200		0100447	0100110	0.2.2
2701	170	.856	240 000	46 2775	46 2777	- 0.0	74 606	74 500	0.2
			210.000		16.2337	00	31.606	31.599	• 0 2
2702	171	.469	215.000		16.2222	06	58.512	58.060	.78
2703	172	• 500	215.000		16.2209	05	58.448	58.062	• 66
2704	173	• 443	220.000	16.1898	16.2035	08	85.232	84.510	- 85
2705	174	. 438	225.000	16.1658	16.1825	10	111.886	110.924	.87
2706	175	•453	230.000		16.1600	11	138.448	137.330	.81
2707	176	.514	240.000	16.1000		10	191.559	190.338	.64
2708	177	.640	250.000						
				16.0663		07	244.729	243.756	. 40
2709	178	• 916	260.000	16.0387	16.0422	02	297.816	297.496	.11
2801	179	. 130	200.000	17.4218	17.3894	-19	31.480	33.640	-6.42
2802	180	.670	205.000	17.3954	17.3901	.03	66.075	66.459	58
2803	181	.953	210.000		17.3662	.00	99.016	99.081	06
2804	182	.824	215.000		17.3399	01	131.690	131.554	.10
2805	183	• 8 31	220.000		17.3136	01	164.255	164.056	.12
2806	184	.883		17.2878		01	196.897	196.720	.09
2807	185	.973	230.000	17.2674	17.2671	.00	229.561	229.587	01
2808	186	.801	235.000	17.2496	17.2459	.02	262.222	262.634	16
2809	187	.664	240.000	17.2338	17.2255	. 05	294.843	295.812	33
		•••		2.0200	2. 00000				
2901	188	. 453	190.000	18.5460	4.9 5/.00	.03	49.777	50.391	-1.22
2902	189	.733	194.000		18.5171	• 02	82.053	82.376	39
2903	190	• 962	200.000		18.4790	00	129.824	129.807	.01
2904	191	.907	205.000		18.4484	01	169.481	169.320	.10
2905	192	.992	210.000	18 - 4200	18.4207	00	209.251	209.169	• 0 4
2906	193	. 834	215.000	18.3975	18.3956	.01	249.137	249.407	11
2907	194	.681	220.000	18.3784		• 03	289.058	289.938	30
	-, .								
3001	195	440	476 000	19.4280	40 /.460	.06	17.750	19.171	-7.41
		-118							
3002	196	• 339	180.000	19.4013		• 04	55.751	56.830	-1.90
3003	197	• 567	184.000	19.3709	19.3661	.02	93.066	93.743	72
3004	198	.720	188.000	19.3395	19.3364	. 02	129.796	130.245	34
3005	199	.603	192.000	19.3107	19.3046	.03	165.910	166.845	• 56
3006	200	.627	196-000	19.2854	19.2794	.03	202.775	203.742	47
3007	201	• 596	200.000			. 04	239.813	241.067	52
3008	202	•603		19.2418		.04	286.807	288.164	47
3000	202	• 6 0 3	203.000	13.5410	1305341	. 0 4	200.007	200.104	- 0 - 7 /
							47 670	40 460	7 74
3101	203	.113			20.6327	.04	17.679	19.162	-7.74
3102	204	.375		20.6080		.03	64.347	65.395	-1.60
3103	205	.543	168.000	20.5707	20.5665	.02	109.477	110.323	77
3104	206	.646		20.5342		.02	154.178	154.894	46
3105	207	.691		20.5028		.02	199.376	200.065	34
		.637		20.4773		.02	245.058	246.126	43
3106	208								
3107	209	• 556	184.000	20.4564	<0.4460	. 04	291.075	292.877	62
3201	210	.222		21.7506		.01	20.326	21.059	-3.48
3202	211	.524	148.000	21.7109	21.7083	.01	75.762	76.421	86

Table 5. Continued.

NF3 PVT DATA VS. EQNSTATE.
(1) NBS VIRIAL, (100+) NBS (1979), (26) BURNS (1975), (27) VANDERWALL (1977).

1D 3203 3204 3205 3206	PN 212 213 214 215	WT •772 •777 •796 •637	T,K 152.000 156.000 160.000 164.000	21.5942	CALCD 21.6652 21.6280 21.5928 21.5648	0.PCT .01 .01 .01	P,8AR 129.502 184.095 238.550 294.473	CALCD 1 29 • 818 184 • 495 238 • 958 295 • 777	P,PCT24221744
3301 3302 3303 3304 3305 3306 3307	216 217 218 219 220 221 222	.282 .646 .659 .654 .640 .688	124.000 128.000 130.000 132.000 134.000 136.000 138.000	22.9620 22.9351 22.9090 22.8853 22.8649 22.8474	22.9112 22.8881 22.8675 22.8492	00 01 01 01 01 01	15.792 83.605 116.223 148.828 182.078 215.960 250.446	15.402 83.156 115.629 148.048 181.060 214.971 249.765	2.53 .54 .51 .53 .56 .46
3308 3401 3402 3403 3404 3405 3406 3407	223 224 225 226 227 228 229 230	.997 .439 .554 .782 .946 .822 .895	140.000 108.000 110.000 112.000 114.000 116.000 120.000	24.0635 24.0333 24.0018 23.9724 23.9470 23.9259	22.8326 24.0620 24.0316 24.0010 23.9725 23.9478 23.9264 23.9073	00 .01 .00 00 00 00	285.347 52.250 91.280 129.716 168.714 209.069 250.608 292.951	285.241 52.943 92.041 130.110 168.663 208.673 250.359 293.350	-1.31 83 30 .03 .19 .10
3501 3502 3503 3504 3505 3506 3507	231 232 233 234 235 236 237	.174 .418 .930 .566 .502 .515	90.000 92.000 94.000 96.000 98.000 100.000	25.0055 24.9696 24.9344 24.9040	25.0362 25.0038 24.9693 24.9361 24.9070 24.8827 24.8617	.01 .00 01 01 01	21.866 68.766 113.787 158.957 205.933 255.263 306.123	22.976 69.788 113.964 157.891 204.107 253.125 304.360	-4.83 -1.47 16 .68 .89 .84

NP = 220, DNRMSPCT = .721, PMEANDIF = .405, PMEANPCT = .372

Table 5. Continued.

NF3 PVT DATA VS. EQNSTATE.

(1) NBS VIRIAL, (100+) NBS (1979), (26) BURNS (1975), (27) VANDERWALL (1977). ID PN WT P.PCT T.K MOL/L CALCD D.PCT P.BAR CALCD 26 238 1.000 273.150 1.0663 1.0567 .90 21.464 21.637 -.80 22-180 26 239 1.000 282.150 1.0663 1.0470 1.84 22.548 -1.63 299.150 1.0663 1.0407 2.46 26 240 23.725 1.000 24.260 -2.21 26 241 1.000 319.350 1.0663 1.0414 2.39 25.710 26.282 -2.18 . 47 27 242 1.000 273.150 1.6887 1.6983 -.56 32.336 32.185 27 243 1.000 294.250 1.6887 1.6735 . 91 35.508 35.788 -.78 27 244 1.000 321-150 1-6887 .16 1.6861 40.265 40.322 -.14 344.150 27 245 1.000 .94 1.6887 1.6730 43.782 44.160 -.86 26 246 1.000 273.150 2.3661 2.4174 -2.12 42.810 42.117 1.64 . 22 2.3609 26 247 1.000 282.650 2.3661 44.471 44.549 -.18 26 248 1.000 300.250 2.3505 48.739 -.55 2.3661 .67 49.007 26 249 1.000 319.350 2.3661 2.3381 1.20 53.241 53.789 -1.02 -.51 27 250 1.000 273.150 2.9651 2.9802 49.918 49.738 • 36 27 251 1.000 295.150 2.9651 2.9540 . 37 56.951 57.117 -.29 252 1.000 324.650 2.9651 2.9825 27 -.58 67.155 66.825 .49 . 81 -.71 27 253 1.000 344.250 2.9651 2.9412 72.671 73.188 26 254 1.000 273.150 3.3225 3.4557 -3.86 55.296 53.841 2.70 284.150 3.3225 3.3846 -1.84 26 255 1.000 58.895 58.111 1.35 3.3660 -1.29 26 256 1.000 298.950 3.3225 64.432 63.790 1.01 319.150 3.3225 -.20 257 1.000 3.3291 71.561 71.444 .16 26 3.7558 3.7997 .76 27 258 1.000 273.150 -1.15 58.881 58.436 27 259 1.000 292.850 3.7558 3.7433 .33 67.155 67.319 -.24 27 260 1.000 324.250 3.7558 3.7414 .38 80.944 81.200 -.31 1.000 4.5272 -3.08 65.776 27 261 273.150 4.3876 64.516 1.95 1.000 27 262 292.150 4.3876 4.4829 -2.13 76.118 74.961 1.54 27 263 1.000 323.950 4.3876 4.4595 -1.61 93.355 92.116 1.35 4.4287 -.93 103.697 27 264 4.3876 102.858 . 82 1.000 344.150 265 4.5272 -1.24 65.776 65.273 .77 27 1.000 273.150 4.4712 76.877 27 266 1.000 295.150 4.4712 4.4098 1.39 77.650 -1.00 27 267 323.550 .79 1.000 4.4712 4.4361 92.734 93.336 - . 64 4.4051 1.50 103.215 104.565 -1.29 27 268 1.000 344.150 4.4712 6.3954 -.80 80.944 80.548 . 49 269 1.000 273.150 6.3442 27 291.550 6.3442 6.2783 1.05 96.320 97.068 27 270 1.000 -.77 271 318.650 6.3442 6.2899 .86 120.245 121.155 -.75 27 1.000 344.250 6.3442 6.2833 .97 142.377 143.709 -.93 27 272 1.000 2.48 128.656 131.590 27 273 326.150 6.5508 6.3920 -2.23 1.000 344.250 6.5508 6.4277 1.91 145.548 27 274 1.000 148.283 -1.84 .05 27 275 1.000 273.150 8.8026 8.8078 -.06 101.629 101.576 1.000 292.450 8.8026 8.6875 1.33 128.242 129.993 -1.35 27 276 .98 154.374 -1.11 8.8026 8.7168 156.112 27 277 1.000 310.150 27 278 1.000 316.650 8.8026 8.6951 1.24 163.337 165.710 -1.43 1.61 202.292 -2.02 279 344.250 8.8026 8.6630 206.473 27 1.000 1.13 138.929 141.562 -1.86 273.150 11.6398 11.5100 27 280 1.000 281 1.000 283.450 11.6398 11.4328 1.81 162.027 167.130 -3.05 27 1.81 2.04 -3.47 27 282 1.000 288.150 11.6398 11.4069 172.645 178.855 293.150 11.6398 11.3728 191.364 -4.02 2.35 183.676 27 283 1.000 46. DNRMSPCT = 1.515. PMEANDIF = 1.254, PMEANPCT = 1.208 NP = 237, DNRMSPCT = .693, PMEANDIF = .372, PMEANPCT = .358

Table 6. Coefficients of the Equation of State.

EQUATION OF STATE, COEFFICIENTS DGAT = .336118520E-06. TBLP = 144.0935 DGBP = .878210055E-01, DLBP = 21.6617DTRP = 26.3200, TTRP = 66.350, PTRP = .185425421E-05 DCRT = 7.9200, TCRT = 234.000, PCRT = 44.607130324 DPS/DTB = .70882E-01, QVAPB, KJ/MOL = 11.583 IX = 1, ER = 0.000AL = 1.00000000, BE = 0.00000000, GA = 1.00000000 $DE = .50000000 \cdot EP = 1.00000000$ B1 = .55199813920, B2 = .13268809584, B3 = .20608495802C1 = .74067409894, C2 = .29375371520, C3 = 0.000000000000MOL/L TSAT THETA PSAT В C 1.0 194.018 -.59895 183.967 12.719 .5720 .5986 2.0 212.116 205.168 23.561 - . 47316 3.0 221.972 217.769 31.741 -. 36236 .6318 4.0 227.832 225.639 37.549 .6716 -. 26555 5.0 231.310 230.387 41.392 .7179 6.0 233.188 232.923 43.610 .7708 7.0 233.913 233.884 44.499 .8303 .8963 8.0 234.000 234.000 44.607 .9689 9.0 233.930 233.882 44.520 10.0 233.503 43.994 233.166 1.0481 11.0 232.416 231.328 42.685 1.1338

#### TABLE 7. Calculated P(p) Critical Isotherm

The following page gives a high-resolution examination of the critical isotherm as computed by equation of state (6). Column headings have the following interpretations—

D/DC  $\equiv$  d/d<sub>C</sub>, density reduced at the critical point. TS/TC  $\equiv$  T<sub>o</sub>( $\rho$ )/T<sub>c</sub>, reduced coexistence temperature. PS/PC  $\equiv$  P<sub>o</sub>( $\rho$ )/P<sub>c</sub>, reduced coexistence pressure. P/PC  $\equiv$  P/P<sub>c</sub>, pressure reduced at the critical point. DP/DR  $\equiv$   $\partial P/\partial \rho$  slope of the critical isotherm, bar.

The last five columns give the density-dependence of functions used in the equation of state, where R  $\equiv$   $\rho$   $\equiv$  d/d $_t$  is density reduced at the liquid triple point--

DTS/DR  $\equiv$   $dT_{\sigma}(\rho)/d\rho$ , K. DTH/DR  $\equiv$   $d(\rho)/d\rho$ , K. DPS/DR  $\equiv$   $dP_{\sigma}(\rho)/d\rho$ , bar. DXB/DR  $\equiv$   $\partial(\rho,T)/\partial\rho$ . DXC/DR  $\equiv$   $\partial(\rho,T)/\partial\rho$ .

<sup>\*</sup>Note:  $\rho \equiv d/d_t$ , density reduced at the liquid triple-point.

THE CRITICAL ISOTHERM

Table 8. Comparisons With Ideal Gas Functions.

	PCNT	00	000		02	000		00.	000-			00.		000		- 000	000-
	CALCD	34.04	42.78	3.3	8	1.8	7.5	1.4	4.0	5.9	7.3	8.3	9.1	6	80.22	0.6	0.9
		4.0	42.78	3.3	3.5	1.8	7.5	1.04	4.0	5.9	7.3	8.3	9.1	9.7	0.2	0.6	0.9
	PCNT	00.	• 00	.01	00.00	00.	00	00.	• 0 0	000	- 000	00.	• <b>0</b> 0		00 • -		
GAS FUNCTIONS, JOULES, MOLES, KELVINS	CALCD	15.6	S	60.6	260.990	77.6	92 . 0	04.7	15.9	25.9	35.0	43.2	50.7	57.6	64.0	70.0	75.5
JOULE S, MOL		15.68	r.	60 ° 65	66°09	77.6	95 ° 06	04.74	15.96	25.99	35.02	43.22	50.73	S	64.04	70.00	<b>~</b>
CTIONS,	PCNT	- 06	- 04	.05	000	- 00	00 -	- 00	00	01	- 000		- 00	00 • -	000		
AL	CALCD	3336.7	-	184	11949.5	77440	423	1196.	8480.	5988.	365	144	9321.	72	5265	3307.	1384.
NF3 IDE	ZH-Z	334.	7117.0	1849.	949.	7744.	4233.	1195.	8480.	5986.	3655.	1442.	9320.	7265.	5265.	3307.	82.
	₩.	0000	200.00	98.0	0000	0000	0000	0000	0.00	0000	0000	0000	100.0	0000	300.0	40000	500.0

Table 9. Interpolated Ideal Gas Functions.

#### NF3 IDEAL GAS FUNCTIONS, JOULES, MOLES, KELVINS

T • K	EZ-EZZ	HZ-HZZ	SZ	CVZ	CPZ
50.0	1247.6	1663.3	192.512	24.95	33.26
60.0	1497.1	1996.0	198.576	24.96	33.27
70.0	1746.9	2328.9	203.708	25.01	33.32
80.0	1997.5	2662.7	208.165	25.14	33.45
90.0	2249.9	2998.2	212.117	25.37	33.68
100.0	2505.3	3336.7	215.683	25.72	34.04
110.0	2764.8	3679.4	218.948	26.21	34.52
120.0	3029.8	4027.6	221.977	26.81	35.13
130.0	3301.4	4382.3	224.816	27.53	35.84
140.0	3580.7	4744.7	227.502	28.34	36.65
150.0	3868.5	5115.7	230.060	29.23	37.55
160.0	4165.6	5495.9	232.514	30.19	38.51
170.0	4472.5	5886.0	234.879	31.21	39.52
180.0	4789.9	6286.5	237.167	32.26	40.58
190.0	5117.9 5457.0	6697.7 7119.9	239.390 241.556	33.35	41.67 42.78
210.0	5807.2	7553.2	243 • 670	34.46 35.58	43.90
220.0	61 68 • 6	7997.8	245.738	36.71	45.02
230.0	6541.4	8453.7	247.764	37.83	46.15
240.0	6925.3	8920.7	249.752	38.95	47.26
250.0	7320.3	9398.9	251.703	40.05	48.36
260.0	7726.2	9888.0	253.621	41.13	49.45
270.0	8142.9	10387.8	255.508	42.20	50.51
280.0	8570.1	10898.2	257.364	43.24	51.56
290.0	9007.6	11418.8	259.191	44.26	52.57
300.0	9455.2	11949.5	260.990	45.25	53.56
310.0	9912.4	12489.9	262.762	46.21	54.52
320.0	10379.2	13039.8	264.507	47.14	55.45
330.0	10855.1	13598.9	266.228	48.04	56.36
340.0	11339.9	14166.9	267.923	48.91	57.23
350.0	11833.3	14743.4	269.594	49.76	58.07
360.0	12335.0	15328.2	271.242	50.57	58.89
370.0	12844.6	15921.0	272.866	51.36	59.67
380.0	13362.0	16521.5	274.467	52.11	60.43
390.0	13886.8	17129.5	276.046	52.84	61.16
400.0	14418.8	17744.6	277.604	53.54	61.86
420.0	14957.6 15503.1	18366.6 18995.2	279.139 280.654	54.22 54.87	62.54
430.0	16055.0	19630-2	282.148	55.50	63.81
440.0	16613.0	20271.3	283.622	56.10	64.41
450.0	17176.8	20918.4	285.076	56.68	64.99
460.0	17746.4	21571.1	286.511	57.23	65.55
470.0	18321.4	22229.2	287.926	57.77	66.08
480.0	18901.6	22892.6	289.323	58.28	66.59
490.0	19486.9	23561.0	290.701	58.77	67.09
500.0	20077.1	24234.3	292.061	59.25	67.56
510.0	20671.9	24912.3	293.404	59.71	68.02
520.0	21271.1	25594.7	294.729	60.15	68.46
530.0	21874.7	26281.4	296.037	60.57	68.88
540.0	22482.4	26972.3	297.328	60.98	69.29
550.0	23094.2	27667.1	298.633	61.37	69.68
560.0	23709.7	28365.8	299 • 862	61.74	70.06
570.0	24329.0	29068.2	301.106	62.11	70.42
580.0	24951.8	29774.2	302.333	62.45	70.77
590.0 600.0	25578.0 26207.6	30483.6 31196.3	303.546 304.744	62.79 63.11	71.11 71.43
00000	2020100	2113003	3070144	0.20 II	1 T 9 42

Table 10. The Heats of Vaporization.

NF3 QVAP, NF = 3, E = .380, QT = 14.548

(23) AEROJET, (39) THERMALOOPS, (40) CLAPEYRON.

	9982471		269536103E		L0672E+00	
Û.		0 (		0 •		
ID	WT	T,K	KJ/MOL	CALC	PCNT	RESID.
39	1.000	66.360	14.548	14.548	.09	•1613E+01
39	• 989	70.000	14.406	14.402	• 0 3	.8935E+00
39	. 974	75.000	14.213	14.207	. 04	.9022E+00
39	• 95 8	80.000	14.021	14.017	• 03	•9100E+00
39	. 943	85.000	13.832	13.830	.02	.9200E+00
39	• 927	90.000	13.645	13.646	01	•9302E+00
39 39	•911 •894	95.000 100.000	13.461	13.464	02	.9415E+00
39	. 377	105.000	13.278 13.096	13.283 13.102	03 04	•9523E+00
39	.860	110.000	12.914	12.920	04	.9735E+00
39	.843	115.000	12.731	12.736	04	.9835E+00
39	. 825	120.000	12.546	12.549	03	.9930E+00
39	. 806	125.000	12.358	12.359	01	.1002E+01
39	.788	130.000	12.165	12.164	.01	.1010E+01
39	.768	135.000	11.967	11.963	.04	.1018E+01
39	.749	140.000	11.761	11.754	. 06	.1024E+01
40	1.000	66.350	14.548	14.548	.00	0 •
40	.989	70.000	14.487	14.402	.03	.9000E+00
40	.974	75.000	14.214	14.207	• 05	.9051E+00
40	• 95 8	80.000	14.022	14.017	. 04	•9120E+00
40	. 943	85.000	13.832	13.830	. 02	•9205E+00
40	• 927	90.000	13.645	13.646	01	•9303E+00
40	. 911	95.000	13.460	13.464	03	.9409E+00
40	·894	100.000	13.278	13.283	04	•9522E+00
40	. 877	105.000	13.097	13.102	03 02	.9636E+00
40	.860 .843	110.000 115.000	12.917 12.736	12.920 12.736	00	•9854E+00
40	.825	120.000	12.552	12.730	• 02	•9952E+00
40	.806	125.000	12.364	12.359	. 04	.1004E+01
40	. 788	130.000	12.171	12.164	. 06	.1012E+01
40	. 768	135.000	11.970	11.963	. 06	.1018E+01
40	.749	140.000	11.761	11.754	. 06	.1024E+01
40	.729	145.000	11.543	11.538	• 04	.1029E+01
40	.708	150.000	11.314	11.311	.02	.1032E+01
40	.686	155.000	11.073	11.074	01	.1035E+01
40	. 664	160.000	10.821	10.824	04	•1037E+01
40	•642	165.000	10.554	10.561	06	•1039E+01
40	_	170.000	10.273	10.281	08	.1040E+01
40	• 593	175.000	9.975	9.983	08	-1041E+01
40	•563	180.000	9.657 9.318	9.664 9.322	07 05	•1042E+01 •1041E+01
40	•541 •512	185.000 190.000	8.952	8.953	01	•1041E+01
40	. 482	195.000	8.556	8.553	. 04	.1040E+01
40	. 450	200.000	8.122	8.115	. 09	.1038E+01
40	. 416	205.000	7.640	7.631	• 13	.1035E+01
40	• 378	210.000	7.099	7.089	.13	.1030E+01
40	.337	215.000	6.476	6.471	. 08	.1025E+01
40	.289	220.000	5.739	5.743	07	.1017E+01
40	•232	225.0 CO	4.818	4.834	33	.1008E+01
40	. 154	230.000	3.521	3.532	32	•1001E+01
40	0.000	234.000	0.000	0.000	0.00	û •

Table 10. Continued.

NF3	QVAP,	NF = 3, $E =$	.380, QT	= 14.548		
ID	WT	Ť•K	KJ/MOL	CALC	PCNT	RESID.
		•				
23	0.000	70.000	14.469	14.402	• 46	.1216E+01
23	0.000	80.000	14.137	14.017	• 86	.1070E+01
23	0.000	90.000	13.790	13.646	1.06	-1048E+01
23	0.000	100.000	13.429	13.283	1.10	•1039E+01
23	0.000	110.000	13.049	12.920	1.00	•1035E+01
23	0.000	120.000	12.651	12.549	.81	•1032E+01
23	0.000	130.000	12.229	12.164	• 54	.1031E+01
23	0.000	140.000	11.782	11.754	• 23	•1030E+01
23	0.000	150.000	11.303	11.311	08	•1029E+01
23	0.000	160.000	10.787	10.824	35	.1029E+01
23	0.000	170.000	10.225	10.281	54	.1030E+01
23	0.000	180.000	9.605	9.664	61	•1031E+01
23	0.000	190.000	8.908	8.953	51	.1032E+01
23	0.000	200.000	8.102	8.115	16	•1034E+01
23	0.000	210.000	7.129	7.089	• 56	•1037E+01
23	0.000	220.000	5.850	5.743	1.86	.1042E+01
23	0.000	230.000	3.699	3.532	4.73	•1057E+01
NP	= 50,	RMSPCT =	• 0 5			

#### TABLE 11. Calculated P(T) Isochores

The following pages give P(T) along isochores, as computed by the equation of state. The third column DP/DD is the isotherm slope ( $\partial P/\partial \rho$ ) in units of the bar and mol/L. The last two columns give the isochore slopes and curvatures  $\partial P/\partial T$ ,  $\partial^2 P/\partial T^2$ , in units of the bar and K.

These tables show that the isochore curvatures are qualitatively consistent with a maximum in the specific heat  $C_V(\rho,T)$  at the critical point.

Table 11. Calculated P(T) Isochores.

	NF3 IS	CHORE AT	.500 MOL/	L	
T , K	P,BAR	Z	OP/DO	OP/OT	D2P/DT2
177.084	6.388	.86770	10.916	.0473	000113
180.000	6.525	.87200	11.233	.0470	000092
188.000	6.898	.88264	12.077	- 0464	000060
196.000	7.268	.89193	12.899	.0460	000844
204.000	7.634	.90015	13.706	.0456	000034
212.000	7.998	•90750	14.502	.0454	000028
220.000	8.360	.91412	15.289	.0452	000023
228.000	8.721	.92012	16.070	• 0450	000019
236.000	9.081	• 92558	16.845	.0449	000617
244.000	9.440	.93059	17.615	• 0448	00 00 14
252.000	9.797	.93518	18.381	.0447	00 0013
260.000	10.154	•93942 •94334	19.143	• 0446	000011
268.000 276.000	10.510	.94534	19.902	.0445	000010
284.000	10.866 11.220	• 95036	20.659 21.412	.0444	000009
292.000	11.575	.95351	22.164	.0443	000008
300.000	11.929	•95645	22.913	0442	000007
308.000	12.282	• 95920	23.661	.0442	000007
316.000	12.635	.96179	24.407	.0441	000006
324.000	12.987	.96421	25.151	. 0440	000006
332.000	13.340	• 96 65 0	25.894	.0440	000005
340.000	13.691	.96865	26.635	.0440	000005
348.000	14.043	.97068	27.375	.0439	000005
356.000	14.394	.97259	28.113	.0439	000004
364.000	14.745	.97441	28.851	. 0438	000004
372.000	15.096	.97613	29.587	.0438	000004
380.000	15.446	.97776	30.323	.0438	000004
388.000	15.796	.97931	31.057	.0438	0000004
396.000	16.146	.98078	31.791	• 0437	000003
404.000	16.496	•98218	32.523	• 0437	000003
412.000	16.845	.98351	33.255	.0437	000003
420.000	17.195	.98478	33.986	.0436	000003
428.000	17.544	• 98599	34.716	• 0436	000003
436.000	17.893	-98715	35.445	.0436	000003
444.000	18.241	.98825	36.174	• 0436	000003
452.000	18.590	.98931	36.902	.0436	000003
460.000 468.000	18.938 19.286	.99032	37.629	.0435 .0435	000003 000002
476.000	19.634	.99129 .99222	38.356 39.082	• 0435 • 0435	000002
484.000	19.982	.99311	39.808	.0435	000002
492.000	20.330	•99396	40.533	.0435	000002
500.000	20.678	•99478	41.257	.0434	000002
		0 7 7 7 1 0	121271	9 9 10 1	1 00000



Table 11. Calculated P(T) Isochores.

	NF3 IS	OCHORE AT	.500 MOL/	L	
T » K	P.BAR	Z	OP/00	DP/DT	02P/0T2
177.084	6.388	.86770	10.916	.0473	000113
180.000	6.525	.87200	11.233	.0470	000092
188.000	6.898	.88264	12.077	.0464	000060
196.000	7.268	.89193	12.899	.0460	000044
204.000	7.634	.90015	13.706	.0456	000034
212.000	7.034	•90750	14.502	.0454	000034
220.000	8.360	.91412	15.289	.0452	000023
228.000	8.721	•92012	16.070	• 0450	000019
236.000	9.081	.92558	16.845	. 8449	800017
244.000	9.440	.93059	17.615	.0448	000014
252.000	9.797	.93518	18.381	.0447	000013
260.000	10.154	.93942	19.143	0446	000011
268.000	10.510	.94334	19.902	.0445	000010
276.000	10.866	.94698	20.659	.0444	000009
284.000	11.220	.95036	21.412	.0443	000008
292.000	11.575	.95351	22.164	.0443	000008
300.000	11.929	.95645	22.913	.0442	000007
308.000	12.282	.95920	23.661	.0441	000007
316.000	12.635	.96179	24.407	.0441	000006
324.000	12.987	.96421	25.151	.0440	000006
332.000	13.340	.96650	25.894	.0440	000005
340.000	13.691	.96865	26.635	.0440	000005
348.000	14.043	.97068	27.375	.0439	000005
356.000	14.394	•97259	28.113	.0439	000004
364.000	14.745	.97441	28.851	.0438	000004
372.000	15.096	.97613	29.587	.0438	000004
380.000	15.446	.97776	30.323	.0438	000004
388.000	15.796	.97931	31.057	.0438	000004
396.000	16.146	.98078	31.791	.0437	000003
404.000	16.496	.98218	32.523	• 0437	000003
412.000	16.845	.98351	33.255	.0437	000003
420.000	17.195	.98478	33.986	.0436	000003
428.000	17.544	•98599	34.716	• 0436	000003
436.000	17.893	•98715	35.445	.0436	000003
444.000	18.241	.98825	36.174	.0436	000003
452.000	18.590	•98931	36.902	.0436	000003
460.000	18.938	.99032	37.629	.0435	000003
468.000	19.286	.99129	38.356	. 0435	000002
476.000	19.634	•99222	39.082	• 0435	000002
484.000	19.982	.99311	39.808	.0435	000002
492.000	20.330	• 99396	40.533	.0435	000002
500.000	20.678	• 99478	41.257	. 0434	000002

Table 11. Continued.

### NF3 ISOCHORE AT 1.000 MOL/L

T. K	P.BAR	Z	DP/00	DP/DT	02P/0T2
194.018	12.719	.78847	9.474	.1036	000398
196.000	12.924	.79305	9.731	.1029	000341
204.000	13.738	.80992	10.723	.1007	- 000216
212.000	14.537	.82472	11.673	-0993	000156
220.000	15.327	.83789	12.595	.0982	000121
228.000	16.108	.84972	13.498	.0973	- 000097
236.000	16.884	86044	14.386	.0966	- 000081
244.000	17.654	87019	15.262	.0960	000068
252.000	18.420	.87911	16.128	.0955	000059
260.000	19.182	.88731	16.986	.0950	000051
268.000	19.940	.89487	17.837	0947	000045
276.000	20.696	.90187	18.681	.0943	000040
284.000	21.449	90837	19.520	. 0940	000036
292.000	22.200	.91441	20.354	.0937	000033
300.000	22.949	.92004	21.184	. 0935	~ . 000030
308.000	23.696	. 92531	22.009	.0932	000028
316.000	24.441	.93024	22.832	.0930	000025
324.000	25.185	.93487	23.650	. 0928	000023
332.000	25.927	.93923	24.466	.0927	000022
340.000	26.667	.94332	25.279	.0925	000020
348.000	27.496	.94719	26.090	.0923	000019
356.000	28.144	.95084	26.898	.0922	00 00 18
364.000	28.881	.95429	27.704	.0920	000017
372.000	29.617	.95755	28.508	.0919	000016
380.000	30.352	. 96065	29.309	.0918	000015
388.000	31.086	.96359	30.109	.0917	000014
396.000	31.819	.96638	30.907	-0916	000014
404.000	32.551	.96904	31.703	.0914	000013
412.000	33.282	.97157	32.498	.0913	000012
420.000	34.012	.97398	33.291	.0913	000012
428.000	34.742	• 97628	34.083	0912	000011
436.000	35.471	.97847	34.874	-0911	0000011
444.000	36.199	.98057	35.663	.0910	000010
452.000	36.926	.98257	36.450	-0909	000010
460.000	37.653	.98449	37.237	.0908	000010
468.000	38.380	.98632	38.022	.0907	000009
476.000	39.105	.98808	38.807	.0907	000009
484.000	39.831	.98977	39.590	.0906	000009
492.000	40.555	•99139	40.372	- 0905	000008
500.000	41.279	• 99294	41.153	.0905	000008

Table 11. Continued.

# NF3 ISOCHORE AT 2.000 MOL/L

T <sub>*</sub> K	P.BAR	Z	OP/DD	DP/DT	D2P/DT2
212.116	23.561	.65796	6.446	.2374	001518
220.000	25.395	.69416	7.668	.2289	000800
228.000	27.204	.71751	8.820	.2236	000544
236.000	28.977	.73837	9.923	.2199	000409
244.000	30.724	.75721	10.996	-2169	000324
252.000	32.449	.77435	12.045	. 2146	000266
260.000	34.158	.79005	13.075	.2126	000224
268.000	35.852	.80448	14.091	.2110	000192
276.000	37.534	.81781	15.095	-2095	000168
284.000	39.206	.83016	16.088	-2083	000148
292.000	40.867	.84164	17.072	.2072	000132
300.000	42.521	.85234	18.049	-2062	000118
308.000	44.166	.86233	19.018	.2053	000107
316.000	45.805	.87169	19.981	-2045	000098
324.000	47.438	.88047	20.938	.2037	000089
332.000	49.065	.88872	21.890	.2030	000082
340.000	50.686	.89649	22.837	.2024	000076
348.000	52.303	.90382	23.780	.2018	0000071
356.000	53.915	•91074	24.718	.2013	000066
364.000	55.523	. 91 729	25.654	.2007	000062
372.000	57.127	• 92349	26.585	-2003	000058
380.000	58.728	•92938	27.513	.1998	000055
388.000	60.324	• 93496	28.439	•1994	00 0052
396.000	61.918	.94027	29.361	.1990	000049
404.000	63.508	.94532	30.281	•1986	000047
412.000	65.095	.95013	31.198	• 1982	000044
420.000	66.679	•95472	32.112	•1979	000042
428.000	68.261	.95910	33.025	•1975	000040
436.000	69.840	.96328	33.935	.1972	000039
444.000	71.417	.96728	34.842	•1969	000037
452.000	72.991	•97110	35.748	•1966	000035
460.000	74.563	.97477	36.652	.1964	000034
468.000	76.133	•97828	37.554	.1961	000033
476.000	77.701	.98164	38.455	-1958	000031
484.000	79.267	.98487	39.353	•1956	800030
492.000	80.830	•98797	40.250	»1954	000029
500.000	82.392	•99095	41 • 1 45	•1951	000028

Table II. Continued.

# NF3 ISOCHORE AT 3.000 MOL/L

T , K	P.BAR	Z	DP/00	DP/DT	D2P/DT2
221.972	31.741	.57328	3.991	3925	003709
228.000	34.057	.59884	5.055	.3775	001772
236.000	37.030	.62904	6.345	• 3666	001081
244.000	39.931	.65610	7.576	.3593	000779
252.000	42.783	.68063	8.771	.3538	000604
260.000	45.595	.70305	9.942	.3495	000490
268.000	48.376	.72367	11.095	.3459	000410
276.000	51.131	.74270	12.232	.3428	000350
284.000	53.863	.76035	13.358	.3402	000303
292.000	56.575	.77676	14.473	.3380	000267
300.000	59.271	.79207	15.579	.3360	000237
308.000	61.951	.80638	16.677	.3342	000213
316.000	64.618	.81980	17.768	. 3325	000193
324.000	67.272	.83240	18.854	.3311	000176
332.000	69.915	.84426	19.933	.3297	000161
340.000	72.548	. 85544	21.008	.3285	000149
348.000	75.171	.86599	22.078	.3273	000138
356.000	77.785	.87597	23.143	.3263	000128
364.000	80.391	.88542	24.205	<b>325</b> 3	000120
372.000	82.990	.89439	25.263	•3243	000113
380.000	85.581	.90289	26.317	.3235	000106
388.000	88.165	.91098	27.368	. 3226	000100
396.000	90.743	.91868	28.416	.3219	000095
404-000	93.315	.92601	29.461	.3211	000090
412.000	95.882	.93300	30.503	.3204	000085
420.000	98.442	•93967	31.543	.3198	000081
428.000	100.998	. 94605	32.580	.3191	000077
436.000	103.549	.95214	33.615	-3185	0000074
444.000	106.095	.95797	34.647	.3179	000071
452.000	108.636	• 96356	35.677	.3174	000068
460.000	111.173	.96891	36.705	• 3169	000065
468.000	113.706	.97404	37.731	•3163	- 000063
476.000	116.234	.97897	38.755	.3159	000060 000058
484.000	118.759	.98371	39.777		000056
492.000	121.281	• 98825	40.797 41.815	.3149	000054
500.000	123.798	.99263	41.013	03143	- 0000074

Table 11. Continued.

#### NF3 ISOCHORE AT 4.000 MOL/L

T,K	P,BAR	Z	DP/DD	OP/DT	D2P/DT2
227.832	37.549	• 49555	2.234	• 5625	007997
228.000	37.643	.49643	2.269	.5612	007513
236.000	41.990	•53499	3.730	.5314	002198
244.000	46.183	•56911	5.073	.5178	001352
252.000	50.287	.60001	6.376	-5086	000979
260.000	54.327	.62827	7.657	.5017	000764
268.000	58.318	•65429	8.922	•4962	000623
276.000	62.269	.67837	10.175	• 4916	000523
284.000	66.186	.70073	11.419	.4878	000449
292.000	70.075	.72158	12.656	. 4844	000392
300.000	73.938	.74105	13.885	.4815	000346
308.000	77.779	.75930	15.109	.4789	000310
316.000	81.600	.77644	16.328	. 4765	000279
324.000	85.404	.79257	17.542	.4744	000254
332.000	89.191	.80777	18.752	.4724	000233
340.000	92.963	.82212	19.959	• 4706	000214
348.000	96.721	.83569	21.161	• 4690	000199
356.000	100.467	.84855	22.361	• 4675	000185
364.000	104.201	.86074	23.557	• 4660	000173
372.000	107.924	.87232	24.751	•4647	000162
380.000	111.636	.88333	25.941	• 4634	000153
388.000	115.339	.89381	27.129	•4622	000145
396.000	119.032	.90380	28.315	.4611	000137
404.000	122.716	.91332	29.498	-4600	000130
412.000	126.393	• 92242	30.679	• 4590	000124
420.000	130.061	.93111	31.857	.4580	000118
428.000	133.721	.93942	33.034	.4571	000113
436.000	137.375	.94738	34.208	. 4562	000109
444.000	141.021	•95500	35.380	• 4554	000104
452.000	144.661	.96231	36.551	. 4546	000100
460.000	148.294	.96933	37.719	. 4538	000096
468.000	151.922	.97606	38.886	.4530	000093
475.000	155.543	.98253	40.051	• 4523	000090
484.000	159.158	.98875	41.214	. 4516	000087
492.000	162.768	.99474	42.375	. 4509	000084
500.000	166.373	1.00050	43.534	. 4503	000081

Table 11. Continued.

# NF3 ISOCHORE AT 5.000 MOL/L

T,K 231.310	P,BAR 41.392	. 43044	DP/DD 1.064	DP/DT .7415	D2P/DT2
236.000	44.772	. 45634	1.961	.7080	- 003813
244.000	50.344	. 49631	3.372	. 5875	- 001829
252.000	55.794	.53257	4.757	6756	- 001231
260.000	61.163	.56586	6.134	.6671	000929
268.000	66.472	•59662	7.506	.6604	- 000744
276.000	71.733	.62518	8.875	6550	000618
284.000	76.955	.65179	10.242	26505	000527
292.000	82.142	.67667	11.606	. 6465	- 000458
300.000	87.300	69998	12.970	e 6431	- 000405
308.000	92.432	.72188	14.331	.6400	000362
316.000	97.541	.74250	15.692	.6373	000327
324.000	102.629	.76194	17.051	.6348	000298
332.000	107.698	.78031	18.408	.6325	000274
340.000	112.750	.79768	19.765	•6304	000253
348.000	117.785	. 81 415	21.120	.6284	000236
356.000	122.805	.82977	22.473	e6266	000220
364.000	127.811	.84462	23.826	.6249	000207
372.000	132.803	.85873	25.177	.6233	000195
380.000	137.783	.87218	26.526	.6218	000185
388.000	142.751	.88500	27.875	.6203	000176
396.000	147.708	.89723	29.221	.6189	000167
404.000	152.655	.90891	30.567	.6176	000160
412.000	157.591	.92008	31.911	.6164	000153
420.000	162.517	.93077	33.254	.6152	000147
428.000	167.434	.94101	34.595	-6140	000141
436.000	172.342	.95082	35.935	.6129	000136
444.000	177.241	.96023	37.274	.6119	000131
452.000	182.132	.96926	38.611	.6108	000126
460.000	187.015	.97794	39.946	.6099	000122
468.000	191.890	.98628	41.281	.6089	000118
476.000	196.757	.99430	42.614	.6080	000115
484.000	201.617	1.00202	43.945	.6071	000111
492.000	206.470	1.00945	45.275	.6062	000108
500.000	211.316	1.01662	46.604	-6053	000105

Table 11. Continued.

#### NF3 ISOCHORE AT 6.000 MOL/L

T,K	P,BAR	Z	DP/DD	DP/DT	D2P/DT2
233.188	43.610	.37488	. 356	•9237	044724
236.000	46.145	.39194	.890	.8896	005383
244.000	53.150	. 43664	2.345	.8658	001870
252.000	60.026	.47748	3.817	.8541	001187
260.000	66.824	.51520	5.304	. 8459	000878
268.000	73.566	•55024	6.802	.8397	000698
276.000	80.262	•58293	8.309	.8346	000580
284.000	86.921	.61351	9.824	.8303	000496
292.000	93.549	.64220	11.345	.8266	000434
300.000	100.148	•66917	12.871	.8233	000386
308.000	106.723	•69458	14.401	.8204	000348
316.000	113.275	.71856	15.934	.8177	000317
324.000	119.807	.74123	17.470	.8153	000292
332.000	126.321	.76269	19.008	.8131	000271
340.000	132.817	.78304	20.548	-8110	000253
348.000	139.296	.80237	22.089	.8090	000238
356.000	145.761	.82074	23.631	-8071	000225
364.000	152.211	.83822	25.174	.8054	000213
372.000	158.648	.85488	26.718	.8037	000203
380.000	165.071	.87076	28.262	.8021	000194
388.000	171.482	.88593	29.806	.8006	000186
396.000	177.881	•90042	31.351	•7992	000179
404.000	184.269	.91429	32.895	•7978	000173
412.000	190.645	•92756	34.439	• 7964	000167
420.000	197.011	•94027	35.982	.7951	000161
428.000	203.367	• 95246	37.525	•7938	000156
436.000	209.712	• 96416	39.067	• 7926	000152
444.000	216.048	• 97539	40.609	.7914	000148
452.000	222.375	.98619	42.150	• 7902	000144
460.000	228.692	• 99656	43.690	.7891	000140
468.000	235.000	1.00655	45.229	.7880	000136
476.000	241.299	1.01616	46.768	• 7869	000133
484-000	247.590	1.02542	48.305	-7858	000130
492.000	253.873	1.03434	49.841	.7848	000127
500.000	260.148	1.04295	51.377	-7838	000125

Table 11. Continued.

#### NF3 ISOCHORE AT 7.000 HOL/L

T.K	P.BAR	Z	00 (00	00.407	000/070
233.913	44.499	.32686	DP/00	09/01	D2P/DT2
236.000	46.752	.34037	041	1.1021	189899
244.000			0417	1.0716	004383
	55.244	.38901	1.947	1.0550	001208
252.000	63.651	. 43398	3.548	1.0474	000755
260.000	72.009	.47586	5.190	1.0422	<b>∞</b> 000563
268.000	80.330	•51500	6.861	1.0382	000456
276.000	88.622	.55169	8.554	1.0348	000387
284.000	96.889	.58617	10.264	1.0320	000340
292.000	105.134	.61862	11.988	1.0294	000305
300.000	113.360	.64924	13.724	1.0270	000279
308.000	121.568	.67816	15.469	1.0249	- 000259
316.000	129.759	.70553	17.222	1.0229	<b>~.</b> 000243
324.000	137.934	.73146	18.982	1.0210	000230
332.000	146.095	.75607	20.748	1.0192	000219
340.000	154.242	.77945	22.519	1.0175	000210
348.000	162.375	.80169	24.294	1.0159	000202
356.000	170.496	.82287	26.072	1.0143	000195
364.000	178.604	.84305	27.854	1.0127	000189
372.000	186.700	.86232	29.637	1.0112	000184
380.000	194.784	.88071	31.423	1.0098	000180
388.000	202.856	.89830	33.211	1.0084	000176
396.000	210.918	.91513	35.000	1.0070	000172
404.000	218.968	.93125	36.790	1.0056	000168
412.000	227.008	.94669	38.580	1.0043	000165
420.000	235.037	.96151	40.372	1.0030	000162
428.000	243.055	.97572	42.163	1.0017	000159
436.000	251.064	.98938	43.955	1.0004	000157
444.000	259.062	1.00250	45.747	.9992	000154
452.000	267.050	1.01513	47.539	.9979	000152
460.000	275.029	1.02728	49.330	.9967	000150
468.000	282.998	1.03897	51.121	. 9956	000148
476.000	290.958	1.05024	52.912	.9944	000146
484.000	298.908	1.06111	54.702	. 9932	000144
492.000	306.850	1.07158	56.491	.9921	000142
500.000	314.782	1.08170	58.279	-9909	000140
- 40000	3210106				•

Table 11. Continued.

#### NF3 ISOCHORE AT 7.920 MOL/L

T . K	P.BAR	Z	DP/DD	DP/DT	D2P/DT2
234.000	44.607	. 28949	0.000	1.2451	0.000000
236.000	47.097	.30306	.371	1.2451	000005
244.000	57.058	. 35511	2.044	1.2450	000025
252.000	67.016	•40385	3.826	1.2447	000042
260.000	76.972	.44957	5.668	1.2443	000056
268.000	86.925	. 49255	7.552	1.2438	000069
276.000	96.873	.53301	9.469	1.2432	000081
284.000	106.816	.57116	11.410	1.2425	000091
292.000	116.753	.60719	13.373	1.2417	000100
300.000	126.684	.64127	15.353	1.2409	000107
308.000	136.607	.67354	17.346	1.2400	000114
316.000	146.524	.70414	19.352	1.2391	000120
324.000	156.433	.73320	21.368	1.2381	000125
332.000	166.334	.76082	23.393	1.2371	000130
340.000	176.226	.78710	25.426	1.2360	000134
348.000	186.110	.81214	27.464	1.2350	000137
356.000	195.986	.83601	29.509	1.2338	000140
364.000	205.852	.85880	31.558	1.2327	000143
372.000	215.709	.88057	33.611	1.2316	000145
380.000	225.557	•90139	35.667	1.2304	000147
388.000	235.395	.92131	37.725	1.2292	000148
396.000	245.224	•94039	39.788	1.2280	000150
404.000	255.044	•95868	41.851	1.2268	000151
412.000	264.854	• 97622	43.917	1.2256	000152
420.000	274.654	.99306	45.983	1.2244	000152
428.000	284.444	1.00923	48.051	1.2232	000153
436.000	294.224	1.02478	50.119	1.2219	000153
444.000	303.995	1.03973	52.187	1.2207	000154
452.000	313.756	1.05413	54.256	1.2195	000154
460.000	323.507	1.06798	56.325	1.2183	000154
468.000	333.248	1.08134	58.394	1.2170	000154
476.000	342.979	1.09421	60.463	1.2158	000153
484.000	352.701	1.10662	62.531	1.2146	000153

Table 11. Continued.

# NF3 ISOCHORE AT 9.000 MOL/L

T . K	P.BAR	Z	DP/00	DP/DT	D2P/DT2
233.930	44.520	• 25432	•036	1.4263	•199779
236.000	47.540	. 26920	. 488	1.4713	. 00 7078
240.000	53.465	.29770	1.433	1.4886	.002903
244.000	59.439	. 32554	2.428	1.4979	.001892
248.000	65.444	. 35265	3.455	1.5044	.001408
252.000	71.472	.37902	4.506	1.5094	.001115
256.000	77.518	. 40466	5.577	1.5134	.000914
260.000	83.579	• 42958	6.663	1.5168	000766
264.000	89.652	• 45381	7.764	1.5196	.000651
268.000	95.735	.47737	8.877	1.5220	.000558
272.000	101.827	.50028	10.000	1.5241	.000482
276.000	107.927	.52257	11.132	1.5259	.000417
280.000	114.034	.54425	12.273	1.5274	.000363
284.000	120.146	.56535	13.421	1.5288	.000315
288.000	126.264	.58588	14.576	1.5300	.000273
292.000	132.386	.60587	15.738	1.5310	.000236
296.000	138.512	.62534	16.905	1.5319	.000204
300.000	144.640	.64430	18.077	1.5326	.000174
304.000	150.772	.66278	19.254	1.5333	.000148
308.000	156.906	.68079	20.435	1 . 5338	0000124
312.000	163.042	.69834	21.621	1.5342	.000102
316.000	169.180	.71546	22.810	1.5346	.000083
320.000	175.319	.73215	24.002	1.5349	.000065
324.000	181.459	.74844	25.198	1.5351	.000048
328.000	187.600	.76433	26.396	1.5353	.000033
332.000	193.742	.77984	27.598	1.5354	.000019
336.000	199.883	.79498	28.801	1.5354	.000006
340.000	206.025	.80977	30.007	1.5354	000006
344.000	212.167	.82422	31.216	1.5354	000017
348.000	218.308	.83833	32.426	1.5353	000028
352.000	224.449	. 85211	33.638	1.5352	000037
356.000	230.590	.86559	34.852	1.5350	000046
360.000	236.729	. 87876	36.067	1.5348	000055
364.000	242.868	.89164	37.284	1.5346	000062
368.000	249.006	.90424	38.502	1.5343	000070
372.000	255.143	.91656	39.721	1.5340	000076
376.000	261.278	• 92862	40.942	1.5337	000083
380.000	267.412	.94041	42.164	1.5334	000089
384.000	273.545	.95196	43.386	1.5330	000094 000099
388.000	279.676	.96326	44.610 45.834	1.5326	
392.000	285.806	. 97433		1.5322 1.5318	000104 000109
396.000	291.934	.98517	47.060 48.285	1.5313	000113
400.000	298.060	.99578	49.512	1.5309	000117
404.000	304.184	1.00618	50.739	1.5304	000121
	310.307 316.427	1.01637	51.967	1.5299	000125
412.000	322.546	1.03614	53.195	1.5294	000128
420.000	328.663	1.04574	54.423	1.5289	000120
424.000	334.777	1.05514	55.652	1.5283	000134
428.000	340.889	1.06437	56.881	1.5278	000137
432.000	346.999	1.07341	58.110	1.5272	000140
436.000	353.107	1.08228	59.340	1.5267	000142
440-000	359.213	1.09099	60.570	1.5261	000145
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Table 11. Continued.

#### NF3 ISOCHORE AT 10.000 MOL/L

TV	0.040	Z	00/00	DP/DT	0.20 (0.7.2
T, K	P + 8AR	_	DP/00		D2P/DT2
233.503	43.994	. 22660	.310	1.6604	.075649
236.000	48.241	.24585	1.020	1.7230	.012050
240.000	55.205	.27665	2.171	1. 7553	. 005775
244.000	62.266	.30692	3.364	1.7742	.003911
248.000	69.391	.33653	4.590	1.7877	.002970
252.000	76.564	. 36542	5.840	1.7984	. 00 2387
256.000	83.776	•39359	7.111	1.8071	. 001984
260.000	91.019	.42104	8 • 400	1.8144	.001684
264.000	98-290	•44778	9.704	1.8206	.001452
268.000	105.583	•47383	11.022	1.8261	.001265
272.000	112.897	.49920	12.352	1.8308	.001111
276.000	120.229	•52392	13.692	1.8350	.000981
280.000	127.576	•54799	15.042	1.8387	.000871
284.000	134.938	•57145	16.400	1.8420	.000775
288.000	142.312	.59431	17.766	1.8449	.000692
292.000	149.696	.61658	19.139	1.8475	.000618
296.000	157.091	.63830	20.519	1.8499	• 000553
300.000	164.495	•65947	21.904	1.8519	.000495
304.000	171.907	.68012	23.295	1.8538	. 000443
308.000	179.325	.70025	24.691	1.8555	.000395
312.000	186.750	.71990	26.092	1.8570	. 0003 52
316.000	194.181	.73907	27.497	1.8583	.000314
320.000	201.617	.75777	28.906	1.8595	.000278
324.000	209.057	.77604	30.318	1.8605	.000245
328.000	216.501	.79387	31.734	1.8615	.000215
332.000	223.948	.81129	33.152	1.8623	.000188
336.000	231.399	.82830	34.574	1.8630	.000163
340.000	238.852	.84492	35.998	1.8636	.000139
344.000	246.307	.86116	37.425	1.8641	.000117
348.000	253.764	.87703	38.854	1.8645	.000097
352.000	261.223	.89255	40.285	1.8649	.000078
356.000	268.683	• 90773	41.718	1.8651	.000061
360.000	276.144	.92257	43.153	1.8654	.000044
364.000	283.606	.93708	44.590	1.8655	. 000029
368.000	291.068	• 95129	46.028	1.8656	.000015
372.000	298.531	.96518	47.467	1.8656	.000001
376.000	305.993	• 97879	48.908	1.8656	000011
380.000	313.455	•99210	50.350	1.8655	000023
384.000	320.917	1.00514	51.793	1.8654	000034
388.000	328.379	1.01790	53.237	1.8653	000044
392.000	335.839	1.03041	54.681	1.8651	000054
396.000	343.299	1.04266	56.127	1.8648	000063
400.000	350.758	1.05466	57.574	1.8646	000072
404.000	358.215	1.06642	59.021	1.8643	000080

Table 11. Continued.

#### NF3 ISOCHORE AT 11.000 MOL/L

T,K	PyBAR	Z	DP/DD	DP/DT	D2P/DT2
232.416	42.685	.20081	1.174	1.9648	.044829
236.000	49.898	.23118	2.516	2.0442	.013076
240.000	58.161	.26497	3.979	2.0840	.007801
244.000	66.553	.29823	5.462	2.1104	.005643
248.000	75.036	.33082	6.969	2-1303	.004425
252.000	83.590	.36268	8.495	2.1463	. 003627
256.000	92.203	.39380	10.040	2.1597	.003056
260.000	100.865	. 42417	11.601	2.1710	.002623
264.000	109.569	. 45 379	13.176	2.1808	.002281
268.000	118.309	.48267	14.764	2.1893	.002004
272.000	127.082	.51084	16.364	2.1968	.001773
276.000	135.883	•53830	17.974	2.2035	.001578
280.000	144.789	•56508	19.593	2.2095	.001411
284.000	153.558	.59119	21.221	2.2149	.001266
288.000	162.427	.61665	22.856	2.2197	.001139
292.000	171.315	.64148	24.498	2.2240	.001027
296.000	180.218	.66570	26.147	2.2279	.000928
300.000	189.137	.68933	27.802	2.2314	. 000839
304.000	198.069	.71 239	29.463	2.2346	.000759
308.000	207.014	.73489	31.128	2.2375	.000686
312.000	215.969	.75685	32.798	2.2401	.000621
316.000	224.934	.77829	34.472	2-2425	.000561
320.000	233.909	.79922	36.150	2.2446	.000506
324.000	242.891	.81967	37.832	2.2465	.000456
328.000	251.881	.83964	39.517	2.2483	.000410
332.000	260.877	.85915	41.205	2.2498	.000368
336.000	269.879	.87822	42.896	2.2512	.000329
340.000	278.886	. 89685	44.590	2.2525	.000293
344.000	287.898	.91507	46.286	2.2536	.000259
348.000	296.915	.93288	47.984	2.2545	.000228
352.000	305.935	.95029	49.684	2.2554	.000199
356.000	314.958	.96733	51.386	2.2561	• 000172
360.000	323.983	.98399	53.090	2.2568	- 000147
364.000	333.012	1.00030	54.796	2.2573	.000123
368.000	342.042	1.01625	56.502	2.2577	.000101
372.000	351.073	1.03187	58.210	2.2581	.000080

Table 11. Continued.

	NF3 IS	OCHORE AT	12.000 MOL	/L .	
T,K	P,BAR	Z	DP/00	DP/DT	D2P/DT2
230.408	40.364	.17558	3.120	2.3546	.032221
232.000	44.148	.19072	3.917	2.3959	. 021328
236.000	53.870	.22878	5.815	2-4590	.012081
240.000	63.791	.26640	7.683	2.4995	.008590
244.000	73.852	.30336	9.554	2.5297	.006682
248.000	84.021	.33956	11.435	2.5538	.005453
252.000	94.277	.37496	13.327	2.5738	.004582
256.000	104.607	.40955	15.232	2.5908	.003927
260.000	115.000	.44331	17.149	2.6054	.003414
264.000	125.448	.47626	19.075	2.6182	.002999
268.000	135.944	.50840	21.012	2.6295	.002655
272.000	146.483	•53976	22.958	2.6395	.002365
276.000	157.059	•57034	24.912	2.6485	.002118
280.000	167.669	.60017	26.874	2.6565	.001904
284.000	178.310	.62927	28.843	2.6637	.001717
288.000	188.978	•65766	30.819	2.6703	.001552
292.000	199.671	•68535	32.800	2.6762	.001405
296.000	210.387	•71238	34.787	2.6815	.001275
300.000	221.123	•73875	36.779	2.6864	.001157
304.000	231.878	.76448	38.775	2.6908	.001052
308.000	242.649	.78961	40.776	2.6948	.000956
312.000	253.436	.81413	42.780	2.6985	.000868
316.000	264.236	.83808	44.788	2.7018	.000789
320.000	275.050	.85148	46.800	2.7048	.000716
324.000	285.874	.88433	48.814	2.7075	.000649
328.000	296.709	•90665	50.831	2.7100	.000587
332.000	307.554	.92847	52.851	2.7122	. 00 05 31
336.000	318.407	.94979	54.873	2.7142	.000478
340.000	329.268	• 97063	56.897	2.7161	.000429
344.000	340.135	.99100	58.923	2.7177	.000384
348.000	351.009	1.01093	60.950	2 . 71 91	.000342

Table 11. Continued.

# NF3 ISOCHORE AT 13.000 MOL/L

TyK	PoBAR	79	00/00	00 10 9	000 (090
		2	OP/00	OP/OT	D2P/DT2
227.273	36.961	•15046	6.763	2.8478	.025811
228.000	39.038	. 15840	7.229	2.8654	.022921
230.000	44.810	.18025	8 - 473	2.9055	. 817674
232.000	50.654	.20200	9.686	2.9374	.014476
234.000	56.557	.22361	10.881	2.9641	.012295
236.000	62.508	.24504	12.067	2.9870	.010696
238.000	68.503	26629	13.246		009465
				3.0071	
240.000	74.535	.28732	14.423	3.0250	. 008482
242.000	80.602	.30814	15.598	3.0412	.007676
244.000	86.699	.328-73	16.773	3.0558	.007000
246.000	92.824	.34910	17.947	3.0692	.006424
248.000	98.975	• 36923	19.122	3.0816	. 005926
250.000	105.150	.38912	20.298	3.0930	.005490
252.000	111.346	-40879	21.475	3.1036	. 005105
254.000	117.563	.42821	22.653	3.1134	.004762
256.000	123.800	.44740	23.832	3.1226	.004455
258.000	130.054	.46635	25.012	3.1313	.004177
260.000	136.324	• 48509	26.194	3.1394	.003924
262.000	142.611	•50358	27.378	3.1470	.003694
264.000	148.912	.52185	28.562	3.1541	.003482
266.000	155.227	•53989	29.748	3.1609	.003288
268.000	161.555	.55771	30.936	3.1673	.003109
270.000	167.896	.57530	32.125	3.1734	.002942
272.000	174.249	•59268	33.315	3.1791	.002788
274.000	180.612	.60984	34.506	3.1845	.002644
276.000	186.986	.62679	35.698	3.1897	.002509
278.000	193.371	.64353	36.892	3.1946	.002384
280.000	199.765	.66006	38.087	3.1992	.002266
	_	.67638	39.283		
282.000	206.167			3.2036	•002155
284.000	212.579	.69250	40.479	3.2078	.002050
286.000	218.999	.70843	41.677	3.2118	.001952
288.000	225.426	•72416	42.876	3.2156	001859
290.000	231.861	.73969	44.076	3.2193	.001771
292.000	238.303	.75504	45.277	3.2227	.001688
294.000	244.752	.77019	46.478	3.2260	.001609
296.000	251.207	.78516	47.681	3.2292	.001535
298.000	257.668	.79995	48.884	3.2322	.001463
300.000	264.136	.81457	50.088	3.2350	.001396
302.000	270.609	.82900	51.293	3.2378	.001331
304.000	277.087	. 84 326	52.498	3.2404	.001270
		.85735	53.704	3.2428	.001211
306.000	283.570		54.911	3.2452	.081155
308.000	290.058	.87127			
310.000	296.551	.88503	56.118	3.2475	.001102
312.000	303.048	.89862	57.326	3.2496	.001051
314.000	309.549	.91205	58.534	3.2517	.001002
316.000	316.054	•92533	59.743	3.2536	.000955
318.000	322.563	.93844	60.953	3.2555	.000910
320.000	329.076	.95141	62.162	3.2573	.000867
322.000	335.592	.96422	63.373	3.2590	.000826
324.000	342.112	.97689	64.583	3.2606	.000786
326.000	348.635	.98940	65.795	3.2621	.000748
328.000	355.160	1.00178	67.006	3.2636	.000712
320000	327.100	7 4 40 71 0	0.4000		

Table 11. Continued.

#### NF3 ISOCHORE AT 14.000 MOL/L

T.K	P.BAR	Z	0P/00	DP/DT	D2P/DT2
222.861	32.572	.12556	12.816	3.4645	.022137
224.000	36.533	.14011	13.717	3.4883	.019766
226.000	43.547	.16553	15.267	3.5246	.016677
228.000	50.628	.19076	16.788	3.5556	.014441
230.000	57.767	.21577	18.290	3.5827	.012734
232.000	64.957	. 24053	19.778	3.6068	.011380
234.000	72.193	.26504	21.257	3.6284	.010275
236.000	79.470	.28928	22.729	3.6480	•009352
238.000		•31325	24.196	3.6659	•008568
240.000	94.132	• 33695	25.658	3.6824	.007892
242.000	101.512	.36036	27.118	3.6975	.007302
244.000		.38350	28.575	3.7116	. 006782
246.000		.40635	30.031	3.7247	.006319
248.000	123.820	.42892	31.485	3.7369	.005904
250.000	131.305	. 45121	32.939	3.7483	. 005530
252.000	138.813	.47322	34.392	3.7591	.005191
254.000	146.341	.49496	35.844	3.7691	.004882
256.000		•51642	37.296	3.7786	• 004599
258.000	161.455	.53761	38.748	3.7875	.004338
260.000		•55853	40.200	3.7960	.004898
262.000		.57919	41.652	3.8039	.003876
264.000		.59958	43.104	3.8115	.003670
266.000		.61972	44.556	3. 81 86	.003478
268.000		.63960	46.009	3.8254	.003299
270.000		•65922	47.461	3.8318	. 003131
272.000		.67860	48.914	3.8379	.002974
274.000		.69773	50.367	3.8437	.002827
276.000		.71662	51.820	3.8492	.002688
278.000		.73527	53.273	3.8545	.002558
280.000		.75369	54.727	3.8595	.002435
282.000		.77187	56.181	3.8642	.002318
284.000		.78983	57.635	3.8688	.002208
286.000	268.847	.80756	59.089	3.8731	.002104
288.000		.82507	60.544	3.8772	. 002005
290.000		.84236	61.999	3.8811	.001911
292.000	292.121	.85944	63.454	3.8848	.001821
294.000		.87631	64.909	3.8884	.001736
296.000	307.675	.89297	66.364	3.8918	.001655
298.000		.90942	67.820	3.8950	.001578
300.000	323.255	.92568	69.275	3.8981	.001504
302.000		.94173	70.731	3.9010	.001434
304.000		•95759	72.187	3.9038	.001367
306.000	346.669	•97326	73.643	3.9065	.001302
308.000	354.485	.98874	75.099	3.9090	.001241

Table 11. Continued.

#### NF3 ISOCHORE AT 15.000 MOL/L

T,K	P.BAR	Z	DP/00	OP/DT	D2P/DT2
217.076	27.447	.10138	22.066	4.2287	.019869
218.000	31.365	.11536	22.963	4.2465	.018627
220.000	39.894	.14540	24.879	4.2814	.016404
222.000	48.488	.17513	26.766	4.3124	.014642
224.000	57.141	.20454	28.632	4.3402	.013205
226.000	65.847	.23361	30.482	4.3654	.012006
228.000	74.601	.26235	32.319	4.3883	.010988
230.000	83.399	.29074	34.145	4.4094	.010110
232.000	92.238	.31878	35.962	4.4289	.009344
234.000	101.113	.34647	37.772	4.4469	.008669
236.000	110.024	.37381	39.576	4.4636	.008069
238.000	118.967	.40079	41.375	4.4792	.007532
240.000	127.940	. 42743	43.170	4.4937	.007047
242.000	136.941	. 45372	44.961	4.5074	.006608
244.000	145.969	.47967	46.749	4.5202	.006208
246.000	155.022	.50528	48.533	4.5322	. 005841
248.000	164.098	•53055	50.316	4.5436	.005505
250.000	173.196	• 55548	52.096	4.5543	.005195
252.000	182.314	.58009	53.874	4.5644	.004908
254.000	191.453	.60437	55.650	4.5739	. 004641
256.000	200.610	.62833	57.425	4.5830	.004394
258.000	209.784	•65197	59.199	4.5915	.004163
260.000	218.975	.67530	60.971	4.5996	.083947
262.000	228.182	.69832	62.741	4.6073	.003745
264.000	237.404	.72104	64.511	4.6146	.003555
266.000	246.641	.74346	66.280	4.6215	.003377
268.000	255.890	.76558	68.047	4.6281	.003209
270.000	265.153	.78742	69.814	4.6344	.003050
272.000	274.428	.80897	71.580	4.6403	.002901
274.000	283.714	.83024	73.345	4.6460	.002759
276.000	293.011	.85123	75.110	4.6514	.002626
278.000	302.319	.87195	76.873	4.6565	.002499
280.000	311.637	.89241	78.636	4.6614	.002378
282.000	320.964	.91260	80.398	4.6660	.002264
284.000	330.301	• 93253	82.160	4.6704	.002155
286.000	339.646	• 95221	83.921	4.6746	.002051
288.000	348.999	.97164	85.681	4.6786	.001953
290.000	358.360	.99082	87.440	4.6824	.001859

Table 11. Continued.

### NF3 ISOCHORE AT 16.000 MOL/L

T <sub>2</sub> K	P,BAR	Z	DP/DD	DP/DT	D2P/DT2
209.872	21.943	.07859	35.358	5.1684	.018399
210.000	22.605	.08091	35.510	5.1707	.018273
212.000	32.981	.11694	37.859	5.2054	.016478
214.000	43.424	. 15253	40.179	5.2368	. 014977
216.000	53.927	.18767	42.476	5.2655	.013700
218.000	64.485	.22235	44.754	5.2918	. 012597
220.000	75.093	. 25658	47.015	5.3160	. 011633
222.000	85.747	-29034	49.263	5.3384	. 010783
224.000	96.445	.32365	51.499	5.3592	.010026
226.000	107.183	·35650	53.724	5.3785	.009348
228.000	117.958	.38890	55.941	5.3966	.008737
230.000	128.769	-42085	58.150	5.4135	.008182
232.000	139.612	.45235	60.351	5.4294	. 007677
234.000	150.485	.48342	62.546	5.4442	.007215
236.000	161.388	.51405	64.736	5.4582	.006790
238.000	172.318	•54425	66.920	5.4714	.006398
240.000	183.273	•57403	69.099	5.4839	.006036
242.000	194.253	.60339	71.274	5.4956	.005700
244.000	205.255	.63234	73.446	5.5067	•005387
246.000	216.279	.66088	75.613	5.5172	.005096
248.000	227.323	-68903	77.777	5.5271	.004824
250.000	238.387	.71678	79.938	5.5365	. 004569
252.000	249.469	.74415	82.095	5.5454	.004330
254.000	260.568	.77114	84.251	5.5538	.004106
256.000	271.684	.79775	86.403	5.5618	.003894
258.000	282.815	-82400	88.553	5.5694	.003695
260.000	293.961	.84989	90.700	5.5766	• 003507
262.000	305.121	.87542	92.846	5.5834	•003330
264.000	316.295	•90060	94.989	5.5899	.003162
266.000	327.481	. 92544	97.129	5.5961	.003002
268.000	338.679	.94994	99.268	5.6019	.002851
270.000	349.888	.97411	101.405	5.6075	.002708

Table 11. Continued.

### NF3 ISOCHORE AT 17.000 MOL/L

ToK	P .BAR	Z	09/00	DP/DT	D2P/DT2
201.249	16.476	.05792	53.597	6.3179	. 017416
202.000	21.226	.07434	54.669	6.3307	.016850
204.000	33.920	.11764	57.503	6.3630	.015480
206.000	46.676	.16030	60.312	6.3928	.014282
208.000	59.489	.20234	63.098	6.4203	013223
210.000	72.356	.24376	65.865	6-4457	.012279
212.000	85.271	.28457	68.615	6.4694	. 011433
214.000	98.232	.32476	71.350	6.4915	.010669
216.000	111.236	.36434	74.072	6.5122	.009976
218.000	124.280	.40333	76.782	6.5315	.009344
220.000	137.361	•44173	79.480	6.5496	.008766
222.000	150.478	• 47955	82.169	6.5666	.008234
224.000	163.627	-51680	84.849	6.5825	.007744
226.000	176.807	•55349	87.520	6.5976	.007291
228.000	190.017	• 58962	90.183	6.6117	.006871
230.000	203.254	.62521	92.840	6.6251	.006481
232.000	216.516	•66026	95.490	6.6377	.006117
234.000	229.804	.69479	98.133	6.6496	.005777
236.000	243.114	.72881	100.771	6.6608	.005459
238.000	256.447	•76232	103.403	6.6714	.005161
240.000	269.799	•79533	106-030	6.6814	-004881
242.000	283.172	.82785	108.652	6.6909	.004618
244.000	296.563	.85989	111.270	6.6999	.004370
246.000	309.971	.89146	113.883	6.7084	.004137
248.000	323.396	• 92257	116.492	6.7165	.003916
250.000	336.837	•95322	119.097	6.7241	.003707
252.000	350.292	.98343	121.697	6.7313	.003509

Table 11. Continued.

#### NF3 ISOCHORE AT 18.000 MOL/L

T . K	P.BAR	Z	DP/0D	DP/DT	02P/DT2
191.243	11.458	.04003	77.762	7.7196	.016749
192.000	17.310	.06024	79.065	7.7321	.016261
193.000	25.051	• 08673	80.780	7.7481	.015648
194.000	32.806	.11299	82.487	7.7634	.015068
195.000	40.577	•13904	84.189	7.7782	. 014519
196.000	48.363	•16487	85.884	7.7925	.013999
197.000	56.162	.19049	87.573	7.8062	. 013504
198.000	63.975	.21589	89.257	7.8195	.013033
199.000	71.801	.24108	90.936	7.8323	.012585
200.000	79.639	.26607	92.610	7.8447	.012157
201.000	87.490	.29084	94.280	7.8566	.011749
202.000	95.352	.31541	95.945	7.8682	.011359
203.000	103.226	.33977	97.606	7.8793	.010986
204.000	111.111	.36393	99.263	7.8901	.010629
205.000	119.006	.38789	100.916	7. 9006	.010287
206.000	126.912	•41165	102.565	7.9107	.009958
207.000	134.828	• 43521	104.211	7.9205	.009643
208.000	142.753	• 45858	105.853	7.9300	.009340
209.000	150.687	.48175	107.493	7.9392	. 00 90 49
210.000	158.631	•50473	109.129	7.9481	.008769
211.000	166.584	.52752	110.762	7.9567	.008500
212.000	174.545	•55013	112.392	7.9651	.008240
213.000	182.514	•57254	114.019	7.9732	.007990
214.000	190.491	•59477	115.644	7.9811	• 007749
215.000	198.476	•61682	117.265	7.9887	.007516
216.000	206.468	.63869	118.885	7.9961	.007291
217.000	214.468	•66038	120.502	8.0033	.007074
218.000	222.475	.68189	122.116	8.0103	.006865
219.000	230.488	.70323	123.728	8.0170	.006662
220.000	238.509	.72439	125.338	8.0236	.006466
221.000	246.536	.74538	126.946	8.0300	.006276
222.000	254.569	.76620	128.552	8.0362	. 006092
223.000	262.608	.78685	130.156	8.0422	.005914
224.000	270.653	-80734	131.757	8.0480	.005741
225.000	278.704	.82766	133.357	8.0536	.005574
226.000	286.760	.84782	134.954	8.0591	.005412
227.000	294.822	.86781	136.550	8.0645	. 005255
228.000					
	302.889	88765	138.144	8.0696	• 005102
229.000	310.961	.90732	139.737	8.0747	.004954
230.000	319.038	.92684	141.327	8.0796	.004811
231.000	327.120	.94621	142.916	8.0843	. 004671
232.000	335.207	• 96542	144.503	8.0889	.004535
233.000	343.298	.98448	146.089	8.0934	• 004403
234.000	351.394	1.00339	147.673	8.0977	.004275
235.000	359.493	1.02215	149.255	8.1019	.004150

Table 11. Continued.

# NF3 ISOCHORE AT 19.000 MOL/L

	2 2 4 2	_			
1,K	P,BAR	Z	DP/DD	OP/DT	D2P/DT2
179.919	7.236	.02546	108.950	9.4275	.016303
180-000	7.996	.02812	169.117	9.4289	• 016255
181.000	17.433	.06097	111.190	9.4448	.015666
182.000	26.886	.09351	113.257	9.4602	.015106
183.000	36.353	•125,75	115.316	9.4750	.014572
184.000	45.836	•15769	117.369	9.4894	.014062
185.000	55.332	•18933	119.415	9.5032	.013574
186.000	64.842	.22067	121.456	9.5165	.013108
187.000	74.365	•25173	123.491	9.5294	.012662
188.000	83.900	.28250	125.520	9.5418	.012234
189.000	93.448	-31298	127.544	9.5539	.011824
190.000	103.008	.34318	129.563	9.5655	.011430
191.000	112.579	.37311	131.578	9.5767	.011052
192.000	122.161	•40276	133.587	9.5876	.010689
193.000	131.754	.43213	135.592	9.5981	.010339
194.000	141.357	•46124	137.593	9.6083	.010003
195.000	150.971	.49008	139.590	9.6181	.009679
196.000	160.594	•51866	141.582	9.6276	.009367
197.000	170.226	• 54698	143.571	9.6369	.009067
198.000	179.867	•57504	145.556	9.6458	.008777
199.000	189.517	•60285	147.537	9.6544	.008497
200.000	199.176	.63040	149.514	9.6628	.008227
201.000	208.843	.65771	151.488	9.6709	.007966
202.000	218.518	.68477	153.459	9.6787	.007713
203.000	228.200	.71159	155.426	9.6863	.007470
204.000	237.890	.73817	157.391	9.6937	. 007234
205.000	247.587	.76451	159.352	9-7008	.007006
206.000	257.292	.79062	161.310	9.7077	.006785
207.000	267.003	.81650	163.265	9.7143	.006571
208.000	276.720	.84215	165.218	9.7208	.006364
209.000	286.444	.86757	167.167	9.7271	.006163
210.000	296.174	.89277	169.114	9.7331	.005968
211.000	305.910	.91775	171.058	9.7390	.005779
212.000	315.652	.94250	173.000	9.7447	.005596
213.000	325.400	.96705	174.939	9.7502	.005419
214.000	335.153	.99138	176.875	9.7555	.005246
215.000	344.911	1.01550	178.809	9.7607	.005079
216.000	354.674	1.03941	180.741	9.7657	.004916

Table 11. Continued.

# NF3 ISOCHORE AT 20.000 MOL/L

T,K P,8AR Z DP/DD DP/DT D2P/DT2 167.370	T 4	0 040	7	00/00	00/07	000/070
168.000       11.288       .04041       150.050       11.5220       .015659         169.000       22.818       .08119       152.553       11.5373       .015092         170.000       34.363       .12156       155.049       11.5522       .014549         171.000       45.922       .16150       157.537       11.5665       .014029         172.000       57.496       .20102       160.019       11.5802       .013530         173.000       69.083       .24014       162.494       11.5935       .013051         174.000       80.683       .27885       164.962       11.6063       .012591         175.000       92.295       .31716       167.424       11.6187       .012149         160.001       103.920       .35507       169.881       11.6306       .011723         177.000       15.556       .39260       172.331       11.6422       .011314         178.000       127.204       .42975       174.776       11.6533       .010921         179.000       138.863       .46652       177.215       11.6642       .01176         181.000       150.532       .50291       179.649       11.6744       .010176         <	-	•	_			
169.000       22.818       .08119       152.553       11.5373       .015092         170.000       34.363       .12156       155.049       11.5522       .014549         171.000       45.922       .16150       157.537       11.5665       .014029         172.000       57.496       .20102       160.019       11.5802       .013530         173.000       69.083       .24014       162.494       11.5935       .013530         174.000       80.683       .27885       164.962       11.6063       .012591         175.000       92.295       .31716       167.424       11.6187       .012149         176.000       103.920       .35507       169.881       11.6306       .011723         177.000       115.556       .39260       172.331       11.6422       .011314         178.000       127.204       .42975       174.776       11.6533       .010921         179.000       138.863       .46652       177.215       11.6640       .010541         180.000       162.211       .53893       182.078       11.6744       .010176         181.000       162.211       .53893       182.078       11.6940       .009483						
170.000       34.363       .12156       155.049       11.5522       .014549         171.000       45.922       .16150       157.537       11.5665       .014029         172.000       57.496       .20102       160.019       11.5802       .013530         173.000       69.083       .24014       162.494       11.5935       .013051         174.000       80.683       .27885       164.962       11.6063       .012591         175.000       92.295       .31716       167.424       11.6187       .012149         176.000       103.920       .35507       169.881       11.6306       .011723         177.000       115.556       .39260       172.331       11.6422       .011314         178.000       127.204       .42975       174.776       11.6533       .010921         179.000       138.863       .46652       177.215       11.6640       .010176         181.000       162.211       .53893       182.078       11.6744       .010176         181.000       162.211       .53893       182.078       11.6744       .009823         183.000       177.307       .64485       189.336       11.7123       .008838						
171.000       45.922       .16150       157.537       11.5665       .014029         172.000       57.496       .20102       160.019       11.5802       .013530         173.000       69.083       .24014       162.494       11.5935       .013051         174.000       80.683       .27885       164.962       11.6063       .012591         175.000       92.295       .31716       167.424       11.6187       .012149         176.000       103.920       .35507       169.881       11.6306       .011723         177.000       115.556       .39260       172.331       11.6422       .011314         178.000       127.204       .42975       174.776       11.6533       .010921         179.000       138.863       .46652       177.215       11.6640       .010541         180.000       150.532       .50291       179.649       11.6744       .010176         181.000       162.211       .53893       182.078       11.6844       .009823         183.000       173.900       .57460       184.502       11.6940       .009483         183.000       197.307       .64485       189.336       11.7123       .00838						
172.000       57.496       .20102       160.019       11.5802       .013530         173.000       69.083       .24014       162.494       11.5935       .013051         174.000       80.683       .27885       164.962       11.6063       .012591         175.000       92.295       .31716       167.424       11.6187       .012149         176.000       103.920       .35507       169.881       11.6306       .011723         177.000       115.556       .39260       172.331       11.6422       .011314         178.000       127.204       .42975       174.776       11.6642       .010541         180.000       150.532       .50291       179.649       11.6744       .010176         181.000       162.211       .53893       182.078       11.6844       .009823         182.000       173.900       .57460       184.502       11.6940       .009483         183.000       185.599       .60990       186.921       11.7033       .009155         184.000       197.307       .64485       189.336       11.7123       .00838         185.000       29.024       .67945       191.746       11.7230       .008532						
173.000       69.083       .24014       162.494       11.5935       .013051         174.000       80.683       .27885       164.962       11.6063       .012591         175.000       92.295       .31716       167.424       11.6187       .012149         176.000       103.920       .35507       169.881       11.6306       .011723         177.000       115.556       .39260       172.331       11.6422       .011314         178.000       127.204       .42975       174.776       11.6533       .010921         179.000       138.863       .46652       177.215       11.6640       .010541         180.000       150.532       .50291       179.649       11.6744       .010176         181.000       162.211       .53893       182.078       11.6844       .009823         182.000       173.900       .57460       184.502       11.6940       .009483         183.000       185.599       .60990       186.921       11.7033       .009155         184.000       197.307       .64485       189.336       11.7123       .00838         185.000       209.024       .67945       191.746       11.7294       .008236						
174.000       80.683       .27885       164.962       11.6063       .012591         175.000       92.295       .31716       167.424       11.6187       .012149         176.000       103.920       .35507       169.881       11.6306       .011723         177.000       115.556       .39260       172.331       11.6422       .011314         178.000       127.204       .42975       174.776       11.6533       .010921         179.000       138.863       .46652       177.215       11.6640       .010541         180.000       150.532       .50291       179.649       11.6744       .010176         181.000       162.211       .53893       182.078       11.6844       .009823         182.000       173.900       .57460       184.502       11.6940       .009483         183.000       185.599       .60990       186.921       11.7033       .009155         184.000       197.307       .64485       189.336       11.7123       .00838         185.000       209.024       .67945       191.746       11.7294       .008236         187.000       232.482       .74762       196.553       11.7453       .007673	172.000	57.496		160.019		.013530
175.000       92.295       .31716       167.424       11.6187       .012149         176.000       103.920       .35507       169.881       11.6306       .011723         177.000       115.556       .39260       172.331       11.6422       .011314         178.000       127.204       .42975       174.776       11.6533       .010921         179.000       138.863       .46652       177.215       11.6640       .010541         180.000       150.532       .50291       179.649       11.6744       .010176         181.000       162.211       .53893       182.078       11.6940       .009823         182.000       173.900       .57460       184.502       11.6940       .009483         183.000       185.599       .60990       186.921       11.7033       .009155         184.000       197.307       .64485       189.336       11.7123       .008838         185.000       209.024       .67945       191.746       11.7294       .008236         187.000       232.482       .74762       196.553       11.7375       .007950         188.000       244.224       .78120       198.950       11.7453       .007406 <tr< td=""><td>173.000</td><td>69.083</td><td>.24014</td><td>162.494</td><td>11.5935</td><td>.013051</td></tr<>	173.000	69.083	.24014	162.494	11.5935	.013051
176.000       103.920       .35507       169.881       11.6306       .011723         177.000       115.556       .39260       172.331       11.6422       .011314         178.000       127.204       .42975       174.776       11.6533       .010921         179.000       138.863       .46652       177.215       11.6640       .010541         180.000       150.532       .50291       179.649       11.6744       .010176         181.000       162.211       .53893       182.078       11.6844       .009823         182.000       173.900       .57460       184.502       11.6940       .009483         183.000       185.599       .60990       186.921       11.7033       .009155         184.000       197.307       .64485       189.336       11.7123       .00838         185.000       209.024       .67945       191.746       11.7210       .008532         186.000       220.749       .71371       194.151       11.7294       .008236         187.000       232.482       .74762       196.553       11.7453       .007673         189.000       244.224       .78120       198.950       11.7453       .007673 <tr< td=""><td>174.000</td><td>80.683</td><td>.27885</td><td>164.962</td><td>11.6063</td><td>.012591</td></tr<>	174.000	80.683	.27885	164.962	11.6063	.012591
177.000       115.556       .39260       172.331       11.6422       .011314         178.000       127.204       .42975       174.776       11.6533       .010921         179.000       138.863       .46652       177.215       11.6640       .010541         180.000       150.532       .50291       179.649       11.6744       .010176         181.000       162.211       .53893       182.078       11.6844       .009823         182.000       173.900       .57460       184.502       11.6940       .009483         183.000       185.599       .60990       186.921       11.7033       .009155         184.000       197.307       .64485       189.336       11.7123       .008838         185.000       209.024       .67945       191.746       11.7210       .008532         186.000       220.749       .71371       194.151       11.7294       .008236         187.000       232.482       .74762       196.553       11.7375       .007950         188.000       244.224       .78120       198.950       11.7453       .007406         190.000       267.729       .84738       203.731       11.7601       .007147 <t< td=""><td>175.000</td><td>92.295</td><td>.31716</td><td>167.424</td><td>11.6187</td><td>.012149</td></t<>	175.000	92.295	.31716	167.424	11.6187	.012149
178.000       127.204       .42975       174.776       11.6533       .010921         179.000       138.863       .46652       177.215       11.6640       .010541         180.000       150.532       .50291       179.649       11.6744       .010176         181.000       162.211       .53893       182.078       11.6844       .009823         182.000       173.900       .57460       184.502       11.6940       .009483         183.000       185.599       .60990       186.921       11.7033       .009155         184.000       197.307       .64485       189.336       11.7123       .008838         185.000       209.024       .67945       191.746       11.7210       .008532         186.000       220.749       .71371       194.151       11.7294       .008236         187.000       232.482       .74762       196.553       11.7375       .007950         188.000       244.224       .78120       198.950       11.7453       .007673         189.000       255.973       .81445       201.343       11.7528       .007406         190.000       267.729       .84738       203.731       11.7601       .007147 <t< td=""><td>176.000</td><td>103.920</td><td>.35507</td><td>169.881</td><td>11.6306</td><td>.011723</td></t<>	176.000	103.920	.35507	169.881	11.6306	.011723
179.000       138.863       .46652       177.215       11.6640       .010541         180.000       150.532       .50291       179.649       11.6744       .010176         181.000       162.211       .53893       182.078       11.6844       .009823         182.000       173.900       .57460       184.502       11.6940       .009483         183.000       185.599       .60990       186.921       11.7033       .009155         184.000       197.307       .64485       189.336       11.7123       .008838         185.000       209.024       .67945       191.746       11.7210       .008532         186.000       220.749       .71371       194.151       11.7294       .008236         187.000       232.482       .74762       196.553       11.7375       .007950         188.000       244.224       .78120       198.950       11.7453       .007673         189.000       255.973       .81445       201.343       11.7528       .007406         190.000       267.729       .84738       203.731       11.7601       .007147         191.000       279.493       .87998       206.116       11.7739       .006896 <t< td=""><td>177.000</td><td>115.556</td><td>.39260</td><td>172.331</td><td>11.6422</td><td>.011314</td></t<>	177.000	115.556	.39260	172.331	11.6422	.011314
180.000       150.532       .50291       179.649       11.6744       .010176         181.000       162.211       .53893       182.078       11.6844       .009823         182.000       173.900       .57460       184.502       11.6940       .009483         183.000       185.599       .60990       186.921       11.7033       .009155         184.000       197.307       .64485       189.336       11.7123       .008838         185.000       209.024       .67945       191.746       11.7210       .008532         186.000       220.749       .71371       194.151       11.7294       .008236         187.000       232.482       .74762       196.553       11.7375       .007950         188.000       244.224       .78120       198.950       11.7453       .007673         189.000       255.973       .81445       201.343       11.7528       .007406         190.000       267.729       .84738       203.731       11.7601       .007147         191.000       279.493       .87998       206.116       11.7739       .006896         193.000       303.041       .94423       210.875       11.7804       .006417 <t< td=""><td>178.000</td><td>127.204</td><td>.42975</td><td>174.776</td><td>11.6533</td><td>.010921</td></t<>	178.000	127.204	.42975	174.776	11.6533	.010921
181.000       162.211       .53893       182.078       11.6844       .009823         182.000       173.900       .57460       184.502       11.6940       .009483         183.000       185.599       .60990       186.921       11.7033       .009155         184.000       197.307       .64485       189.336       11.7123       .008838         185.000       209.024       .67945       191.746       11.7210       .008532         186.000       220.749       .71371       194.151       11.7294       .008236         187.000       232.482       .74762       196.553       11.7375       .007950         188.000       244.224       .78120       198.950       11.7453       .007673         189.000       255.973       .81445       201.343       11.7528       .007406         190.000       267.729       .84738       203.731       11.7601       .007147         191.000       279.493       .87998       206.116       11.7739       .006896         192.000       291.264       .91226       208.497       11.7739       .006553         193.000       303.041       .94423       210.875       11.7867       .006189 <t< td=""><td>179.000</td><td>138.863</td><td>.46652</td><td>177.215</td><td>11.6640</td><td>.010541</td></t<>	179.000	138.863	.46652	177.215	11.6640	.010541
182.000       173.900       .57460       184.502       11.6940       .009483         183.000       185.599       .60990       186.921       11.7033       .009155         184.000       197.307       .64485       189.336       11.7123       .008838         185.000       209.024       .67945       191.746       11.7210       .008532         186.000       220.749       .71371       194.151       11.7294       .008236         187.000       232.482       .74762       196.553       11.7375       .007950         188.000       244.224       .78120       198.950       11.7453       .007673         189.000       255.973       .81445       201.343       11.7528       .007406         190.000       267.729       .84738       203.731       11.7601       .007147         191.000       279.493       .87998       206.116       11.7671       .006896         192.000       291.264       .91226       208.497       11.7739       .006553         193.000       303.041       .94423       210.875       11.7804       .006417         194.000       314.824       .97589       213.249       11.77867       .006189      <	180.000	150.532	.50291	179.649	11.6744	.010176
183.000       185.599       .60990       186.921       11.7033       .009155         184.000       197.307       .64485       189.336       11.7123       .008838         185.000       209.024       .67945       191.746       11.7210       .008532         186.000       220.749       .71371       194.151       11.7294       .008236         187.000       232.482       .74762       196.553       11.7375       .007950         188.000       244.224       .78120       198.950       11.7453       .007673         189.000       255.973       .81445       201.343       11.7528       .007406         190.000       267.729       .84738       203.731       11.7601       .007147         191.000       279.493       .8798       206.116       11.7671       .006896         192.000       291.264       .91226       208.497       11.7739       .006653         193.000       303.041       .94423       210.875       11.7804       .006189         195.000       326.614       1.00724       215.619       11.7928       .005968         196.000       338.410       1.03830       217.986       11.7987       .005754 <td>181.000</td> <td>162.211</td> <td>•53893</td> <td>182.078</td> <td>11.6844</td> <td>.009823</td>	181.000	162.211	•53893	182.078	11.6844	.009823
184.000       197.307       .64485       189.336       11.7123       .008838         185.000       209.024       .67945       191.746       11.7210       .008532         186.000       220.749       .71371       194.151       11.7294       .008236         187.000       232.482       .74762       196.553       11.7375       .007950         188.000       244.224       .78120       198.950       11.7453       .007673         189.000       255.973       .81445       201.343       11.7528       .007406         190.000       267.729       .84738       203.731       11.7601       .007147         191.000       279.493       .8798       206.116       11.7671       .006896         192.000       291.264       .91226       208.497       11.7739       .006553         193.000       303.041       .94423       210.875       11.7804       .006417         194.000       314.824       .97589       213.249       11.7867       .006189         195.000       326.614       1.00724       215.619       11.7987       .005968         196.000       338.410       1.03830       217.986       11.7987       .005754 <td>182.000</td> <td>173.900</td> <td>•57460</td> <td>184.502</td> <td>11.6940</td> <td>.009483</td>	182.000	173.900	•57460	184.502	11.6940	.009483
184.000       197.307       .64485       189.336       11.7123       .008838         185.000       209.024       .67945       191.746       11.7210       .008532         186.000       220.749       .71371       194.151       11.7294       .008236         187.000       232.482       .74762       196.553       11.7375       .007950         188.000       244.224       .78120       198.950       11.7453       .007673         189.000       255.973       .81445       201.343       11.7528       .007406         190.000       267.729       .84738       203.731       11.7601       .007147         191.000       279.493       .87998       206.116       11.7671       .006896         192.000       291.264       .91226       208.497       11.7739       .006553         193.000       303.041       .94423       210.875       11.7804       .006417         194.000       314.824       .97589       213.249       11.7867       .006189         195.000       326.614       1.00724       215.619       11.7987       .005754	183.000	185.599	.60990	186.921	11.7033	.009155
185.000       209.024       .67945       191.746       11.7210       .008532         186.000       220.749       .71371       194.151       11.7294       .008236         187.000       232.482       .74762       196.553       11.7375       .007950         188.000       244.224       .78120       198.950       11.7453       .007673         189.000       255.973       .81445       201.343       11.7528       .007406         190.000       267.729       .84738       203.731       11.7601       .007147         191.000       279.493       .87998       206.116       11.7671       .006896         192.000       291.264       .91226       208.497       11.7739       .006553         193.000       303.041       .94423       210.875       11.7804       .006417         194.000       314.824       .97589       213.249       11.7867       .006189         195.000       326.614       1.00724       215.619       11.7928       .005968         196.000       338.410       1.03830       217.986       11.7987       .005754	184.000	197.307	.64485		11.7123	.008838
186.000       220.749       .71371       194.151       11.7294       .008236         187.000       232.482       .74762       196.553       11.7375       .007950         188.000       244.224       .78120       198.950       11.7453       .007673         189.000       255.973       .81445       201.343       11.7528       .007406         190.000       267.729       .84738       203.731       11.7601       .007147         191.000       279.493       .87998       206.116       11.7671       .006896         192.000       291.264       .91226       208.497       11.7739       .006553         193.000       303.041       .94423       210.875       11.7804       .006417         194.000       314.824       .97589       213.249       11.7867       .006189         195.000       326.614       1.00724       215.619       11.7928       .005968         196.000       338.410       1.03830       217.986       11.7987       .005754	185.000		.67945	191.746	11.7210	.008532
187.000       232.482       .74762       196.553       11.7375       .007950         188.000       244.224       .78120       198.950       11.7453       .007673         189.000       255.973       .81445       201.343       11.7528       .007406         190.000       267.729       .84738       203.731       11.7601       .007147         191.000       279.493       .87998       206.116       11.7671       .006896         192.000       291.264       .91226       208.497       11.7739       .006553         193.000       303.041       .94423       210.875       11.7804       .006417         194.000       314.824       .97589       213.249       11.7867       .006189         195.000       326.614       1.00724       215.619       11.7928       .005968         196.000       338.410       1.03830       217.986       11.7987       .005754	186.000	220.749	.71371	194.151	11.7294	.008236
189.000       255.973       .81445       201.343       11.7528       .007406         190.000       267.729       .84738       203.731       11.7601       .007147         191.000       279.493       .87998       206.116       11.7671       .006896         192.000       291.264       .91226       208.497       11.7739       .006553         193.000       303.041       .94423       210.875       11.7804       .006417         194.000       314.824       .97589       213.249       11.7867       .006189         195.000       326.614       1.00724       215.619       11.7928       .005968         196.000       338.410       1.03830       217.986       11.7987       .005754	187.000		.74762	196.553	11.7375	.007950
189.000       255.973       .81445       201.343       11.7528       .007406         190.000       267.729       .84738       203.731       11.7601       .007147         191.000       279.493       .87998       206.116       11.7671       .006896         192.000       291.264       .91226       208.497       11.7739       .006653         193.000       303.041       .94423       210.875       11.7804       .006417         194.000       314.824       .97589       213.249       11.7867       .006189         195.000       326.614       1.00724       215.619       11.7928       .005968         196.000       338.410       1.03830       217.986       11.7987       .005754	188.000	244.224	.78120	198.950	11.7453	.007673
191.000       279.493       .87998       206.116       11.7671       .006896         192.000       291.264       .91226       208.497       11.7739       .006653         193.000       303.041       .94423       210.875       11.7804       .006417         194.000       314.824       .97589       213.249       11.7867       .006189         195.000       326.614       1.00724       215.619       11.7928       .005968         196.000       338.410       1.03830       217.986       11.7987       .005754	189.000	255.973	.81445	201.343	11.7528	.007406
192.000     291.264     .91226     208.497     11.7739     .006653       193.000     303.041     .94423     210.875     11.7804     .006417       194.000     314.824     .97589     213.249     11.7867     .006189       195.000     326.614     1.00724     215.619     11.7928     .005968       196.000     338.410     1.03830     217.986     11.7987     .005754	190.000	267.729	.84738	203.731	11.7601	-007147
192.000     291.264     .91226     208.497     11.7739     .006653       193.000     303.041     .94423     210.875     11.7804     .006417       194.000     314.824     .97589     213.249     11.7867     .006189       195.000     326.614     1.00724     215.619     11.7928     .005968       196.000     338.410     1.03830     217.986     11.7987     .005754	191.000	279.493	.87998	206.116	11.7671	. 006896
194.000       314.824       .97589       213.249       11.7867       .006189         195.000       326.614       1.00724       215.619       11.7928       .005968         196.000       338.410       1.03830       217.986       11.7987       .005754	192.000		.91226		11.7739	.006653
194.000       314.824       .97589       213.249       11.7867       .006189         195.000       326.614       1.00724       215.619       11.7928       .005968         196.000       338.410       1.03830       217.986       11.7987       .005754	193.000	303.041	. 94423	210.875	11.7804	.006417
195.000     326.614     1.00724     215.619     11.7928     .005968       196.000     338.410     1.03830     217.986     11.7987     .005754						
196.000 338.410 1.03830 217.986 11.7987 .005754						
	197.000	350.211	1.06905	220.349	11.8043	.005546

## NF3 ISOCHORE AT 21.000 MOL/L

Y V	0.010	*9	00.400	Ph 10 4 Fb 57	000 1070
T, K	P,BAR	Z	DP/00	OP/DT	D2P/DT2
153.700	1.894	.00706	198.018	14.0671	.015907
154.000	6.117	.02275	198.935	14.0719	.015720
155.000	20.196	.07463	201.983	14.0873	.015114
156.000	34.291	.12589	205.024	14.1021	.014532
157.000	48.400	. 17656	208.056	14.1163	.013974
158.000	62.524	. 22664	211.080	14.1300	.013437
159.000	76.660	.27613	214.096	14.1432	.012921
160.000	90.810	.32506	217.105	14.1559	.012425
161.000	104.972	.37342	220.106	14.1681	.011947
162.000	119.146	.42122	223.101	14.1798	.011488
163.000	133.331	.46848	226.089	14.1911	. 011045
164.000	147.528	•51520	229.070	14.2019	.010618
165.000	161.735	.56139	232.044	14.2123	.010206
166.000	175.952	.60706	235.012	14.2223	.009809
167.000	190.180	.65222	237.975	14.2319	.009426
168.000	204.416	.69687	240.931	14.2412	.009056
169.000	218.662	.74102	243.881	1 4. 2500	.008699
170.000	232.916	.78468	246.826	14.2586	.008354
171.000	247.179	.82787	249.765	14.2668	.008020
172.000	261.449	.87057	252.698	14.2746	.007698
173.000	275.728	.91281	255.627	14.2822	.007386
174.000	290.014	.95458	258.550	14.2894	.007084
175.000	304.307	.99590	261.468	14-2963	.006792
176.000	318.606	1.03678	264.381	14.3030	.006509
177.000	332.912	1.07721	267.290	14.3093	.006236
178.000	347.225	1.11721	270.193	14.3154	.005970

## NF3 ISOCHORE AT 22.000 MOL/L

		490	00.400	00.408	020/072
ToK	P.BAR	Z	DP/DD	DP/DT	D2P/DT2
139.023	.700	.00275	260.017	17.2235	.015949
140.000	17.541	.06850	263.681	17.2387	.015272
141.000	34.787	.13488	267.421	17.2536	.014608
142.000	52.048	.20038	271.151	17.2679	.013970
143.000	69.323	.26502	274.871	17.2816	.013356
144.000	86.611	.32882	278.582	17.2947	.012767
145.000	103.912	.39178	282.284	17.3071	.012200
146.000	121.225	. 45392	285.976	17.3191	.011654
147.000	138.550	.51526	289.661	17.3305	.011129
148.000	155.886	.57582	293.336	17.3413	.010623
149.000	173.232	.63560	297.004	17.3517	.010135
150.000	190.589	.69462	300.663	17.3616	.009666
151.000	207.955	.75290	304.315	17.3710	.009213
152.000	225.331	.81044	307.959	17.3800	.008776
153.000	242.715	.86726	311.596	17.3886	.008354
154.000	260.108	.92337	315.225	17.3967	-007947
155.000	277.509	.97878	318.848	17.4045	.007554
156.000	294.917	1.03351	322.463	17.4119	- 007174
157.000	312.332	1.08757	326.071	17.4188	.006807
158.000	329.754	1.14097	329.673	17.4255	.006453
159.000	347.183	1.19372	333.268	17.4318	.006110

Table 11. Continued.

# NF3 ISOCHORE AT 23.000 HOL/L

T, K	P,BAR	Z	DP/00	DP/DT	D2P/DT2
123.448	.182	.00077	338.197	21.1699	.016196
124.000	11.861	.05002	340.779	21.1787	.015729
125.000	33.048	.13825	345.451	21.1940	.014908
126.000	54.249	.22514	350.109	21.2085	. 014121
127.000	75.465	.31072	354.755	21.2223	.013365
128.000	96.693	.39502	359.389	21.2353	.012640
129.000	117.935	.47807	364.012	21.2475	.011944
130.000	139.188	• 55988	368.622	21.2592	.011276
131.000	160.453	.64049	373.222	21.2701	.010633
132.000	181.728	.71992	377.810	21.2804	• 010015
133.000	203.014	.79820	382.388	21.2901	.009420
134.000	224.308	.87534	386.956	21.2993	.008848
135.000	245.612	•95138	391.513	21.3078	.008298
136.000	266.924	1.02632	396.060	21.3159	.007768
137.000	288.244	1.10021	400.597	21.3234	.007257
138.000	309.571	1.17305	405.124	21.3304	.006765
139.000	330.904	1.24487	409.642	21.3369	.006290
140.000	352.244	1.31568	414.151	21.3430	.005833

## NF3 ISOCHORE AT 24.000 MOL/L

T <sub>2</sub> K	P.BAR	Z	DP/00	DP/DT	D2P/DT2
107.074	.027	.00013	438.669	26.1953	•016748
108.000	24.303	.11277	444.203	26.2103	。015713
109.000	50.521	.23227	450.159	26.2255	.014644
110.000	76.753	.34967	456.097	26.2396	.013621
111.000	103.000	.46501	462.019	26.2527	.012643
112.000	129.259	.57835	467.923	26.2649	.011707
113.000	155.529	.68974	473.812	26.2762	.010811
114.000	181.811	.79922	479.684	26.2866	. 009953
115.000	208.102	.90684	485.542	26.2961	.009130
116.000	234.403	1.01264	491.383	26.3048	.008342
117.000	260.711	1.11667	497.211	26.3128	.007586
118.000	287.028	1.21897	503.023	26.3200	.006860
119.000	313.351	1.31958	508.821	26.3265	.006164
120.000	339.681	1.41854	514.606	26.3323	.005496

Table 11. Continued.

## NF3 ISOCHORE AT 25.000 HOL/L

T <sub>2</sub> K	P.BAR	Z	DP/DD	DP/DT	D2P/DT2
89.971	.002	.00001	571.934	32.7759	.017810
90.000	. 959	.00513	572.165	32.7765	.017761
91.000	33.744	.17840	580.059	32.7934	.016110
92.000	66.546	.34798	587.925	32.8087	.014542
93.000	99.361	•51399	595.764	32.8225	.013051
94.000	132.190	• 676 <u>5</u> 4	603.578	32.8348	.011633
95.000	165.030	.83573	611.365	32.8458	.010283
96.000	197.881	.99165	619.128	32.8554	.008999
97.000	230.741	1.14440	626.867	32.8638	.007775
98.000	263.608	1.29407	634.582	32.8710	.006608
99.000	296.483	1.44075	642.273	32.8770	.005496
100.000	329.362	1.58452	649.942	32.8820	.004435

### NF3 ISOCHORE AT 26.000 MOL/L

					20212
T.K	P.BAR	Z	DP/00	DP/DT	D2P/DT2
	• -		757 400	64 7005	040964
72.183	.000	.00000	757.199	41.7825	.019864
	7. 4.70	04677	766.216	41.7978	.017536
73.000	34.139	.21633	100.510	410 1210	
7. 000	75.945	.47474	777.209	41.8140	014839
74.000	790949	04(4(4			
75.000	117.766	.72635	788.154	41.8275	.012301
194000					00.0044
76.000	159.599	. 97142	799.053	41.8386	.009911
			000 000	41.8474	.007658
77.000	201.442	1.21018	809.905	41.04/4	. 00/000
	017 007	1.44287	820.716	41.8540	.005534
78.000	243.293	1044501	0500110	_	
79.000	285.150	1.66969	831.482	41.8585	.003530
79.000	2030730				
80.000	327.010	1.89087	842.206	41.8611	.001638
00.000	OCIDATA	7 00001	0.0000		

### TABLE 12. Calculated $P(\rho)$ Isotherms

The following pages give P(p) isotherms, as computed by the equation of state (6). The third column DP/DD is the isotherm slope ( $\partial P/\partial \rho$ ) in units of the bar and mol/L. The last two columns give the isochore slopes and curvatures, DP/DT = ( $\partial P/\partial T$ ), D2P/DT2 = ( $\partial^2 P/\partial T^2$ ) in units of the bar and kelvins.

These tables show that  $\partial P/\partial \rho$  is non-negative, and that it increases monotonically with density.

Table 12. Calculated  $P(\rho)$  Isotherms.

	NF3 IS	OTHERM AT	80.00	K	
MOL/L	P.BAR	Z	09/00	DP/DT	D2P/DT2
.000	.000	.99997	6.651	.0000	000000
25.565	.000	.00000	668.426	37.4843	.018796
25.580	9.943	.05844	673.736	37.6250	.018230
25.600	23.490	.13795	680.965	37.8157	.017465
25.620	37.182	.21818	688.267	38.0075	. 016698
25.640	51.021	. 299.16	695.642	38.2003	.015929
25.660	65.008	.38088	703.091	38.3941	.015158
25.680	79.145	• 46334	710.616	38.5891 ,	.014385
25.700	93.431	•54655	718.216	38.7850	.013610
25.720	107.873	.63054	725.895	38.9821	.012833
25.740	122.468	.71530	733.653	39-1803	.012053
25.760	137.220	.80084	741.490	39.3795	.011270
25.780	152.129	.88716	749.408	39.5799	.010485
25.800	167.197	.97428	757.409	39.7814	.009697
25.820	182.426	1.06220	765.493	39.9841	.008906
25.840	197.818	1.15092	773.661	40.1879	.008112
25.860	213.373	1.24047	781.915	40.3928	.007315
25.880	229.095	1.33084	790.256	40.5990	.006515
25.900	244.984	1.42204	798.686	40.8063	.005711
25.920	261.043	1.51409	807.205	41-0148	.004904
25.940	277.273	1.60698	815.815	41.2245	.004093
25.960	293.676	1.70074	824.518	41.4355	.003279
25.980	310.254	1.79537	833.314	41.6477	.002460
26.000	327.010	1.89087	842-206	41.8611	.001638
26.020	343.943	1.98725	851.195	42.0758	.000811
26.040	361.058	2.08454	860.281	42.2918	000019
26.060	378.355	2.18273	869.467	42.5090	000854
26.080	395.837	2.28183	878.755	42.7276	001693

Table 12. Continued.

## NF3 ISOTHERM AT 100.00 K

MOL/L .001	P.BAR .009	. 99904	DP/DD 8.299	DP/DT . 0001	D2P/DT2 000000
24.419	.009 .702	.00005	489.627 489.972	28.7231 28.7325	. 017112 . 017082
24.440	10.551 20.497	.05192 .10079	494.861 499.791	28.8666	• 016649 • 016217
24.480	30.542	• 15006	504.762	29.1366	• 015785
24.500	40.688	.19974	509.774	29.2725	.015354
24.520	50.934	-24983	514.827	29.4090	.014922
24.540	61.281	.30034	519.923	29.5462	.014490
24.560	71.731	.35127	525.061	29.6839	.014059
24.580	82.284	.40262	530.243	29.8223	. 013627
24.600	92.941	. 45440	535.468	29.9613	. 013195
24.620	103.703	•50660	540.737	30.1009	. 012763
24.640	114.571	•55924	546.050	30.2412	.012330
24.660	125.545	.61231	551.409	30.3821	.011897
24.680	136.627	• 66582	556.814	30.5237	. 011464
24.700	147.818	.71977	562.264	30.6659	.011030
24.720	159.118	.77417	567.761	30.8088	.010596
24.740	170.529	.82901	573.306	30.9523	.010161
24.760	182.051	.88431	578.898	31.0966	.009726
24.780	193.685	.94007	584.539	31.2415	.009290
24.800	205.433	• 99628	590.228	31.3871	.008853
24.820	217.294	1.05296	595.967	31.5333	.008416
24.840	229.272	1.11010	601.756	31.6803	.007978
24.860	241.365	1.16772	607.596	31.8280	.007538
24.880	253.576	1.22580	613.486	31.9764	-007098
24.900	265.905	1.28437	619.429	32.1255	.006657
24.920	278.353	1.34342	625.424	32.2754	•006215
24.940	290.922	1.40296	631.473	32.4259	. 005772
24.960	303.613	1.46298	637.574	32.5772	.005328
24.980	316.425	1.52350	643.731	32.7292	. 004882
25.000 25.020	329.362	1.58452	649.942	32.8820	004435
25.040	342.424 355.611	1.64604 1.70807	656 • 209 662 • 533	33.0355 33.1898	.003987
25.060	368.925			33.3449	.003087
25.080	382.368	1.77060 1.83366	668.913 675.352	33.5007	• 003087
25.100	395.940	1.83723	681.848	33.6573	•002181
C3 0 T 0 0	3770740	T+03153	0010040	33.0513	•005101

Table 12. Continued.

#### NF3 ISOTHERM AT 120.00 K

P.BAR	Z	DP/00	DP/DT	D2P/DT2
.128	.99219	9.823	.0011	000000
.127	.00055	357.601	22.1445	.016284
9.291	.04007	362.014	22.2703	.015924
23.911	.10295	369.028	22.4691	.015361
38.815	.16582	376.143	22.6694	.014801
54.004	.23171	383.362	22.8712	. 014244
69.485	•29762	390.685	23.0746	.013689
85.261	•36456	398.116	23.2797	.013137
101.336	• 43256	405.655	23.4863	.012587
117.715	•50162	413.306	23.6947	.012038
134.402	•57176	421.070	23. 9046	. 011491
151.402	.64299	428.950	24.1163	.010945
168.719	.71532	436.947	24.3297	.010400
186.359	.78877	445.064	24.5449	.009856
204.326	.86336	453.303	24.7619	.009312
222.625	.93910	461.667	24.9806	.008768
241.261	1.01600	470.157	25.2012	.008224
260.239	1.09408	478.778	25.4236	.007680
279.565	1.17336	487.530	25-6479	.007136
299.243	1.25385	496.417	25.8741	.006590
319.280	1.33557	505.441	26.1022	.006044
339.681	1.41854	514.606	26.3323	.005496
360.451	1.50277	523.913	26.5644	.004947
381.596	1.58829	533.367	26.7986	.004396
	.128 .127 9.291 23.911 38.815 54.004 69.485 85.261 101.336 117.715 134.402 151.402 168.719 186.359 204.326 222.625 241.261 260.239 279.565 299.243 319.280 339.681 360.451	.128 .99219  .127 .00055 9.291 .04007 23.911 .10295 38.815 .16682 54.004 .23171 69.485 .29762 85.261 .36456 101.336 .43256 117.715 .50162 134.402 .57176 151.402 .64299 168.719 .71532 186.359 .78877 204.326 .86336 222.625 .93910 241.261 1.01600 260.239 1.09408 279.565 1.17336 299.243 1.25385 319.280 1.33557 339.681 1.41854 360.451 1.50277	.128       .99219       9.823         .127       .00055       357.601         9.291       .04007       362.014         23.911       .10295       369.028         38.815       .16582       376.143         54.004       .23171       383.362         69.485       .29762       390.685         85.261       .36456       398.116         101.336       .43256       405.655         117.715       .50162       413.306         134.402       .57176       421.070         151.402       .64299       428.950         168.719       .71532       436.947         186.359       .78877       445.064         204.326       .86336       453.303         222.625       .93910       461.667         241.261       1.01600       470.157         260.239       1.09408       478.778         279.565       1.17336       487.530         299.243       1.25385       496.417         319.280       1.33557       505.441         339.681       1.41854       514.606         360.451       1.50277       523.913	.128       .99219       9.823       .0011         .127       .00055       357.601       22.1445         9.291       .04007       362.014       22.2703         23.911       .10295       369.028       22.4691         38.815       .16582       376.143       22.6694         54.004       .23171       383.362       22.8712         69.485       .29762       390.685       23.0746         85.261       .36456       398.116       23.2797         101.336       .43256       405.655       23.4863         117.715       .50162       413.306       23.6947         134.402       .57176       421.070       23.5046         151.402       .64299       428.950       24.1163         168.719       .71532       436.947       24.3297         186.359       .78877       445.064       24.5449         22.625       .93910       461.667       24.9806         241.261       1.01600       470.157       25.2012         260.239       1.09408       478.778       25.4236         279.565       1.17336       487.530       25.6479         299.243       1.25385       496.

Table 12. Continued.

## NF3 ISOTHERM AT 140.00 K

MOL/L	P,BAR	Z	DP/00	DP/DT	D2P/DT2
-040	.457	.98179	11.224	.0034	000001
.067	.754	.97015	10.957	.0057	000003
21.935	.754	.00295	255.568	16.9979	. 015940
21.960	7.095	.02775	258.642	17.0894	.015684
22.000	17.541	.06850	263.681	17.2387	. 015272
22.040	28.190	.10988	268.787	17.3890	. 014865
22.080	39.045	.15191	273.959	17.5404	. 014461
22.120	50.108	.19461	279.200	17.6928	.014062
22.160	61.382	.23796	284.510	17.8462	.013666
22.200	72.869	.28199	289.891	18.0008	.013273
22.240	84.574	.32669	295.343	18.1565	.012884
22.280	96.498	.37208	300.867	18.3132	. 012497
22.320	108.644	•41817	306.466	18.4711	.012113
22.360	121.016	.46495	312.139	18.6302	. 011732
22.400	133.616	.51245	317.888	18.7904	.011353
22.440	146.448	• 56065	323.715	18.9517	. 010976
22.480	159.514	.60959	329.620	19.1143	.010601
22.520	172.818	•65926	335.605	19.2781	.010228
22.560	186.364	.70967	341.671	19.4431	.009856
22.600	200.153	.76083	347.820	19.6093	.009486
22.640	214.190	.81275	354.052	19.7768	.009118
22.680	228.479	.86544	360.370	19.9455	.008750
22.720	243.021	.91891	366.774	20.1155	.008383
22.760	257.822	.97316	373.266	20.2868	.008018
22.800	272.884	1.02820	379.848	20.4595	. 007653
22.840	288.211	1.08405	386.520	20.6335	.007288
22.880	303.807	1.14071	393.285	20.8088	.006924
22.920	319.675	1.19820	400.145	20.9855	.006560
22.960	335.820	1.25652	407.099	21.1635	.006197
23.000	352.244	1.31568	414.151	21.3430	.005833
23.040	368.953	1.37570	421.302	21.5239	.005469
23.080	385.950	1.43658	428.554	21.7062	.005105

Table 12. Continued.

NF3 ISOTHERM AT 160.00 k	NF	3	ISOT	HERM	AT	160.	0.0	K
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MOL/L •040 •080 •120 •160 •200 •222	P,BAR .524 1.034 1.530 2.013 2.482 2.730	2 •98538 •97180 •95860 •94560 •93272 •92578	DP/DD 12.924 12.573 12.230 11.892 11.554 11.371	DP/DT • 0034 • 0068 • 0103 • 0139 • 0176 • 0197	D2P/DT2000000000002000005000010000019000026
20.549 20.560 20.600 20.640 20.680 20.720 20.760 20.800	2.730 4.697 11.779 19.005 26.377 33.895 41.563 49.382	.00999 .01717 .04298 .06922 .09588 .12297 .15050	174.284 175.280 178.849 182.462 186.121 189.827 193.578	12.8485 12.8800 12.9923 13.1053 13.2191 13.3335 13.4487	.015943 .015848 .015514 .015186 .014862 .014543 .014229
20.840 20.880 20.920 20.960 21.000 21.040 21.080	57.354 65.481 73.764 82.207 90.810 99.576	.20688 .23574 .26505 .29482 .32506 .35576	201.224 205.120 209.065 213.060 217.105 221.201 225.350	13.6814 13.7988 13.9171 14.0361 14.1559 14.2765 14.3979	.013613 .013311 .013012 .012717 .012425 .012136
21.120 21.160 21.200 21.240 21.280 21.320	117.605 126.872 136.310 145.921 155.709 165.674	.41858 .45070 .48332 .51643 .55003	229.551 233.805 238.113 242.476 246.895 251.370	14.5202 14.6432 14.7672 14.8919 15.0175	.011567 .011287 .011009 .010733 .010459 .010188
21.360 21.400 21.440 21.480 21.520 21.560 21.600	175.819 186.147 196.659 207.359 218.248 229.329 240.604	.61874 .65386 .68950 .72566 .76234 .79956	255.902 260.492 265.140 269.848 274.616 279.445 284.337	15.2714 15.3997 15.5289 15.6589 15.7899 15.9219	.009918 .009650 .009384 .009120 .008857 .008595
21.640 21.680 21.720 21.760 21.800 21.840	252.076 263.748 275.622 287.700 299.986 312.482	.87563 .91448 .95389 .99386 1.03440 1.07551	289.291 294.308 299.391 304.539 309.753 315.035	16.1886 16.3234 16.4591 16.5959 16.7336 16.8724	.008076 .007817 .007560 .007304 .007048 .006793
21.880 21.920 21.960 22.000 22.040 22.080	325.190 338.113 351.255 364.618 378.205 392.018	1.11721 1.15949 1.20236 1.24583 1.28991 1.33460	320.385 325.805 331.295 336.857 342.491 348.198	17.0122 17.1530 17.2948 17.4377 17.5817 17.7267	.006539 .006285 .006032 .005779 .005526

Table 12. Continued.

NF3	ISOT	HERM	AT	180.00	K
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MOL/L .080 .160 .240 .320 .400 .480 .560	P,BAR 1.170 2.289 3.361 4.387 5.366 6.299 7.186 7.261	7 • 976 95 • 955 99 • 935 77 • 915 94 • 8 96 34 • 8 76 86 • 8 5 7 4 3 • 8 5 5 7 5	DP/DD 14.299 13.694 13.107 12.529 11.954 11.377 10.797	OP/DT .0068 .0138 .0210 .0286 .0365 .0448 .0535 .0543	D2P/DT2 000001 000004 000012 000025 000047 000081 000135 000141
18.993	7.261	.02554	108.713	9.4148	.016306
19.040	12.409	.04355	111.531	9.5122	.015956
19.120	21.528	.07523	116.453	9.6803	.015378
19.200	31.045	.10804	121.501	9.8504	.014824
19.280	40.971	.14199	126.679	10.0226	.014291
19.360	51.317	.17711	131.990	10.1969	.013778
19.440	62.093	.21342	137.436	10.3734	.013282
19.520	73.311	.25095	143.022	10.5522	.012802
19.600	84.981	-28970	148.751	10.7332	.012336
19.680	97.115	• 32972	154.625	10.9165	-011882
19.760	109.725	.37103	160.648	11.1023	.011441
19.840	122.823	• 41 364	166.825	11.2905	. 011010
19.920	136.421	•45760	173.157	11.4811	.010589
20.000	150.532	•50291	179.649	11.6744	.010176
20.080	165.169	•54961	186.305	11.8702	.009771
20.160	180.345	•59773	193.129	12.0687	.009373
20.240	196.074	.64729	200.125	12.2699	.008981
20.320	212.370	.69833	207.296	12.4738	.008595
20.400	229.246	.75087	214.647	12.6806	.008214
20.480	246.718	.80494	222.183	12.8902	.007837
20.560	264.801	.86057	229.907	13.1028	. 007465
20.640	283.509	•91780	237.826	13.3184	.007096
20.720	302.858	• 97665	245.942	13.5370	.006729
20.800	322.865	1.03717	254.262	13.7587	.006366
20.880	343.546	1.09937	262.791	13.9835	.006004
20.960	364.917	1.16331	271.534	14.2116	.005644
21.040	386.997	1.22900	280.495	14.4430	.005285

Table 12. Continued.

NF3 ISOTHERM AT 200.00	ł K
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1404 44		-			
MOL/L	P,BAR	Z	DP/DD	OP/DT	D2P/DT2
•160	2.564	.96361	15.467	· 0137	000003
.320	4.955	.93120	14.432	.0283	000013
.480	7.184	.90001	13.428	.0438	000035
.640	9.253	.86943	12.438	.0603	000073
.800	11.164	.83921	11.454	.0779	000135
.960	12.919	.80924	10.477	. 1968	000233
1.120	14.517	.77947	9.505	.1169	000389
1.259	15.776	.75380	8.666	.1357	000612
		0.5000	0,000	42031	* * * * * * * * * * * * * * * * * * * *
17.133	15.776	.05537	56.440	6.4883	.017312
17.280	24.487	.08522	51.848	6.7065	.016211
17.440	34.874	.12025	68.044	6.9487	.015149
17.600	46.280	.15813	74.592	7.1968	. 014196
17.760	58.763	.19897	81.509	7.4510	.013330
17.920	72.383	.24290	88.810	7.7118	.012534
18.080	87.204	.29005	96.513	7.9793	. 011794
18.240	103.290	.34054	104.636	8.2538	.011100
18.400	120.718	.39451	113.195	8.5357	.010444
18.560	139.536	.45211	122.210	8.8252	.009820
18.720	159.843	.51348	131.700	9.1226	.009223
18.880	181.707	•57877	141.686	9.4281	.008647
19.040	205.210	.64813	152.190	9.7421	.008088
19.200	230.436	.72174	163.233	10.0648	.007545
19.360	257.475	.79977	174.839	10.3965	.007013
19.520	286.416	.88237	187.034	10.7376	.006491
19.680	317.358	.96975	199.843	11.0883	.005975
19.840	350.401	1.06208	213.295	11.4491	.005465
20.000	385.648	1.15957	227.419	11.8201	.004958

Table 12. Continued.

NF3 ISOTHERM AT 220.00	J K
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MOL/L	P.BAR	Z	OP/00	DP/DT	D2P/DT2
.160	2.837	.96949	17.226	.0137	000002
.320	5.518	.94275	16.295	.0281	000008
.480	8.054	.91725	15.400	.0432	000021
.640	10.447	.89240	14.523	.0592	000041
.800	12.702	.86798	13.659	.0760	000070
• 960	14.819	.84387		• 0936	000109
1.120	16.800	•82005	12.806 11.967		000109
				•1121	
1.280	18.649	• 79649	11.142	.1314	000227
1.440	20.367	.77321	10.335	.1515	000309
1.600	21.957	.75022	9.546	.1725	000413
1.760	23.423	.72755	8.778	.1944	000542
1.920	24.767	.70520	8.033	.2171	000703
2.080	25.994	.68321	7.310	.2408	000909
2.240	27.108	.66158	6.612	• 2655	001175
2 - 400	28.111	•64034	5.938	.2912	001532
2.560	29.009	•61949	5.287	.3181	002038
2.720	29.804	•59903	4.658	• 3465	002815
2.753	29.954	.59491	4.532	• 3525	003029
14.525	29.954	.11274	17.219	3.8455	• 02 08 20
14.560	30.570	•11478	17.733	3.8768	•020389
14.720	33.600	•12479	20.172	4.0210	.018682
14.880	37.034	.13606	22.791	4. 1685	.017293
15.040	40.903	.14868	25.599	4.3195	.016132
15.200	45.237	.16270	28.609	4.4745	.015140
15.360	50.069	.17820	31.828	4.6336	.014276
15.520	55.434	.19526	35.268	4.7972	.013512
15.680	61.367	.21396	38.938	4-9653	.012827
15.840	67.907	.23437	42.851	5.1382	.012204
16.000	75.093	• 25658	47.015	5.3160	.011633
16.160	82.966	.28067	51.443	5.4989	.011103
16.320	91.569	.30674	56.146	5.6871	.010607
16.480	100.948	.33487	61.135	5.8807	. 01 0140
16.640	111.148	.36517	66.423	6.0800	.009696
16.800	122.220	.39772	72.023	6.2850	.009273
16.960	134.213	.43262	77.947	6.4959	.008865
17.120	147.181	.46999	84.209	6.7129	.008472
17.280	161.179	•50992	90.822	6.9362	.008089
17.440	176.263	•55253	97.802	7.1660	.007717
17.600	192.495	•59793	105.163	7.4024	.007352
17.760	209.937	.64623	112.921	7.6456	.006994
17.920	228.652	•69756	121.093	7.8958	. 006641
18.080	248.709	.75203	129.694	8.1532	.006291
18.240	270.178	.80978	138.744	8.4181	.005945
18.400	293.132	.87094	148.260	8.6905	.005600
18.560	317.647	• 93564	158.262	8-9709	.005257
18.720	343.803	1.00403	168.771	9.2593	.004913
18.880	371.682	1.07625	179.808	9.5560	.004569
101000	0.74005	200.002	2173000	707700	4 4 4 7 0 J

Table 12. Continued.

## NF3 ISOTHERM AT 230.00 K

MOL/L •320 •640 •960 1.280 1.600 1.920 2.240 2.560	P.BAR 5.799 11.038 15.750 19.952 23.664 26.908 29.715 32.114	2 • 94756 • 90184 • 85791 • 81511 • 77339 • 73286 • 69368 • 65597	DP/DD 17.216 15.540 13.920 12.354 10.855 9.439 8.117 6.895	DP/DT .0280 .0589 .0927 .1294 .1691 .2115 .2567 .3045	D2P/DT2 000007 000033 000084 000167 000288 000453 000674 000965
2.880 3.200	34.139 35.823	.61985 .58539	5.778 4.764	• 3548 • 4075	001349 001867
3.520	37.198 38.298	•55261 •52153	3.852 3.036	•4625 •5200	002595 003696
4.160	39.151	•49213	2.309	.5803	005610
4.480	39.785	. 46438	1.664	.6448	010056
4.557	39.907	•45797	1.519	.6614	012244
12.155	39.907	.17168	3.557	2.4239	.030952
12.160	39.924	.17169	3.578	2.4265	.030791
12.480	41.312	.17310	5.152	2.6017	. 023437
12.800	43.258	.17672	7.073	2.7853	.019405
13.120	45.882	.18287	9.394	2.9799	.016816
13.440	49.319	•19189	12.169	3.1869	014982
13.760	53.725	.20417 .22013	15.455 19.310	3.4076 3.6430	•013590 •012476
14.400	59.271 66.151	.24022	23.797	3.8939	.011545
14.720	74.576	.26493	28.981	4.1613	. 01 07 41
15.040	84.781	• 29477	34.933	4.4460	.010024
15.360	97.022	.33031	41.725	4.7490	.009370
15.680	111.583	.37212	49.437	5.0712	.008761
16.000	128.769	.42085	58.150	5.4135	.008182
16.320	148.915	.47715	67.952	5.7771	.007625
16.640	172.384	.54173	78.939	6.1629	.007082
16.960	199.573	.61533	91.210	6.5722	.006547
17.280	230.908	.69876	104.874	7.0061	.006016
17.600	266.853	.79286	120.047	7.4660	.005483
17.920	307.912	.89851	136.854	7.9533	.004946
18.240	354.629	1.01668	155.433	8.4694	.004401

# NF3 ISOTHERM AT 234.00 K

HOL/L	P.BAR	Z	00/00	DP/DT	D2P/DT2
.320	5.910	.94934	17.583	•0280	000006
•640	11.273	.90531	15.943	• 0587	000030
.960	16.120	.86305	14.360	• 0923	000077
1.280	20.469	.82191	12.829	.1288	000150
1.600	24.338	.78182	11.365	.1680	000255
1.920	27.751	.74289	9.982	• 2098	000395
2.240	30.736	.70526	8.692	. 2542	000575
2.560	33.324	•66907	7.501	.3010	000800
2.880	35.548	.63441	6.412	.3500	001078
3.200	37.439	.60134	5 • 425	-4010	001416
3.520	39.030	•56991	4.537	• 4539	001829
3.840	40.353	.54012	3.745	•5084	002333
4.160	41.437	•51197	3.044	• 5644	002954
4.480	42.310	• 48542	2.428	.6217	003730
4.800	42.999	.46044	1.892	.6801	004722
5.120	43.529	• 43698	1.432	•7394	006026
5.440	43.923	•41500	1.042	• 7995	007806
5.760	44.204	. 39444	.720	.8600	010361
6.080	44.391	•37527	• 463	• 9208	014269
6.400	44.506	.35743	• 268	.9816	020779
6.720	44.569	.34089	•132	1.0419	032965
7.040	44.597	• 32559	•050	1.1012	060115
7.360	44.606	.31150	-012	1.1583	142093
7.680	44.607	•29853	.001	1.2114	669850
8.000	44.607	.28659	.000	1.2549	8.490979
8.320	44.607	.27557	.002	1.3044	• 430249
8.640	44.610	.26538	.014	1.3622	.166301
8 • 960	44.618	• 25595	.046	1.4268	. 093647
9.280	44.642	• 24726	.111	1.4982	• 06 25 0 3
9.600	44.694	.23929	•223	1.5765	.046005
9.920	44.792	.23208	<ul><li>401</li></ul>	1.6622	.036094
10.240	44.960	.22567	• 665	1. 7556	.029618
10.560	45.230	.22014	1.039	1.8573	. 025125
10-880	45.640	.21561	1.550	1.9678	.021862
11.200	46.239	.21220	2.227	2.0876	.019402
11.520	47.087	.21008	3.104	2.2173	.017492
11.840	48.251	.20946	4.217	2.3576	• 015967
12.160	49.815	.21056	5.605	2.5090	.014721
12.480	51.873	.21363	7.311	2.6722	.013679
12.800	54.533	.21898	9.381	2.8477	.012790
13.120	57.921	.22691	11.864	3.0364	. 01 20 16
13.440	62.175	.23778	14.811	3.2389	.011329
13.760	67.455	•25197	18.279	3.4558	-010707
14.080	73.936	·26990	22.327	3.6879	. 01 01 36
14.400	81.813	.29202	27.016	3.9360	.009602
14.720	91.302	.31880	32.414	4.2008	• 009096
15.040	102.641	• 35077	38.589	4.4831	.008609
15.360	116.090	•38846	45.616	4.7839	.008137
15.680	131.934	•43247	53.574	5.1039	.007673
16.000	150.485	.48342	62.546	5.4442	.007215
16.320	172.082	•54195	72.621	5.8058	.006757
16.640	197.091	.60878	83.893	6.1896	.006298
16.960	225.912	.68464	96.465	6.5969	. 005835
17.280	258.978	.77031	110.445	7.0289	.005366
17.600	296.759	.86664	125.951	7.4868	• 004888
17.920	339.763	.97451	143.109	7.9720	.004399
18.240	388.540	1.09486	162.058	8.4860	.003898

# NF3 ISOTHERM AT 240.00 K

MOL/L	P,BAR	Z	DP/DD	DP/DT	D2P/DT2
-320	6.078	.95186	18.133	.0279	000006
.640	11.625	.91022	16.545	.0586	000027
.960	16.673	.87033	15.013	.0919	000068
1.280	21.239	.83151	13.534	.1279	000130
1.600	25.341	.79370	12.119	.1666	000217
1.920	29.003	.75700	10.783	.2077	000330
2.240	32.252	.72154	9.537	.2511	000469
2.560	35.117	.68743	8.386	.2967	000635
2.880	37.630	.65478	7.335	-3443	000827
3.200	39.822	•62363	6.382	.3937	001044
3.520	41.724	•59402	5.524	-4447	001283
3.840	43.367	•56596	4.758	.4971	001538
4.160	44.779	.53943	4.079	•5507	001802
4.480	45.987	.51441	3.482	.6054	002064
4.800	47.016	.49085	2.961	•6609	002309
5.120	47.889	•46873	2.512	.7171	002517
5.440	48.630	•44798	2.130	.7739	002665
5.760	49.259	.42857	1.813	.8313	002728
6.080	49.797	• 41 044	1.558	.8893	002680
6.400	50.263	• 39357	1.366	• 9480	002505
6.720	50.678	.37792	1.235	1.0077	002195
7.040	51.060	. 36346	1.163	1.0685	001756
7.360	51.428	.35017	1.143	1.1309	001204
7.680	51.796	.33798	1.161	1.1953	000556
8.000	52.173	.32682	1.198	1.2619	.000175
8.320	52.563	.31660	1.245	1.3311	.000982
8.640	52.972	.30725	1.314	1.4033	.001858
8.960	53.408	.29871	1.417	1.4789	.002785
9.280	53.884	.29098	1.569	1.5584	.003735
9.600	54.419	.28407	1.784	1.6425	.004675
9.920	55.035	.27802	2.082	1.7320	• 005565
10.240	55.762	.27289	2.481	1.8276	.006370
10.560	56.636	.26877	3.006	1.9301	.007062
10.880	57.702	• 26577	3.681	2.0404	.007625
11.200	59.011	• 26404	4.536	2.1594	.008053
11.520	60.627	• 26374	5.604 6.920	2.2877 2.4262	.008353 .008537
11.840	62.624	.26506 .26823	8.523	2.5756	.008620
12.160	65.087		10.457	2.7367	.008621
12.480	68.114 71.819	.27351 .28118	12.767	2.9101	• 0 0 8 5 5 3
13.120	76.330	•29155	15.502	3.0965	.008430
13.440	81.791	.30497	18.715	3.2967	.008264
13.760	88.365	.32182	22.462	3.5114	. 008062
14.080	96.230	.34250	26.802	3.7413	.007832
14.400	105.588	.36746	31.799	3.9871	.007578
14.720	116.659	.39716	37.518	4.2497	.007303
15.040	129.684	.43211	44.030	4.5297	.007010
15.360	144.930	.47285	51.411	4.8282	.006700
15.680	162.688	.51995	59.739	5.1459	.006375
16.000	183.273	.57403	69.099	5.4839	.006036
16.320	207.031	.63572	79.582	5.8430	.005682
16.640	234.336	.70573	91.283	6.2244	.005313
16.960	265.593	.78477	104.304	6.6291	.004930
17.280	301.243	.87363	118.758	7.0585	.004532
17.600	341.763	.97312	134.762	7.5137	.004118
17.920	387.670	1.08412	152.445	7.9962	.003687
2.0729					

## NF3 ISOTHERM AT 245.00 K

MOL/L	P,BAR	Z	DP/00	DP/DT	D2P/DT2
.320	6.218	• 95385	18.590	.0279	000005
.640	11.917	-91488	17.043	•0584	000025
•960	17.131	.87603	15.554	• 0916	000061
1.280	21.877	.83902	14.115	.1273	000117
1.600	26.171	.80298	12.739	•1655	000192
1.920	30.038	.76800	11.439	• 2061	000289
2.240	33.502	•73421	10.227	• 2489	000405
2.560	36.593	.70171	9.109	.2938	000540
2.880	39.342	.67059	8.086	-3405	000692
3.200 3.520	41.778 43.933	.64091 .61270	7.159	•3890	000856
3.840	45.835	•58596	6.324 5.578	•4390 •4903	001029 001204
4.160	47.512	•56067	4.917	•5429	001374
4.480	48.990	•53682	4.335	•5965	00 1529
4.800	50.294	•51437	3.827	•6511	001659
5.120	51.447	•49327	3.390	.7067	001753
5.440	52.471	.47350	3.020	.7631	001800
5.760	53.387	.45500	2.715	.8204	001790
6.080	54.215	•43774	2.474	.8787	001716
6.400	54.977	.42170	2.298	•9382	001572
6.720	55.693	• 40685	2.188	•9991	001360
7.040	56.384	•39317	2.142	1.0617	001082
7.360	57.070	.38065	2.153	1.1263	000744
7.680	57.767	• 36924	2.206	1.1931	000352
8.000	58.484	•35888	2.283	1.2626	.000088
8.320	59.229	.34947	2.376	1.3349	. 00 05 74
8.640	60.008	• 34095	2.496	1.4104	.001104
8.960	60.831	• 33329	2.658	1.4895	.001670
9.280	61.715	• 32647	2.877	1.5728	• 002263
9.600	62.680 63.754	•32052 •31549	3.170 3.555	1.6606 1.7537	<ul><li>002870</li><li>003475</li></ul>
10.240	64.968	• 31145	4.054	1.8528	. 004060
10.560	66.363	•30850	4.690	1.9584	.004610
10.880	67.986	• 30675	5.489	2.0714	.005109
11.200	69.896	• 30636	6.481	2.1926	.005546
11.520	72.158	.30749	7.698	2.3226	.005913
11.840	74.850	.31034	9.175	2.4624	.006209
12.160	78.062	.31514	10.951	2.6127	.006431
12.480	81 • 895	. 32214	13.069	2.7742	.006585
12.800	86.468	.33162	15.575	2.9478	. 006675
13.120	91.910	.34390	18.518	3.1341	.006707
13.440	98.371	• 35931	21.950	3.3339	•006686
13.760	106.016	.37823	25.927	3.5479	.006620
14.080	115.029	.40105	30.509	3.7770	.006513
14.400	125.613	• 42822	35.759	4.0218	.006371
14.720	137.993	•46020 40740	41.745	4.2833	.006197
15.040 15.360	152.416 169.151	• 49749 5/1061	48.537	4.5622	• 0 0 5 9 9 4 • 0 0 5 7 6 5
15.680	188.493	•54061 •59013	56.211 64.847	4.8593 5.1756	. 00 55 13
16.000	210.765	.64666	74.530	5.5120	.005239
16.320	236.314	.71083	85.351	5 • 86 95	.004944
16.640	265.521	.78333	97.407	6.2492	.004629
16.960	298.797	.86487	110.803	6.6522	.004295
17.280	336.590	• 95621	125.649	7.0796	.003941
17.600	379.381	1.05818	142.067	7.5329	•003568

# NF3 ISOTHERM AT 250.00 K

MOL /I	D DAD		00.400	00.40%	0.00 (0.70
MOL/L	P,BAR	Z	DP/DD	OP/OT	D2P/DT2
•320	6.357	• 95573	19.046	• 0279	000005
.640	12.209	.91774	17.540	.0583	000023
•960	17.588	.88142	16.090	-0913	000056
1.280	22.512	.84611	14.690	.1268	000105
1.600	26.997	-81174	13.351	.1646	000172
1.928	31.065	•77838	12.087	.2048	000256
2.240	34.742	.74615	10.908	.2470	000355
2.560	38.056	.71516	9.820	.2913	000468
2.880	41.036	.68549	8.824	.3373	000592
3.200	43.713	.65748	7.922	-3851	000724
3.520	46.116	.63028	7.110	. 4343	000858
3.840	48.273	.60478	6.384	.4849	000989
4.160	50.211	.58067	5.741	.5367	001112
4.480	51.955	•55793	5.176	•5897	001218
4.800	53.531	•53652	4.684	.6438	001302
5.120	54.960	.51642	4.262	•6990	001356
5.440	56.266	• 49759	3.908	.7552	001374
5.760	57.468	.47999	3.620	-8126	001350
6.080	58.589	•46360	3.398	.8713	001282
6.400	59.651	.44839	3.245	.9315	001202
6.720					001007
	60.674	.43436	3.161	. 9933	
7.040	61.681	• 42150	3.145	1.0571	000802
7.360	62.693	.40979	3.191	1.1231	000556
7.680	63.728	• 39920	3.284	1.1916	000273
8.000	64.798	. 38967	3.406	1.2629	.000045
8.320	65.910	.38111	3.548	1.3372	.000397
8.640	67.072	.37347	3.723	1.4150	.000781
8.960	68.297	.36671	3.946	1.4965	.001193
9.280	69.604	.36084	4.233	1.5823	.001628
9.600	71.016	• 35588	4.603	1.6728	.002078
9.920	72.561	.35190	5.075	1.7685	.002535
10.240	74.277	.34896	5.671	1.8701	.002988
10.560	76.207	.34718	6.415	1.9782	.003427
10.880	78.401	.34667	7.334	2.0935	.003842
11.200	80.922	.34759	8.457	2.2167	.004224
11.520	83.839	.35012	9.817	2.3486	.004563
11.840	87.234	. 35445	11.449	2.4898	.004856
12.160	91.200	.36081	13.393	2.6413	.005099
12.480	95.843	.36946	15.690	2.8037	.005290
12.800	101.284	.38068	18.388	2.9779	.005429
13.120	107.659	.39477	21.533	3.1645	.005518
13.440	115.119	.41207	25.180	3.3643	.005560
13.760	123.834	. 43296	29.384	3.5782	.005558
14.080	133.991	.45782	34.206	3.8070	.005516
14.400	145.798	.48709	39.707	4.0513	.005436
14.720	159.483	•52123	45.957	4.3120	.005321
15.040	175.298	.56073	53.027	4.5900	. 00 51 75
15.360	193.516	-60611	60.992	4.8861	.004999
15.680	214.437	.65793	69.934	5.2013	.004797
	238.387	.71678	79.938	5.5365	.004569
16.000		.78330	91.096	5.8926	.004317
16.320	265.721	• 85816	103.507	6.2708	.004043
16.640	296.822	•94206	117.275	6.6722	.003746
16.960	332.110		132.513	7.0980	.003427
17.280	372.035	1.03577	1360313	7 6 0 7 0 0	9003421

# NF3 ISOTHERM AT 260.00 K

MOL/L	P.BAR	Z	DP/DD	DP/DT	D2P/DT2
•320	6.636	_			
		• 95923	19.955	• 0278	000004
•640	12.791	. 92451	18.528	.0581	000019
.960	18.499	.89138	17.155	.0908	000047
1.280	23.775	.85920	15.828	.1258	000088
1.600	28.635	.82788	14.560	. 1631	000141
1.920	33-101	.79749	13.362	. 2025	000206
2.240	37.196	.76813	12.245	.2439	000282
2.560	40.947	·73990	11.215	-2871	000366
2.880	44.383	.71287	10.273	• 3322	000456
3.200	47.531	.68709	9.419	.3788	000548
3.520	50.420	•66260	8.652	• 4269	000639
3.840	53.077	.63939	7.969	.4764	000725
4.160	55.528	.61747	7.365	•5273	000801
4.480	57.799	•59680	6.837	•5795	000864
4.800	59.912	•57738	6.382	.6330	000910
5.120	61.891	.55917	5.998	.6878	00 09 36
5.440	63.758	.54216	5.684	.7440	000937
5.760	65.536	.52632	5.440	-8016	000914
6.080	67.247	.51164	5.267	.8609	000862
6.400	68.915	.49811	5.169	.9220	000784
6.720	70.563	. 48574	5.147	.9851	000678
7.040	72.217	.47452	5.201	1.0505	000545
7.360	73.900	.46447	5.326	1.1185	000388
7.680	75.632	• 45555	5.507	1.1892	000207
8.000	77.428	.44771	5.724	1.2631	000003
8.320	79.299	• 44089	5.972	1.3402	.000221
8.640	81.255	• 43504	6.263	1.4210	. 000467
8.960	83.313	•43013	6.614	1.5059	.000731
9.280	85.496	.42618	7.044	1.5951	.001012
9.600	87.832	.42322	7.571	1.6892	.001306
9.920	90.355	.42134	8.217	1.7886	.001608
10.240	93.106	.42060	9.006	1.8939	.001914
10.560	96.136	.42113	9.961	2.0057	.002218
10.880	99.502	.42305	11.113	2.1245	.002515
11.200	103.272	• 42654	12.490	2.2510	.002798
11.520	107.524	.43176	14.127	2.3858	.003062
11.840	112.345	. 43893	16.059	2.5298	. 003303
12.160	117.837	• 44827	18.327	2.6836	. 003517
12.480	124.114	. 46 00 4	20.972	2.8479	. 003699
12.800	131.304	.47452	24.040	3.0235	.003848
13.120	139.550	.49202	27.581	3.2112	•003963
13.440	149.012	•51288	31.647	3.4117	.004043
13.760	159.867	•53744	36.296	3.6259	.004087
14.080	172.310	• 56611	41.587	3.8545	.004098
14.400	186.557	•59929	47.583	4.0984	.004075
14.720	202.846	.63745	54.354	4.3583	.004020
15.040			61.972	4.6352	.003934
15.360	221.434 242.606	.68106 .73064	70.513	4.9299	.003820
15.680	266.670	• 73064 • 78672	80.060	5.2434	.003677
16.000	293.961		90.700	5.5766	• 003507
16.320	324.845	.84989 .92 <b>07</b> 6	102.527	5.9305	.003312
16.640	359.716	99999	115.641	6.3063	.003092
16.960	399.003	1.08828	130.148	6.7050	. 002847
10000	0 0 0 0 0 0 0	1.00050	130.140	017070	1 3 3 2 0 41

## NF3 ISOTHERM AT 270.00 K

MOL/L	P.BAR	Z	DP/00	DP/OT	D2P/DT2
-320	6.914	•96242	20.862	-0278	000004
-640	13.371	•93064	19.508	• 0579	000017
.960	19.404	.90039	18.208	.0904	000040
1.280	25.029	.87102	16.951	-1250	000074
1.600	30.259	. 84244	15.750	•1618	000118
1.920	35.116	.81470	14.615	-2006	000171
2.240	39.621	.78792	13.557	• 2413	000232
2.560	43.801	.76216	12.582	-2838	000298
2.880	47.683 51.293	.73751	11.692	•3281	000367
3.520	54.660	•71402 •69171	10.887 10.166	•3739 •4212	000437 000504
3.840	57.808	.67059	9.527	.4701	00 05 67
4.160	60.765	•65067	8.965	•5203	000621
4.480	63.554	.63193	8.480	•5719	000665
4.800	66.200	•61435	8.069	•6250	000696
5.120	68.726	•59793	7.730	•6796	000712
5.440	71.155	.58265	7.464	.7358	000711
5.760	73.511	•56850	7.272	.7937	000691
6.080	75.817	• 55547	7.157	.8534	000653
6.400	78.099	•54359	7.122	• 9152	000595
6.720	80.384	.53284	7.170	•9792	000518
7.040	82.698	•52326	7.304	1.0458	000423
7.360	85.067	•51485	7.516	1.1150	000310
7.680	87.514	•50760	7.791	1.1873	000180
8.000	90.058	.50146	8.112	1.2629	000034
8.320	92.710	•49637	8.471	1.3419	.000127
8.640	95.485	.49229	8 • 885	1.4248	.000303
8.960	98 • 404	•48922	9.370	1.5119	.000494
9.280	101.492	.48717	9.946	1.6035	.000696
9.600	104.782	-48620	10-634	1 - 7001	.000908
9.920	108.312	.48637	11.456	1.8021	.001128
10.240	112.130	. 48778	12.437	1.9100	.001353
10.560	116.292	.49055	13.603	2.0244 2.1457	.001578
10.880	120.859	.49482	14.983 16.610	2.2747	.002017
11.200	125.907 131.519	.50076 .50855	18.517	2.4119	.002223
11.520	137.792	•51841	20.741	2.5581	.002415
12.160	144.832	•53055	23.322	2.7138	.002589
12.480	152.760	• 54525	26.304	2.8798	. 002743
12.800	161.714	•56278	29.733	3.0568	.002873
13.120	171.842	•58344	33.658	3.2456	.002979
13.440	183.314	.60757	38.133	3.4469	.003058
13.760	196.312	.63552	43.215	3.6616	.003110
14.080	211.042	.66768	48.964	3.8904	.003135
14.400	227.728	.70446	55.446	4.1341	.003131
14.720	246.613	.74629	62.728	4.3937	.003100
15.040	267.967	• 79366	70.884	4.6698	.003042
15.360	292.081	.84705	79.993	4.9636	. 002956
15.680	319.273	.90702	90.137	5.2758	.002845
16.000	349.888	.97411	101.405	5.6075	.002708
16.320	384.302	1.04894	113.893	5.9597	.002546

## NF3 ISOTHERM AT 280.00 K

HOL/L	P,BAR	2	DP/DD	DP/DT	D2P/DT2
.320	7.191	•96532	21.766	.0278	000003
.640	13.949	.93622	20.484	.0578	000015
.960	20.306	.90857	19.252	.0900	000035
1.280	26.275	.88174	18.062	.1243	000064
1.600	31.871	.85563	16.924	.1607	000101
1.920	37.114	.83030	15.850	.1990	000145
2.240	42.023	.80584	14.850	.2392	000195
2.560	46.626	.78233	13.928	.2811	000249
2.880	50.946	.75985	13.089	.3247	000304
3.200	55.012	.73843	12.334	.3699	000360
3.520	58.849	.71812	11.660	.4167	000413
3.840	62.483	.69893	11.066	• 4649	000462
4-160	65.939	.68086	10.550	•5147	000504
4.480	69.243	.66390	10.111	• 5660	00 05 37
4.800	72.418	•64806	9.748	.6188	000560
5.120	75.489	•63332	9.459	•6733	000572
5 • 4 4 0	78.480	•61968	9.247	•7295	000571
5.760	81.416	.60714	9.113	.7875	000555
6.080	84.321	•59572	9.061	·8476	000526
6.400	87.224	.58541	9.096	.9099	000482
6.720	90.152	•57625	9.221	•9746	000424
7 • 0 4 0	93.135	•56826	9.439	1.0419	000351
7.360	96.202	•56145	9.743	1.1122	000266
7.680	99.379	• 55583	10.119	1.1856	000168
8.000	102.684	•55134	10.548	1.2624	000057
8.320	106.134	•54795	11.024	1.3429	.000065
8.640	109.747	•54561	11.565	1.4273	.000199
8.960	113.545	•54433	12.188	1.5160	.000344
9.280	117.558	•54414	12.915	1.6094	. 00 0498
9.600	121.823	•54509	13.766	1.7078	• 000660
9.920	126.384	•54725	14.766	1.8118	.000828
10.240	131.292	.55074	15.939	1.9217	.001000
10.560	136.607	•55567	17.315	2.0380	.001174
10.880	142.398	•56219	18.923	2.1613	.001347
11.200	148.746	•57047	20.796	2.2922	.001516
11.520	155.740	•58070	22.969	2.4313	.001679
11.840	163.482	.59310	25.480	2.5791	.001832
12.160	172.087	.60788	28.369	2.7364	.001972
12.480	181.683	.62533	31.681	2.9038	.002098
12.800	192.413	.64570	35.462	3.0820	.002207
13.120	204.435	.66931	39.764	3.2718	. 00 22 97
13.440	217.923	•69648	44.639	3.4739	. 002366
13.760	233.071 250.091	•72757	50.146 56.345	3.6890 3.9181	.002414
14.400	250.091	.76296 .80304	63.303	3.9101 4.1618	.002449
14.720	290.693	• 84827	71.087	4.4211	.002440
15.040	314.805	.89908	79.774	4.6968	.002371
15.360	341.852	.95599	89.441	4.9897	.002301
15.680	372.161	1.01951	100.174	5.3009	.002207
17.000	2150101	TOUTANT	TOOSTIA	70000	4006501

Table 12. Continued.

# NF3 ISOTHERM AT 300.00 K

MOL/L	P.BAR	Z	DP/DD	DP/DT	D2P/DT2
.320	7.746	.97042	23.567	.0277	000003
•640	15.182	.94600	22.420	.0575	000012
-960	22.099	•92288	21.319	.0894	000028
1.280	28.750	.90046	20.255	•1232	000050
1.600	35.067	.87866	19.237	.1589	000077
1.920	41.068	.85751	18.278	•1965	000109
2.240	46.772	-83711	17.387	. 2358	000145
2.560	52.204	-81753	16.572	•2769	000184
3.200	57.386 62.346	•79884 •78109	15.834	• 31 95	000223
3.520	67.108	.76432	15.177 14.601	•3638 •4097	000261
3.840	71.699	•74856	14.104	•4571	000298 000331
4.160	76.143	.73381	13.686	•5062	000351
4.480	80.467	.72008	13.348	•5569	000383
4.800	84.695	.70739	13.090	•6094	000399
5.120	88.853	.69574	12.913	•6637	000407
5.440	92.968	.68514	12.820	.7199	000407
5.760	97.067	.67560	12.814	.7781	000398
6.080	101.179	.66716	12.902	.8387	000381
6.400	105.335	.65983	13.089	.9017	000354
6.720	109.567	• 65366	13.381	•9673	000318
7.040	113.910	.64868	13.779	1.0358	000273
7.360	118.397	.64492	14.279	1.1074	000220
7.680	123.058	•64238	14.867	1.1824	000158
8.000	127.919	.64104	15.522	1.2609	000089
8.320	132.999	.64087	16.242	1.3433	000012
8.640	138.323	.64183	17.047	1.4299	.000072
8.960	143.920	•64395	17.955	1.5209	.000163
9.280	149.827	•64727	18.990	1.6167	.000259
9.600	156.089 162.757	•65184 •65777	20.174 21.534	1.7178 1.8244	•000362 •000468
10.240	169.893	.66515	23.097	1.9370	.000577
10.560	177.564	.67412	24.893	2.0561	.000577
10.880	185.852	.68483	26.954	2.1822	.000798
11.200	194.847	.69746	29.315	2.3158	.000906
11.520	204.650	.71220	32.013	2.4575	.001011
11.840	215.375	.72927	35.087	2.6078	.001110
12.160	227.150	.74890	38.581	2.7674	.001202
12.480	240.116	.77135	42.539	2.9368	.001285
12.800	254.430	.79689	47.010	3.1168	.001357
13.120	270.263	.82584	52.046	3.3081	.001416
13.440	287.806	.85850	57.703	3.5114	.001462
13.760	307.265	.89524	64.040	3.7273	.001492
14.080	328.870	.93641	71.118	3.9568	.001506
14.400	352.867	.98241	79.006	4.2005	.001503
14.720	379.528	1.03366	87.775	4.4593	.001482

Table 12. Continued.

### NF3 ISOTHERM AT 320.00 K

MOL/L	P.BAR	Z	00/90	OP/OT	D2P/DT2
.320	8.299	.97475	25.361	.0276	000002
.640	16.249	.95427	24.340	. 0573	000010
.960	23.881	.93496	23.362	.0889	000022
1.280	31.204	.91626	22.415	-1223	000040
1.600	38.231	.89808	21.511	.1576	000062
1.920	44.977	.88046	20.662	.1946	000087
2.240	51.462	.86348	19.878	.2333	000114
2.560	57.707	.84723	19.166	.2736	000143
2.880	63.736	.83178	18.530	.3156	000173
3.200	69.575	.81717	17.973	•3592	000202
3.520	75.248	.80346	17.497	. 4045	080230
3.840	80.781	.79067	17.102	.4513	000255
4.160	86.202	.77882	16.790	-4999	000277
4.480	91.536	.76794	16.561	•5502	000294
4.800	96.810	.75804	16.417	.6024	000307
5.120	102.052	.74914	16.361	• 6565	000314
5.440	107.291	.74127	16.398	.7127	000316
5.760	112.557	.73445	16.533	.7711	000311
6.080	117.883	.72872	16.772	.8319	000301
6.400	123.303	.72411	17.122	.8953	000284
6.720	128.853	.72068	17.591	.9615	000261
7.040	134.574	.71846	18.182	1.0308	000232
7.360	140.502	•71750	18.888	1.1032	000197
7.680	146.673	.71780	19.697	1.1792	000157
8.000	153.117	•71936	20.589	1.2589	000111
8.320	159.859	.72215	21.563	1.3426	000060
8.640	166.929	•72616	22.640	1.4305	000004
8.960	174.362	.73141	23.842	1.5230	.000057
9.280	182.204	.73794	25.192	1.6204	.000121
9.600	190.504	.74584	26.715	1.7231	.000189
9.920	199.323	.75520	28.440	1.8315	.000260
10.240	208.730	.76612	30.395	1.9459	.000333
10.560	218.803	•77876	32.611	2.0668	.000406
10.880	229.633	.79327	35.124	2.1947	.000479
11.200	241.318	.80982	37.970	2.3301	.000551
11.520	253.973	.82861	41.187	2.4735	.000620
11.840	267.722	.84986	44.816	2.6254	.000685
12.160	282.704	.87380	48.903	2.7865	.000745
12.480	299.074	.90069	53.495	2.9573	.000798
12.800	317.000	.93081	58.641	3.1385	.000844
13.120	336.669	. 96446	64.395	3.3307	.000880
13.440	358 - 284	1.00194	70.815	3.5346	.000905
13.760	382.068	1.04360	77.961	3.7510	.000919

Table 12. Continued.

# NF3 ISOTHERM AT 350.00 K

MOL/L	P,BAR	Z	00/00	DP/DT	D2P/DT2
.320	9.127	.98013	28.041	.0276	000002
.640	17.964	• 96452	27.198	.0570	000008
-960	26.537	.94991	26.391	.0883	000017
1.280	34.857	•93578	25.612	.1213	000030
1.600	42.933	.92207	24.870	.1560	000046
1.920	50.779	.90882	24.178	.1923	000065
2.240	58.413	.89611	23.549	.2303	000085
2.560	65.858	-88402	22.989	•2699	000106
2.880	73.135	.87262	22.505	.3112	000127
3.200	80-270	.86198	22.102	.3540	000148
3.520	87.289	.85214	21.781	•3986	000168
3.840	94.219	.84314	21.546	.4448	000187
4.160	101.087	.83503	21.399	.4928	000203
4.480	107.924	.82782	21.344	.5427	000216
4.800	114.758	.82155	21.383	•5945	000227
5.120	121.620	.81626	21.523	.6484	000234
5.440	128.543	.81198	21.768	.7045	000238
5.760	135.563	.80875	22.126	.7630	000237
6.080	142.717	.80662	22.606	.8240	000233
6.400	150.045	.80563	23.217	.8878	000225
6.720	157.591	.80586	23.966	. 9545	000213
7.040	165.399	.80734	24.857	1.0244	000198
7.360	173.514	.81013	25.887	1.0976	000179
7.680	181.979	.81425	27.040	1.1745	000157
8.000	190.831	.81970	28.299	1.2552	000131
8.320	200.102	.82646	29.665	1.3401	000103
8.640	209.830	.83455	31.162	1.4293	000071
8.960	220.062	. 84398	32.813	1.5232	000037
9.280	230.850	.85483	34.644	1.6221	000001
9.600	242.257	.86716	36.683	1.7263	.000038
9.920	254.353	.88109	38.960	1.8363	.000077
10.240	267.219	.89673	41.505	1.9523	.000118
10.560	280.948	.91424	44.354	2.0749	.000158
10.880	295.642	•93376	47.543	2.2045	.000198
11.200	311.416	• 95547	51.110	2.3415	.000237
11.520	328.398	• 97959	55.098	2.4864	.000274
11.840	346.728	1.00631	59.550	2.6398	.000307
12.160	366.564	1.03589	64.514	2.8021	.000337
12.480	388.077	1.06856	70.038	2.9741	.000361

Table 12. Continued.

NF3 ISOTHERM AT 400.00	T 400.00	_ <b>6</b> 00_0:	ΔΤ	HERM	TSOT	NF3
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MOL/L	P,BAR	Z	DP/DD	DP/DT	D2P/DT2
.320	10.504	.98696	32.484	.0275	000001
.640	20.806	.97749	31.913	. 0567	000006
.960	30.931	.96879	31.372	.0875	000012
1.280	40.886	.96044	30.851	-1200	000021
1.600	50.679	• 95239	30.363	.1540	000032
1.920	60.323	.94469	29.922	-1896	000045
2.240	69.836	.93742	29.542	•2268	000058
2.560	79.238	.93067	29.233	• 2656	000072
2.880	88.554	.92452	29.003	•3059	000087
3.200	97.809	.91984	28.859	.3479	000101
3.520	107.033	.91428	28.805	.3917	000115
3.840	116.255	.91030	28.848	•4371	00 01 28
4.160	125.507	.90715	28.991	• 4845	000139
4.480	134.821	. 90486	29.242	•5337	000150
4.800	144.234	•90350	29.606	•5851	000159
5.120	153.782	.90311	30.091	•6386	000166
5 - 440	163.506	•90373	30.705	•6945	000171
5.760	173.448	• 90542	31.459	• 7529	000174
6.080	183.656	90825	32.364	-8140	000176
6.400	194.178	•91227	33.429	.8779	000176
6.720	205.069	•91756	34.667	•9450	000173
7 - 0 4 0	216.384	• 92418	36.081	1.0153	000169
7.360	228.179	.93218	37.669	1.0891	000164
7.680	240.509	.94161	39.416	1.1667	000157
8.000	253.420	•95248	41.304	1.2482	000148
8.320	266.959	.96477	43.341	1.3339	000138
8.640	281.177	• 97852	45.553	1.4241	000127
8.960	296.135	.99377	47.968	1.5191	000115
9.280	311.901	1.01059	50.613	1.6192	000102
9.600	328.555	1.02906	53.521	1.7246	000089
9.920	346.186	1.04931	56.723	1.8358	000075
10.240	364.893	1.07144	60.255	1.9531	000062
10.560	384.789	1.09563	64.156	2.0770	000049

Table 12. Continued.

## NF3 ISOTHERM AT 450.00 K

MOL/L	P.BAR	Z	DP/DD	DP/DT	D2P/DT2
.320	11.877	•99198	36.904	.0274	000001
.640	23.634	.98699	36.586	.0564	000004
.960	35.294	.98260	36.290	.0870	000009
1.280	46.861	.97849	36.011	.1191	000016
1.600	58.344	.97460	35.763	-1526	000024
1.920	69.754	.97101	35.563	.1877	000033
2.240	81.111	.96779	35.426	.2243	000043
2.560	92.435	.96504	35.364	. 2625	000054
2.880	103.753	• 962 85	35.387	-3022	000065
3.200	115.093	.96128	35.505	• 3436	000075
3.520	126.486	•96040	35.723	.3867	000086
3.840	137.967	•95028	36.051	.4316	000096
4.160	149.572	• 96096	36.496	.4784	000106
4.488	161.338	• 96 25 2	37.064	•5272	000115
4.800	173.307	• 96500	37.766	.5781	000123
5.120	185.523	• 96846	38.611	.6313	000130
5.440	198.034	• 97296	39.610	•6869	000136
5.760	210.891	•97856	40.774	.7451	000141
6.080	224.149	• 98534	42.118	.8060	000146
6.400	237.867	• 99336	43.655	• 8699	000149
6.720	252.110	1.00270	45.395	• 9369	000151
7.040	266.943	1.01344	47.346	1.0072	000153
7.360	282.434	1.02563	49.505	1.0812	000154
7.680	298.647	1.03932	51.858	1.1589	000154
8.000	315.642	1.05452	54.388	1.2406	000154
8.320	333.475	1.07125	57.106	1.3266	000153
8.640	352.213	1.08954	60.043	1.4171	000152
8.960	371.929	1.10944	63.228	1.5124	000150
9.280	392.708	1.13103	66.693	1.6127	000149

# NF3 ISOTHERM AT 500.00 K

MOL/L	P.BAR	Z	DP/DD	DP/DT	D2P/DT2
.320	13.247	•99579	41.308	.0274	000001
•640	26-451	.99418	41.225	.0563	000003
.960	39.633	•99307	41.160	.0866	000007
1.280	52.796	.99216	41.111	.1183	000013
1.600	65.948	.99145	41.094	.1516	000019
1.920	79.101	.99101	41.127	. 1862	000026
2.240	92.276	.99091	41.228	•2224	000034
2.560	105.496	• 991 26	41.410	.2601	000042
2.880	118.788	.99215	41.685	-2993	000051
3.200	132.186	• 99364	42.065	.3402	000060
3.520	145.722	.99581	42.559	.3829	000068
3.840	159.437	•99874	43.177	•4273	000077
4.160	173.370	1.00247	43.927	• 4737	000085
4.480	187.565	1.00709	44.820	•5221	000093
4.800	202.071	1.01264	45.866	•5726	000101
5.120	216.937	1.01920	47.079	•6254	000108
5.440	232.220	1.02682	48.470	•6807	000114
5.760	247.978	1.03558	50.053	.7386	000120
6.080	264.276	1.04556	51.845	•7993	000126
6.400	281.183	1.05682	53.859	.8629	000131
6.720	298.772	1.06946	56.110	•9297	000136
7.040	317.119	1.08354	58.604	•9999	000141
7.360	336.304	1.09913	61.339	1.0737	000145
7.680	356.401	1.11628	64.303	1.1513	000149
8.000	377.480	1.13501	67.478	1.2329	000153
8.320	399.611	1.15534	70.881	1.3188	000158

## NF3 ISOTHERM AT 600.00 K

MOL/L	P,BAR	Z	DP/DD	DP/DT	D2P/DT2
.320	15.982	1.00111	50.077	• 0273	000001
.640	32.062	1.00421	50.431	•0560	000002
.960	48.259	1.00767	50.799	.0860	000005
1.280	64.575	1.01128	51.184	•1173	000008
1.600	81.021	1.01505	51.607	.1500	000013
1.920	97.610	1.01907	52.089	.1841	000018
2.240	114.366	1.02344	52.652	•2196	000023
2.560	131.318	1.02824	53.313	• 2566	000029
2.880	148.499	1.03358	54.089	.2951	000035
3.200	165.948	1.03953	54.992	• 3353	000041
3.520	183.709	1.04617	56.038	• 3772	000047
3.840	201.829	1.05357	57.238	.4209	000054
4.160	220.359	1.06182	58.605	• 4665	000061
4.480	239.355	1.07097	60.154	•5142	000067
4.800	258.879	1.08110	61.899	•5640	000074
5.120	278.993	1.09229	63.855	.6161	000081
5.440	299.770	1.10459	66.040	.6708	000087
5.760	321.285	1.11810	68.470	<b>-7280</b>	000094
6.080	343.619	1.13289	71.164	.7880	000101
6.400	366.860	1.14904	74.142	.8510	000108
6.720	391.102	1.16663	77.418	• 9172	000115

Table 13. The Joule-Thomson Inversion Locus. (Column DI is the initial density for the iteration.)

## THE JOULE-THOMSON INVERSION LOCUS FOR NITROGEN TRIFLUORIDE.

TV	OT	401 41	0.040	- 11	0.7	1101 41	D D 4 D
T,K	01	MOL/L	P BAR	T,K	DI	MOL/L	P.BAR
190	19.228	18.171	15.48	450	11.065	11.059	532 • 62
200	18.823	17.836	65.09	460	10.832	10.812	531.93
210	18.428	17.510	110.99	470	10.604	10.565	530 <b>3</b> 6
220	18.040	17.193	153.47	480	10.381	10.319	527.97
230	17.661	16.884	192.76	490	10.163	10.075	524.85
240	17.289	16.582	229.09	500	9.949	9.832	521.09
250	16.926	16.286	262.67	510	9.740	9.592	516.76
260	16.570	15.997	293.65	520	9.535	9.355	511.95
270	16.221	15.712	322.19	530	9.335	9.122	506.76
280	15.880	15.433	348.44	540	9.138	8.892	501.28
290	15.546	15.158	372.52	550	8.946	8.668	495.59
300	15.219	14.886	394.53	<b>560</b>	8.758	8 • 4 4 8	489.78
310	14.899	14.619	414.60	570	8.574	8.235	483.93
320	14.586	14.354	432.80	580	8.394	8.028	478-11
330	14.279	14.092	449.22	590	8.217	7.828	472.39
340	13.979	13.832	463.95	600	8.044	7.636	466.89
350	13.685	13.575	477.05	610	7.875	7.451	461.56
360	13.397	13.319	488.61	620	7.709	7.272	456.29
370	13.115	13.064	498.67	630	7.547	7.097	451.01
380	12.840	12.811	507.30	640	7.389	6.926	445.66
390	12.570	12.559	514.57	6 <b>50</b>	7.233	6.758	440.17
400	12.305	12.307	520.52	660	7.081	6.592	434.51
410	12.046	12.057	525.22	670	6.932	6.428	428.66
420	11.793	11.807	528.72	680	6.786	6.266	422.59
430	11.545	11.557	531.08	69 <b>0</b>	6-644	6.104	416-30
440	11.302	11.308	532.36	700	6.504	5.944	409.78

TABLE 14. Thermophysical Properties of Saturated Liquid

This table was computed along paths described in section 3.0. Column headings have the following interpretations--

```
dP_{\sigma}/dT, vapor pressure,
DPS/DT
                 dρg/dT, saturated liquid,
DDL/DT
                 (aP/aT), single phase,
DP/DT
           Ξ
                 (∂P/∂ρ), single phase,
DP/DD
           Ξ
                ΔH<sub>vap</sub>, heat of vaporization,
Q,VAP
                C_{V}(\rho,T),
CV
           Ξ
           Ξ
                 C_{\sigma}(T),
CS
                 C_{p}(\rho,T),
           Ξ
CP
W
           Ξ
                 speed of sound.
```

BAR-L/MOL • 8329E+03 • 7237E+03 • 5684E+03 • 5180E+03 • 5717E+03 • 5290E+03 • 4531E+03 • 4531E+03 • 2789E+03 • 1916E+03 • 1916E+03 • 1930E+03 • 1930E+03 • 1930E+03 • 2127E+03 • 1930E+03 • 1930E+03 • 1789E+03 • 1789E	342E+0
00 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	81
DDLL/DT DDL	8931
0PS/0T 0AS/0T 0AS/0T 1141E - 04 1220E - 03 3163E - 03 1510E - 03 1510E - 03 1510E - 03 1510E - 03 1510E - 03 1510E - 01 1513E - 01 1513E - 01 1513E - 01 1513E - 01 1513E - 01 1513E - 01 1515E + 00 1525E	1205E+0 1245E+0
V,6AS L/MOL 1561E+06 1334E+06 1334E+06 1334E+06 1334E+06 1334E+06 1334E+06 14362E+03 2297E+03 2297E+03 2297E+01 21476+02 21476+02 21476+02 21476+01 21746E+01 21756E+01 25910E+01	707E+0 263E+0
C C C C C C C C C C C C C C C C C C C	947
2 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	2121
26.320 26.320 26.320 26.320 27.56.420 22.57.565 22.75.565 22.75.665 22.75.665 22.75.665 22.75.665 22.75.665 22.75.665 22.75.710 22.75.75 22.75 22.75 22.75 22.75 22.75 22.75 22.75 22.75 22.75 22.75 22.75 22.75 2	7.92
BAR 1854E-05 17286E-05 1546E-05 1546E-03 1561E-02 2013E-01 2350E-01 2350E-01 2350E-01 2350E-01 2350E-01 2350E-01 2350E-01 2730E-01	4338E+0
75.000 1150.000	33.00

	33	S	31	28	25	21	17	14	1109	0.7	70	0 0	~	4	0	$\sim$	4	0	8	4	╼	8	4	-	00	5	7	8	5		$\infty$	4	-	~	S	~	S	M	0
	CP	0	3.07	2.8	1.7	1.0	0.5	0.1	70.03	0.0	0.0	0.2	0.5	0.8	1.2	1.7	2.2	2.9	3.4	404	5.3	6.4	7.6	8.9	0.5	2.3	4 . 4	6.9	6.6	3.7	8.6	05.4	15.8	33.5	71.3	05.6	2.9	62.3	0
		0	3.7	2.8	1.7	1.0	0.5	0.1		0.0	0.0	0.2	0.5	0.8	1.2	1.6	2.2	2.8	3.3	4.2	5.0	5.9	7 . 0	8.1	9.5	0.9	2.6	4.5	6.7	9.3	2.6	6.9	03.1	12.9	31.8	87.2	7.1	95.1	0 • 0
0E.	CV	0	0.0	8.5	6.7	5.3	4.1	3.1	42.37	1.7	1.2	0.8	0.5	0.3	0.1	0.0	0.0	0.0	0.0	0.1	0.3	0.5	0.7	1.0	1.3	1.6	1.9	2.5	2.5	2 ° 8	3.1	3.3	3.5	0 ° 4	5.0	8.4	2.2	5.5	0
TRIFLUORI	S	MOL	2.50	6.42	01.41	06.02	10.31	14.33	118.126	21.71	25.13	28.39	31,52	34.53	37.43	40.23	45.95	45.58	47.69	50.65	53.10	55.50	57.85	60.17	62.45	64.71	96 • 99	69.18	71.40	73.63	75.88	78.16	80.51	85.98	85.69	89.08	91.05	92.53	97.03
NITROGEN	r	JVMOL	•	67.	29.	86.	340.	692.	2043.2	392.	742.	093.	445.	798.	154.	512.	873.	237.	538.	926	352.	732.	119.	511.	911.	320.	737。	166.	6.07	0062.	0535.	030.	1553.	2117	2754.	3565.	4041.	4395.	5460.
LIQUID	w	JOWL	•	67.	29.	86.	340.	692.	2043.1	392.	742.	093.	• † † †	798.	153.	511.	871.	234.	533.	969	342.	719.	101.	488.	882.	281.	689	106.	532.	9970°	0422	892.	1385.	1911.	2499°	3237.	3666.	3984.	4897.
SATURATED	. VA	JUMOL	4548.	4405.	4207	4016.	3829.	3645.	63.	3282.	3101.	2919.	2735.	2549.	2359.	2163.	1962.	1754.	1577.	1311.	1074.	0824.	0560	0280.	982.	999	322.	953°	552	114.	630.	089	471.	742.	834.	532.	707	077.	•
PERTIES OF	۵	80	854E-0	286E-0	154E-0	546E-3	299E-0	561E-0	. 4050E-02	448E-0	0.13E - 0	969E-0	323E-0	275E+0	113E+0	3350E+0	111E+0	538E+0	1013E+0	1504E+0	2048E+0	2730E+6	3570E+0	4591E+0	5813E+0	261E+0	8956E+0	1092E+0	319E+0	578E+0	1871E+0	2203E+0	577E+0	995E+0	464E+0	3991E+0	219E+0	338E+0	461E+0
PRO	<b>j</b> -	¥	6.35	0000	2.00	0.00	5.00	0000	95.000	00.00	2.00	10.00	15.00	20.00	25.00	30.00	35.00	40.00	60 • 44	20.00	52 · 00	60.00	65.00	70.00	75.00	80.00	85.00	90.00	95.00	00.00	02.00	10.00	15.00	20.00	25.00	30.00	32.00	33.00	34.00

TABLE 15. Thermophysical Properties Along Isobars\*

The following pages give physical and thermodynamic properties along selected isobars, as computed by methods of section 3 of the text.

The first line of each table refers to freezing liquid on an artifical P(T) melting line adopted from methane.

Each table at  $P < P_C$  contains a blank line for the transition from saturated liquid to vapor, as seen by the abrupt decrease of density.

Table headings for partial derivatives have the following interpretations--

 $DP/DT \equiv \partial P/\partial T$ ,  $DP/DD \equiv \partial P/\partial \rho$ .

The specific heat interpretations are--

 $CV \equiv C_V(\rho,T),$  $CP \equiv C_p(\rho,T).$ 

These tables are extrapolated beyond the range of some of the P-p-T data used for adjusting the equation of state. Small discontinuities may be detected at T = 234.0 K along isobars at  $P > P_C = 44.61$  bar, due to change in the paths of computation, section 3.

184

187 191 203

194 197 200 212

215

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224

221

229 232 235 240 245 245 248 253 255

BAR

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ISOBAR AT

NITROGEN TRIFLUORIDE

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237

M/SEC 1315

BAR

.10000

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1287

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955

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J/MO 269. 269. 988. 2394. 3799. 4513.	16827.6 17024.2 17787.4 18781.9 198586.0 199425.2 20765.4 21234.2 21713.9 22704.4 22705.4 22705.4 22705.4 22705.4 22705.4 22705.4 22705.4 22705.6 26491.3 27654.0 28848.6	11324. 13246. 132611. 23248. 33901. 4560. 5892.
J/MO 267. 986. 1692. 3192. 4510. 4851.	15732.1 15883.3 16475.3 16475.6 17704.7 177434.6 177434.6 118489.5 19644.1 20468.3 227468.3 227468.3 227468.3 227468.3 227468.3 227468.3 227468.3 227468.3	66750 6770 78387 8387 8945 99509 1079 1235 1820
DP/D L/MO 13.06 4.05 11.93 11.93 12.05 13.05 15.	10.715 11.186 12.941 13.807 14.968 17.230 17.230 18.079 18.079 19.771 19.771 22.301 27.339 27.339 27.339 27.339 27.339 27.339 27.339 27.339 27.339 27.339	1 2 4 4 4 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1
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J/MOL 9.3 273.9 993.1 1699.1 2399.1 3199.4 3814.3 4517.2 5271.6	7415. 80465. 8048. 8465. 90324. 10685. 11643. 3685.	24217.4 24761.4 25314.7 25876.9 26447.7 27027.0 27027.0 27014.3 2812.3 30663.3 31293.7 31293.4 31293.7
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BAR/K E	5.522	626	7.991	3.256	9.209	5.703	2.631	9.916	7.498	5,327	3.365	1.578	.937	.412	974°	1740	• 175	.982	509	413	312	263	231	2 08	190	176	164	154	146	138	131	126	120	4 1 1 2	01115 1075	101	100	160	760	091	088	086	084	0.82	080	9
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	0379	2	0390	0399	0408	0418	1429	0440	0453	0467	0482	6640	0519	0543	0572	2190	1000	7270	2706	3088	3748	4241	4665	5048	2404	5745	6065	6377	6680	6975	7264	1248	9797	0770	85443	8045	9174	9435	9698	9953	.0209	• 0464	.0717	0970	. 1221	41.74
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	46.69	.36	93.64	10.91	59.87	78.15	75 90	70.00	00.00	7 7 ° C C	27.72	98.94	2.73	8.85	7.07	6.83	<b>76</b> •	55	.93	.16	0.65	2.76	4.65	6.37	7.97	9.47	06.0	2.27	5 o 5 d		060.02	8 . 47	9.61	0.74	1.84	2 . 93	4 • 00	5 ° 0 5	6.10	7.13	8.14	9.15	U . 15	1.14
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	7.15	80.000	00.06	0000	10.00	00000				70.07	80.00	90.00	00.00	10.00	20.00	30.00	32.68	32,68	40.00	50.00	60.00	70.00	80.00	90.00	00.00	10.00	00.02	30.00			370.000	80.00	00.06	00.00	10.00	20.00	58.00	40°00	50.00	50.00	0000			

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<u> </u>	93.07	6.07	05.64	13.93	21.28	27.93	34.03	39.69	66.44	50.01	54.80	59.40	63.87	68.25	72.62	77.05	81.75	87.69	96°20	12,57	15.92	18.76	21.32	23.69	25,93	28.06	30.11	32.09	34.01	35.88	37.69	39.47	41.21	42.91	44.57	46.21	47.81	49.39	50.93	52.46	53.95	55.43	6.88	58.30	59.71
Σ	270	. M	130	834.	532.	229.	929.	637.	354.	082	823.	582.	364.	175.	0027.	0936.	1946.	3285.	8030.	9163.	0015	0768.	1472.	2148.	2808.	3459.	4104.	4747.	5390.	6034.	.6299	7328.	7979.	8633.	9291.	9953°	0619.	1288.	1962.	2639.	3321.	4006	94.	5387.	6083.
Σ	2 4	42.	956.6	656.	350.	042.	738.	441.	152.	874.	608.	360.	133.	934.	773.	0666.	1652.	2941.	.7469	7817。	8478.	9068	9626.	0168.	0701.	1230.	1759.	2289.	2822.	3359.	3899°	• 4444	*4664	5548.	6107.	6671.	7240.	7814.	8392.	8975.	9563.	0155.	51.	1352.	1956.
	847.20	09.68	• 22	94.46	11.70	40.65	78.90	24.66	76.59	33.66	95.06	60.18	28.55	9.80	3.64	9.84	8.17	8.29	4.16	7.62	0.21	2.39	4.33	60.9	7.72	9.25	0.70	2.09	3.43	4.71	96 • 9	7.18	8.36	9.52	0.66	1.77	2.87	3.95	5.01	6.06	7.10	8.12	9.13	0.14	1.13
DP/DT	5 2 5 4 5	3.751	111	3.373	9.324	5.817	2.746	0.033	7.617	5.450	3.494	1.715	3.084	.575	.161	.807	.452	.890	.543	402	335	292	262	239	220	202	192	181	171	163	156	149	143	137	132	128	123	119	116	112	109	106	1 03	100	960
7	3033	2928	.26165	2377	2189	2038	1915	1815	1734	1667	1614	1572	1543	1527	1526	1546	1606	1797	5428	6473	7110	7571	7927	8213	8448	9646	8814	8958	9083	9195	9288	9372	2446	9514	9573	9627	9675	9718	9757	9792	9824	9854	9880	7066	9927
	0750	0382	0	0398	0408	0417	0428	0440	0452	9940	0481	0498	0517	0240	0568	0605	0658	0770	2428	3016	3446	3810	4137	4439	4724	9664	5257	5510	9 2 2 9	9669	6232	9463	6691	6916	7137	7357	1524	7789	8 0 02	8213	8454	8632	8840	9006	9251
	6.37	6.17	M	5.07	4.50	3.92	3.33	2.72	2.10	1.45	0.77	0.06	9.30	8.48	7.57	6.51	5.17	2.97	•11	• 31	06.	.62	. 41	.25	.11	• 00	• 90	.81	• 73	• 66	• 60	• 54	• 49	* 4 4	• 40	。 35	• 32	• 28	• 25	.21	• 18	•15	• 13	.10	• 08
<b>⊢</b> ≯	7.18	0000	80.000	0.00	00.00	10.00	20.00	30.00	40 · 0 0	50.00	60.00	70.00	80.00	00.06	00.00	10.00	20.00	30.00	40.00	50.00	00.09	70.00	80.00	00.06	00.00	10.00	20.00	30°00	40.00	50.00	00.09	70.00	80.00	90.00	00.00	10.00	20.00	30 000	40°00	50.00	60.00	70.00	0000	00.06	00.00

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2		5260	0120 02120	7000	2256	01007	7777	1007	1207	1864	1792	1735	1690	1658	1640	1637	1657	1715	1883	1657	6080	6831	7354	7752	8368	8326	8545	8725	8881	9017	9135	9238	9329	9410	. 94817	7777	2000	4000	7976	24 - 70	10000	9815	9846	1000	7000
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DEN	MULY	\$ 5 V	07 • 0	200	7. CO	70°4	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	0000	0 1 0 0	2.11	1.46	0.79	0.08	9.33	8.52	7.62	6.58	5.29	3.32	5.16	.79	•25	.90	•66	949	• 31	• 18	• 06	.97	88	• 8 0	• 73	.67	. 51	O 4	40.0	• •	) « ! !! • •	9 7 6	0 0	0.01	77.	42°	0	٦ ( ا ا
<b>⊢</b> :	i	47.0	•							40.00	20.00	60°06	70.00	80.00	00.06	00.00	10.00	20.00	30.00	00.04	50.00	60.00	70.00	80.00	00.06	00.00	10.00	20.00	30.00	40.00	50.00	60.00	70.00	80.00	390.000	•		30.00					0000	80,00	

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0	73.3	2.6	0.8	6.6	9.6	9.8	0.3	1.0	1.9	3.2	4.7	<b>6.7</b>	9.1	2.2	6.3	95.5	04.1	9.04	53.4	1.2	93.7		4.3	0.7	8.5	7.2	4.9	5.9	5.7	5.7	5 . 8	5.9	6.1	4.9	2.9	7.0	7.3	7.7	8.0	3.4	8.7	9.1	9.4	9 ° 8	0.1
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MOL	93.16	6.01	05.58	13.86	21.21	27 . 85	33.95	39.60	06 • 77	06.64	54.68	59.27	63.72	68.08	72.40	76.75	81.28	86.52	98.64	08.74	13.00	216.263	19.07	21.60	23.96	26.19	28.31	33 . 34	32,31	34.22	36.07	37.87	39.64	41.36	43.04	02044	46.32	47.91	49.47	51.00	52,51	53°99	55.45	56.89	58.30
Σ	41.	37.	154.	858.	555.	251.	951.	658.	374.	100.	840.	<b>.</b> 969	374.	9181.	0023.	0916.	1890.	3072	5938	8397.	9482	20346.4	1118.	1841.	2537.	3215.	3883.	4545.	5204.	5861.	6519.	7178.	7838	8501.	9167.	9836.	0508.	1184.	1863.	2546.	3232	3921.	4614.	5311.	6010.
Σ	44.	38.	51.	650.	343.	034°	729.	430°	139.	858。	.065	338.	106.	900	9729.	0604.	1553.	2691.	5276.	7239.	8080.	18754.0	9362.	9937。	0496	1045.	1589.	2133.	2677。	3222.	3771.	4323.	4879.	5439.	6003.	6572.	7145.	7723。	8305°	8891.	9482	00770	0676.	1279.	1885.
	849.58	3.85	96.16	98.23	15,35	44.21	82.41	28.15	80.09	37.18	98.64	63.85	32.33	03.74	7.79	4.28	3.08	4.19	1.18	5.16	8.24	.73	2.89	4.82	9.60	8.25	9.81	1.29	2.71	4.07	5.39	99•9	7.90	9.11	0.30	1.45	2.59	3.71	4.81	5.89	96°9	$\theta \cdot 01$	9006	÷0 • 0	1.1
DP/DI BAR/K	5.564	859	8.213	3.473	9.423	5.915	2.844	0.132	7.718	5.555	3.603	1.830	0.208	•711	.315	066.	.693	• 325	.231	.591	455	383	336	301	275	524	236	221	209	198	188	179	172	165	158	153	147	145	138	133	129	126	22	119	116
7	3528	3412	3048	2770	2550	2374	2231	2114	2018	1940	1878	1829	1794	1773	1769	1787	1843	1993	3317	5573	6488	.70937	1543	7896	8182	8420	8620	8791	8939	1906	9180	9278	9366	9443	9513	9575	9630	9681	9726	9767	9804	9838	9868	9886	9922
VOL	0379	0381	0330	0398	0407	0417	0428	0439	0451	9465	0480	1640	0516	0538	0 565	0600	0648	0732	1273	2227	2697	2	3377	3661	3925	4173	4410	4639	4859	5074	5284	5489	2690	5889	6084	6277	2949	9699	6842	7027	7211	7 393	1574	7753	7932
DEN	6.32	.18	5.64	5.08	4.52	3.94	3.35	2.75	2.12	1.43	0.81	0.11	9.36	8.56	7.67	99*9	2.45	3.64	.85	.48	.70	9	96•	• 73	• 54	•39	• 26	•15	0.05	.97	.89	• 82	• 75	• 69	• 64	• 59	• 54	。 ກາ	940	• 45	• 3	• 35	• 32	• 29	• 26
<b>⊢</b> ⊻	7.32	0.00	0.00	90°06	00.00	10.00	20.00	30.00	40.00	50 · 00	00.09	70.00	80.00	00.06	00.00	10.00	20.00	30.00	40°00	50.00	60°00	270.000	80°00	90.00	00.00	10.00	20.00	30.00	40.00	50.00	60°00	70.00	80.00	90.00	00.00	10.00	20.00	30.00	40.00	50.00	60°00	70.00	80.00	90.00	00.00

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DP/DD	66776 66776 7676 7676 7676 7676 7676 7	19.603 21.189 22.705 24.162 25.568 26.929 30.792 31.792 33.221 34.400 35.559 36.699 40.020 41.098
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4725 4725 3724 3724 3724 3724 3724 2710 2710 2710 2710 2710 2710 2710	22352 2352 22408 22418 22772 22772 3593 46898 46898 47543 7543	.83979 .85002 .87747 .89266 .91769 .92807 .95730 .955956 .955956 .955956 .955956 .955956
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3	9.7	48.51	5.2	3.1	1.7	0 ° 7	0.2	6°6	9.8	9.9	0.2	0.6	1.1	1.6	1.9	1.8	1.4	2.1	6.2	7.0	8.0	8 . 7	8.9	9.2	9.5	6.6	47 ° 0	0.9	1.5	2.1	2.7	3 • 3	3.9	6.5	5.1	5.7	6 ° 2	6 ° 8	7.3	7 . 8	00	80	9.3	9.7	0 • 1
Ö	7,0E/	95.643	05.18	3.44	23.76	27 0 37	33.43	38°02	44.30	49.25	53°95	58.45	62.79	67.01	71.11	75.14	79.12	83.13	87.20	91.85	96.96	02.07	06.53	10.34	13.66	16.60	19.28	21.75	24.06	26.26	28.35	30,36	32 ° 30	34.17	35°99	37.76	39.49	41.17	42.81	24044	46 . 00	45.54	90.64	50,55	52.01
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2	2 4	13.	20°	613.	299.	983。	669°	359°	057.	762.	477.	204.	946	7.05.	485.	0286.	1108.	1970.	2873.	3932.	5104.	6277.	7305.	8198.	8992。	9719.	00000	1052.	1685.	2304.	2916。	3522。	4125.	4727.	5328.	5930	6533。	7138.	24420	8355。	8965.	9581°	98°	0818。	14410
0	865,00	97	21.71	22.63	38 • 92	67.20	05.03	50.58	02.48	59.69	21,39	86.99	56.01	28.09	02.99	80.53	0.63	3.33	8.83	7.75	1.29	99.6	0.19	1.30	2.86	4.60	6.37	6.10	9.78	1.41	2.99	4.51	5°89	7.43	8 . 83	0.20	1.53	2.84	4.11	5,36	6.59	7.80	8 . 99	0.16	1.32
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	F 23	+	5.70	5.16	4.61	4.05	3.47	2.89	2.29	1.67	1.04	0.38	69.6	8.97	8.20	7.37	9409	5.43	4.21	2.72	0.92	•12	• 74	•73	. 98	.43	666	49°	35	.10	.89	.71	° 55	040	•27	• 15	<b>50°</b>	° 95	0 0 0	.77	• 69	• 62	ຸ້ນ	20 (	o 42
<b>⊢</b> 2	8.20	70.000	0.00	00.06	00.00	10.00	20.00	30.00	40°00	50.00	00.09	20.00	80.00	90.00	00.00	10.00	20.00	30.00	40°00	20.00	60.00	70.00	80.00	00.06	00.00	10.00	20.00	30.00	40 ° 0 C	50.00	60.00	70.00	8 0 ° 0 0	90.00	000	10.00	20.00	30 ° 00	40.00	50.00	00000	70.00	0000	00.00	

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	36 1.45	2 17.31	17904	9206	07.99	9.8	98.0	$\leftarrow$
	43 1.25	6 17.97	18704.	0461.	11.12	0.4	3.0	$\forall$
	53 1.09	1 18.82	19461	1370.	14.01	1.0	9.0	44
LO	58 .97	7 19.86	20185.	22440	16.70	1.5	5.7	+1
ന	48 .87	0 21.08	20882	3088.	19.22	2.1	3.1	$ \overline{} $
C	29 .80	7 22.41	21559.	3908	21.59	2.7	0.9	S
	24 •73	1 23.79	22220	4708.	23.85	3.3	9.2	$\sim$
	6.6	9 25.20	22870.	5493°	26.00	3.9	7 . 8	$\sim$
	67 .63	9 26.62	23512.	6266.	28.06	404	6 ° 8	2
	72 .59	3 28.03	24148.	7030.	30.05	5 ° 0	0.9	3
Ö	00 .56	8 29.42	24781.	7787.	31.96	9.6	5.4	M
4	71 .53	5 30.80	25410.	8539°	33.82	6.1	6.4	4
M	05 .50	7 32.16	26039	9286.	35 . 62	6.7	9.4	4
J.	18 .48	7 33.50	26666	0031.	37.37	7.2	4.3	3
	23 .45	2 34.82	27294	0774.	39.08	7 . 7	4.2	. rv
	34 .43	7 36.12	27922	1515	40.75	8	4.4	کیا ،
	59 .42	0 37.40	28552	2256.	42.37	2 e 8	0 0 7	1 15
	0 % 6 0	8 38.66	29182	2997.	43.97	9.1	7	ی ۱
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8	914 .37	73 41.128	3044807	34478.5	247.057	60.06	74.12	267
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303 BAR

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S	1426	3 6	25	19	13	0.8	02	~	2	8	3	S 1	2	$\sim$	σ ı	Ω.	44	ထ	S	3	0	8	9	3	3	44	0	$\sigma$	8	100	~ P	- V	) (	0	9	2	5	S	5	S	5	rU.
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0	47.20	3 C	1.6	0.7	0.1	9.8	9 • 6	9.7	6.6	J • 2	9 • 0	တ္ တ	1.1	ο . Ο .	0.1	ታ • D	4.1	4.3	5.0	5° 8	6.8	7 • 7	8 • 6	9°5	J . C	1.2	2.1	2.9	3 ° 6	7 ° 1	0 U	. M	6.0	7.5	8.0	8.6	9.1	9.6	0.0	0.5	0.9	104
MOL	96.98	11.03	8.22	24.69	31.60	36 • 04	41.10	42.84	50.31	54.54	28.57	62.41	66.08	14.60	72.89	/ p • N 4	78.98	82.05	85 • 03	87.92	90.74	93.48	96.16	98.78	01.32	03.80	06.22	08.57	10.85	13.67	17 22	19,36	21 . 34	23.28	25.16	26.99	28.78	30.53	32.23	33.90	35.54	37.13
3/ M	1830.4	976	658	336.	014.	695.	379.	066.	758.	456.	15%	9870	U586.	1505	2014.	6777	3416.	4169.	4927.	2694	<b>.69</b> 49	7252.	8042	8839°	9641.	0448.	1256.	2066.	2867	3687	44700	0 00	6911	7713.	8512.	9310.	0106.	0901.	1694.	2487	3279.	40700
Σ .	315. 2	4130	65.	711.	356.	001.	648.	297.	949.	604.	262.	926	5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	656	9913	U 7 6 7 0	1195	1881.	25 70 •	3263.	3960°	4661.	5366.	6073.	6781.	7489.	8197.	8903	9508	0.510.	4707	401	3094	3784.	4472.	5159.	5845	6530.	7214.	7898。	8582.	9266.
	• 03	73.72	83.79	07.32	41.57	84.49	34.53	90.50	51.48	16.75	47.60	57.98	55.10	10.02	90.00	7000	5/.12	43.00	30.51	19.53	09.93	01.63	4.50	8 • 45	3.38	9.21	5.83	3.15	1.00	2°57	74.00	7.23	7.03	7.04	7.22	7.52	7.93	8.42	8.98	9.60	0.25	0°94
DP/DT BAR/K	453	7.871	3.704	0.118	7 . 6 00	4.267	1.855	9.716	7.809	6 • 1 0 5	11604	3.203	1.966	24 0 ° 0	9.64	. 434	.120	.381	.714	.114	.573	.087	• 650	•258	606°	• 596	.316	1900	0040	0.04/	4 4 0	170	.043	.929	.825	.732	2490	.570	6640	.435	.375	.320
	2.47836	.0882	.9162	.7770	• 6625	.5671	• 4867	.4186	.3603	.3104	67970	• 2306	.1989	•1/13	.1489	•1290	.1136	.1006	• 09 05	• 0828	• 0775	0743	.0730	.0734	00752	.0782	.0821	• 0868	0.000	4040	1000	1144	.1198	.1250	.1298	.1344	.1387	.1427	.1463	• 1497	.1528	.1557
NOL L/MOL	037	039	39	0 40	0 41	0 42	043	770	042	970	740	0 <b>†</b> 0	ا ا ا	10 C I	υυν 1 ν ν		u かち i	057	058	0 9 0	062	9 0	990	0 6 9 0	071	0 7 3	0.76 0.76	5/0	100	1 M M	- 0 - 0	260	0 95	980	100	103	106	109	111	114	117	120
Σ	S &	5.59	5.10	4.61	4 - 11	3.61	3.11	2.60	2.10	1.59	1 • U8	0.57	0000	7000	V = U S	0.51	8 . U	7.48	96 99	6.45	5.94	5.44	76.4	4.45	3 ° 98	3.52	3.07	2.64	2007	1004	1.12	0 . 79	740	0.18	9.90	• 63	• 38	• 15	• 92	•71	•51	• 32
	73.534		00.00	10.00	20.00	30.00	40.00	20.00	60.00	70.00	000000000000000000000000000000000000000	90.00		0000	20.00	00000	00000	50.00	50.00	70.00	80.00	90.00	00.00	10.00	20.00	30 ° 00	40.00	50.00				0.00	10.00	20.00	30.00	40.00	50.00	00.09	70.00	80.00	90.00	00.00

NITROGEN TRIFLUORIDE

45 C

AT

ISOBAR

500 BAR

Table 16. List of Coefficients for the BWR Equation.

G(1)	=	.1751151116E-31
G(2)	=	5338642406E+00
G(3)	*	.3924633078E+01
G(4)	=	5141353757E+03
G(5)		3243348520E+05
G(6)	=	5912181013E-03
G(7)	=	.9096990477E+00
G (8)	=	4785568295E+03
G( 9)	=	4180501052E+07
G(10)	=	9695778991E-05
G(11)	*	.5361200088E-01
G(12)	=	1443265236E+02
G(13)	=	3322161796E-02
G(14)	=	.2764741771E+00
G(15)	=	.8324982578E+01
G(16)	=	1307102346E-01
G(17)	=	.1851077593E-03
G(18)	=	.2920941516E+00
G(19)	=	6918309272E-02
G(20)	=	.4308730236E+07
G(21)	=	1096864087E+08
G(22)	=	.2380327276E+05
G(23)	=	.3137563559E+07
G(24)	=	.6086206849E+02
G(25)	=	.4205136659E+02
G(26)	=	•1076337320E+00
G(27)	=	3297262333E+02
G(28)	=	.8485003350E-04
G(29)	#	•1224321948E-02
G(30)	=	.1269404637E-06
G(31)	=	8824183840E-06
G(32)	=	.3309207594E-04

Table 17. Comparison of Results From the Two Equations of State.

PRESS	TEMP		- DIFFEREN	NCE IN		
		DENSITY	Н	S	CV	CP
BAR	К	PCT	J/MOL	J/MOL-	K PCT	PCT
1.0 1.0 1.0 1.0 1.0 1.0	70.0 120.0 170.0 220.0 240.0 280.0 320.0 350.0	.011 .010 150 201 186 139 102 387	6 6.6 -15.7 -3.û -1.2 5 3	.111 .125 060 .008 .015 .019 .018	-5.26 3.69 1.35 .30 .20 .07	-2.03 .06 1.17 .26 .13 .02 02
10.0 10.0 10.0 10.0 10.0 10.0	70.0 120.0 170.0 220.0 240.0 280.0 320.0	.306 .317 .057 127 220 223 204 177	5 6.5 -49.1 -17.8 .9 17.2 20.4 19.5	.113 .124 241 109 028 .036 .045 143	-4.04 3.39 -1.62 2.45 1.51 .52 .11 05	-2.04 .06 -1.77 2.39 1.37 .36 .00
40.0 40.0 40.0 40.0 40.0 40.0 40.0	70.0 120.0 170.0 220.0 240.0 280.0 320.0 350.0	.002 .036 .055 057 597 .173 .333	1 6.3 -48.2 -37.4 10.2 27.1 25.7 18.3	.118 .122 235 205 .007 .072 .067	07 2.47 -2.05 4.49 3.79 1.25 01 43	-2.10 .36 -1.79 1.98 .27 .24 28
50.0 50.0 50.0 50.0 50.0 50.0 50.0	70.0 120.0 170.0 220.0 240.0 280.0 320.0 350.0	.003 .043 .054 058 156 029 .333 .386	.1 6.2 -48.0 -38.0 -15.5 41.0 31.0	.121 .122 234 208 127 .124 .390 .057	1.19 2.20 -2.16 4.03 1.76 1.38 14	-2.14 .05 -1.80 2.30 4.34 13 53 63
100.0 100.0 100.0 100.0 100.0 100.0	70.0 120.0 170.0 225.0 240.0 280.0 320.0	.017 .057 .058 095 069 .097 509	1.5 5.7 -47.4 -42.1 34.4 34.3 76.1 48.0	.141 .119 228 227 .109 .085 .231	7.11 1.03 -2.26 3.44 -2.18 1.50 77 -1.45	-2.41 .04 -1.85 3.16 -1.68 4.56 87
200.0 200.0 200.0 200.3 200.3 200.3	120.0 170.0 220.0 243.0 283.0 320.0	.064 .086 031 179 011 .230	5.3 -46.8 -52.2 35.2 21.1 3.8 23.6	.117 223 276 .137 .354 337	57 -1.40 5.45 -1.11 37 -1.35 -1.95	.04 -1.95 3.37 11 -1.14 .59
300.0 300.0 300.0 300.0 300.0 300.0	120.0 170.0 220.0 240.0 280.0 320.0 350.0	.135 .137 .053 353 .144 .196	5.0 -45.8 -58.4 26.3 34.6 6.3 -17.1	.117 215 313 .068 .131 .036	-1.41 .34 8.76 2.02 2.16 .23 80	.09 -2.01 3.28 05 31 -1.08 73

```
PROGRAM NE3THRM (INPUT, OUTPUT)
    NITROGEN TRIFLUORIDE THERMOPHYSICAL PROPERTIES.
    NEW XEF, DENGASF, EDELF, FOR LOW DENSITIES.
     COMMON GK, GKK, B1, B2, B3, B4, B5, C1, C2, C3, E1, E2, E3, ER, IX
     COMMON/1/AL, BE, GA, DE, EP, DCRT, TCRT, PCRT, DGAT, DTRP, TTRP, PTRP
      COMMON/2/ NFP, EPP, PJ(6)
      COMMON/3/DPDT, D2PDT2, DPSDT, DPMDT, DPDD, DPDR, DTSDR, DTHDR
      COMMON/4/XB1, XB2, XC1, XC2, XE1, XE2, DXBDR, DXCDR, DXEDR
      COMMCN/5/ DDSDT
      COMMON/6/ TSAT, THETA, PSAT
      COMMON/7/ NFG, GE, AV(6)
      COMMON/8/ IN, IK, P,T, DEN, E, H, S, CV, CP, CSAT, W, WK
      COMMON/9/ DNG, EG, HG, SG, CVG, CPG, WG, DPGDT, DPGDD
      COMMON/10/ NFL, EL, AW(6)
      COMMON/12/ DELS, DELCV
      COMMON/13/ ZCRT, ZSAT, DZSDT, ZFX, FRT, DFRTDT
      COMMON/19/ KD
      COMMON/99/ TI, EZZ, EZ, SZ, CVZ, HZ, CPZ
      DIMENSION PP(99)
   1 FORMAT(I5. 2F10.0)
   2 FORMAT(I5, 3F10.0)
   3 FORMAT (8 I 10)
   5 FORMAT(1X)
   9 FORMAT (8F10.0)
  14 FORMAT(1H1 18X *NITROGEN TRIFLUORIDE ISOBAR AT *F8.5, 4H BAR / )
  15 FORMAT(1H1 18X *NITROGEN TRIFLUORIDE ISOBAR AT * I3, 4H BAR / )
  16 FORMAT(19X 1HT 6X3HDEN 6X3HVOL 8X1HZ 5X5HDP/DT 5X5HDP/DD
     2 8X1HE 8X1HH 8X1HS 6X2HCV 6X2HCP 5X1HW /
     3 15X 5HDEG K 4X5HMOL/L 4X5HL/MOL 14X5HBAR/K 1X9HBAR-L/MOL
     4 4X5HJ/MOL 4X5HJ/MOL 2X7HJ/MOL/K 1X7HJ/MOL/K
     5 1X7HJ/MOL/K 1X5HM/SEC )
  17 FORMAT (10XF10.3, F9.3, F9.5, F9.5, F10.4, F10.3, 2F9.1, F9.3, 2F8.2, I6)
  18 FORMAT(10XF10.3, F9.5, F9.3, F9.5, F10.6, F10.3, 2F9.1, F9.3, 2F8.2, I6)
  20 CALL PVTDATA
      CALL IDELFIT $ CALL QVAPFIT
  21 CALL JTLOCUS
  22 CALL TABLIQ
  29 GO TO 90
     TEST SUBROUTINE THERMO.
  30 P = 40 $ PRINT 14, P $ PRINT 16
   31 CALL THERMOM $ V = 1/DEN $ IW = W $ Z = P/DEN/GKK/T
   32 PRINT 17, T, DEN, V, Z, DPDT, DPDD, E, H, S, CV, CP, IW
   33 CALL THERMOL $ V = 1/DEN $ IW = W $ Z = P/DEN/GKK/T
   34 PRINT 18, T, DEN, V, Z, DPDT, DPDD, E, H, S, CV, CP, IW
  35 CALL THERMOV $ V = 1/DEN $ IW = W $ Z = P/DEN/GKK/T
  36 PRINT 18, T,DEN, V, Z, DPDT, DPDD, E, H, S, CV, CP, IW
  40 P = 50 $ PRINT 14. P $ PRINT 16
  41 T = 230 $ CALL THERMO $ V = 1/DEN $ IW = W $ Z=P/DEN/GKK/T
  42 PRINT 18, T, DEN, V, Z, DPDT, DPDD, E, H, S, CV, CP, IW
  43 T = 234 $ CALL THERMO $ V = 1/DEN $ IW = W
  46 Z = P/DEN/GKK/T
  47 PRINT 18, T, DEN, V, Z, DPDT, DPDD, E, H, S, CV, CP, IW
  48 T = 24J $ CALL THERMO $ V = 1/DEN $ IW = W $ Z=P/DEN/GKK/T
  49 PRINT 18, T, DEN, V, Z, DPDT, DPDD, E, H, S, CV, CP, IW
C
     COMPUTE THERMOFUNCTIONS ON ISOBARS. START ON THE MELTING LINE.
     ISOBARS AT P UNDER PORT TRAVERSE THE DOME.
C
```

NOTE USE OF QVAP , DATA, TO CROSS THE , DOME, .

```
NOTE USE OF CSAT , DATA, FOR SPECIFIC HEATS IN COMPRESSED LIQUID.
   90 IN = 1 $ NI = 48 $ READ 9, (PP(I), I=1, NI)
  91 DO 300 I=IN.NI $ IP = P = PP(I) $ IK = I $ LS = 0
   92 IF(P-IP) 93,94
   93 PRINT 14, P
                  $
                      GO TO 95
   94 PRINT 15, IP
   95 PRINT 16
  96 IF(I.EQ. 24) P = PCRT
  100 T = FINDTMF(P) $ CALL COMPRLQ $ V=1/DEN $ IW=W
  101 Z = P/DEN/GKK/T
  102 PRINT 17, T, DEN, V, Z, DPDT, DPDD, E, H, S, CV, CP, IW
  103 IT = T/10 $ IF(P.LT.PCRT) 110,180
C
    CASES FOR P LESS THAN PORT.
  110 TS = FINOTSF(P) \% K = L = 0
  111 DO 150 J=1,99 $ T = JT = 10^{+}(IT+J)
  112 IF (T.LT.TS) 115,117
  115 CALL COMPRLQ $ V=1/DEN $ IW=W $ Z = P/DEN/GKK/T
  116 PRINT 17, T,DEN, V, Z, DPDT, DPDD, E, H, S, CV, CP, IW $ GO TO 150
  117 LS = LS + 1 $ IF(LS.EQ.1) 120,130
     CASE FOR SATURATED LIQUID AND VAPOR.
  120 T = TS & CALL CO EXIST
  123 V=1/DEN $ VG=1/DNG $ IW=W $ IWG=WG
      Z = P/DEN/GKK/T $ ZG = P/DNG/GKK/T
  124 PRINT 17, T,DEN,V,Z, DPDT,DPDD,E,H,S,CV,CP,IW $ PRINT 5
  125 IF(P.LT.30) 126,127
  126 PRINT 18, T, DNG, VG, ZG, DPGDT, DPGDD, EG, HG, SG, CVG, CPG, IWG $ GOTO 128
  127 PRINT 17, T, DNG, VG, ZG, DPGDT, DPGDD, EG, HG, SG, CVG, CPG, IWG
  128 T = JT
    CASES FOR THE HOMOGENEOUS DOMAIN.
  130 IF(JT.GT.500) 131,132
  131 K = K+1 \$ T = JT = JT + 10*K \$ IF(JT.GT.500) 300,132
C 132 CALL GENEOUS $ V=1/DEN $ IW=W $ Z = P/DEN/GKK/T
  132 CALL GENIUS $ V=1/DEN $ IW=W $ Z = P/DEN/GKK/T
  133 IF (P.LT. 30) 134,135
  134 PRINT 18, T, DEN, V, Z, DPDT, DPDD, E, H, S, CV, CP, IW $ GO TO 150
  135 PRINT 17, T, DEN, V, Z, DPDT, DPDD, E, H, S, CV, CP, IW
  150 CONTINUE
C
     FOR P.GE.PCRT, CASES T.LE.TCRT, AND T.GT.TCRT.
  180 K=L=0 $ DO 250 J=1,99 $ T = JT = 10*(IT+J)
  181 IF(T.LE.TCRT) 192,210
     CASE FOR T.LE.TCRT.
  192 CALL COMPFLQ $ V=1/DEN $ IW=W $ Z = P/DEN/GKK/T
  193 PRINT 17, T, DEN, V, Z, DPDT, DPDD, E, H, S, CV, CP, IW $ GO TO 250
     CASE FOR T ABOVE TORT, HOMOGENEOUS DOMAIN.
  210 IF(JT.GT.500) 211,220
  C 220 CALL GENEOUS $ V=1/DEN $ IW=W $ Z = P/DEN/GKK/T
  220 CALL GENIUS $ V=1/DEN $ IW=W $ Z = P/DEN/GKK/T
  221 PRINT 17, T, DEN, V, Z, DPDT, DPDD, E, H, S, CV, CP, IW
  250 CONTINUE
  300 CONTINUE
  999 STOP $
                 END
```

```
SUBROUTINE COEXIST
C
     GIVEN T AT COEXISTENCE, GET BOTH VAPOR AND LIQUID FUNCTIONS.
C
     FOR VAPOR, GET DNG, EG, HG, SG, CVG, CPG, WG, DPGDT, DPGDD,
C
     FOR LIQUID, GET DEN, E, H, S, CV, CP, CSAT, W. DPDT, DPDD.
C
     COEXIST CALLED BY COMPRLQ. P NOT USED, MUST NOT CHANGE.
     COMMON/1/AL, BE, GA, DE, EP, DCRT, TCRT, PCRT, DGAT, DTRP, TTRP, PTRP
     COMMON/3/DPDT, D2POT2, DPSDT, DPMDT, DPDD, DPDR, DTSDR, DTHDR
     COMMON/5/ DDSDT
     COMMON/8/ IN, IK, P,T, DEN, E, H, S, CV, CP, CSAT, W, WK
     COMMON/9/ONG, EG, HG, SG, CVG, CPG, WG, DPGDT, DPGDD
     COMMON/12/ DELS, DELCV
     COMMON/99/ TI, EZZ, EZ, SZ, CVZ, HZ, CPZ
     DATA (Q=1.01325), (G=0.083145)
    1 FORMAT(1H0 9X *T EXCEEDS TCRT IN COEXIST. * / )
    2 IF(T.GT.TCRT) 3,4
    3 PRINT 1 $
                   STOP
    4 PS = PSATF(T) $ DNG = DB = DENGASF(T)
    5 TI = T $ CALL IDEAL $ N = 11 $ LD = 1
                                                 $ DA = 0
    6 EG = EZZ + EZ + EDELF(0,N,T,DA,DB,LD) $ HG = EG + 100*PS/DB
    7 SG = SZ + DELS - 100*G*ALOG(G*T*DB/Q)
    8 IF(T.EQ.TCRT) 9,11
    9 PX = PVTF(T.DB.1) % DPGDT = DPDT % DPGDD = DPDD
   10 CPG = CVG = WG = 0 $ GO TO 14
   11 CVG = CVZ + DELCV $ PX = PVTF(T,DB,1)
   13 DPGDT = DPDT $ DPGDD = DPDD
     NOW TRAVERSE THE , DOME, USING QVAP , DATA, .
   14 DEN = DL = DENLIGF(T) $ DDLDT = DDSDT $ QV = QVAPXF(T)
  15 QVT = -QV/T $ H = HG-QV $ S = SG+QVT $ E = H - 100 + PS/DL
  17 IF(T.EQ.TCRT) 18,19
  18 PX = PVTF(T,DL,1) $ CP=CV=CSAT=W=0 $
                                              RETURN
  19 CSAT = CSATXF(T) $ PX = PVTF(T,DL,1)
  29 IF(T.GT.200) 21,22
  21 CV = CVSATF(T) $ GO TO 23
   22 CV = CSAT + 100*T*DPDT*DDLDT/DL/DL
   23 CP = CV + 100 + T/DPDD + (DPDT/DL) + 2
   30 W = SQRT(WK*CP*DPDD/CV)
                                   RETURN
                                          $ END
```

```
FUNCTION CSATXF(T)
     NF3 SATLIQ ENTROPY AND CSAT, J/MOL/K, RDG/NBS, NOV. 13, 1979.
C
C
     SSAT = SCRT + A*U**ES + B*LN(X) + C*U + D*U**2 + E*U**3,
     WHERE X E T/TCRT, U E (1-X).
C
C
     CSAT = -ES*A*X/U**(1-ES) + B - C*X - 2*D*X*U - 3*E*X*U**2.
      DIMENSION AS(7)
      DATA (NFS=7), (ES=0.33), (TCRT=234.0), (SCRT=197.03182)
      DATA(AS = -27.04141165, 168.4875348, 117.5913487,
     1 -16.46287979, 241.1959696, -288.5828349, 230.9162107)
    1 FORMAT(1H0 9X 3HT =F10.5, * IN CSATXF(T). * / )
    2 IF(TCRT-T) 3,4,5
    3 PRINT 1, 1
                  $
                       STOP
    4 CSATXF = 0
                  3
                       RETURN
    5 X = T/TCRT  $ U = 1.0 - X  $ UE = U**(ES-1)
    6 CS = -AS(1) *ES*UE + AS(2)/X $
                                         DO 7 K=3,NFS
    7 \text{ CS} = \text{CS} - (K-2) + AS(K) + U + + (K-3)
    9 CSATXF = X*CS
                    $
                          RETURN $ END
```

```
SUBROUTINE COMPRLQ
C
    GIVEN P,T FOR COMPRLIQ. AT T.LE.TC, GET DEN AND FUNCTIONS.
C
    REVISED TO USE HSATF, SSATF, CSATXF, BUT NOT COEXIST. TIMESAVER.
C
    INTEGRATE ALONG ISOTHERM T FROM SATLIQ UP TO POINT (P.T).
     COMMON/1/AL, BE, GA, DE, EP, DCRT, TCRT, PCRT, DGAT, DTRP, TTRP, PTRP
     COMMON/3/DPDT,D2PDT2,DPSDT,DPMDT,DPDD,DPDR,DTSDR,DTHDR
     COMMON/5/ DOSDT
     COMMON/8/ IN, IK, P,T, DEN, E,H,S, CV,CP,CSAT, W,WK
     COMMON/12/ DELS, DELCV
   1 FORMAT (1H0 9X *COMPRLQ T.GT.TCRT. * / )
   2 IF (T.GT. TCRT) 3.4
   3 PRINT 1
              $
                   STOP
    GET PSAT, DENLIQ, AND SATLIQ FUNCTIONS FOR START.
C
   4 PS = PSATF(T) $ DL = DENLIQF(T) $ DDLDT = DDSDT
                   $ ES = HS - 100*PS/DL $ SS = SSATF(T)
   6 \text{ HS} = \text{HSATF}(T)
C
   7 IF (T.GT. 200) 8,9
   8 CVS = CVSATF(T) $ GO TO 10
C
   9 PX=PVTF(T,OL,0) $ CVS = CSATXF(T) + 100*T*DPDT*DDLDT/DL/DL
    INTEGRATE UP TO POINT (P.T).
                                 DX = DB - DL
  10 DEN = DB = FINDENF(T,P)
                             $
  11 N = 10 $ LD = 2 $ E = ES + EDELF(1,N,T,DL,DB,LD)
  12 H = E + 100*P/DB $ S = SS + DELS $ CV = CVS + DELCV
  13 PX = PVTF(T,DB,1) \$ IF(T.EQ.TCRT) 14,15
  14 CP = CV = W = 0 $
                          RETURN
  30 RETURN $
                 END
```

```
FUNCTION DENGASE(T)
    DESIGNED FOR ZSAT = 1 AT LOW DENSITIES, 5/29/77.
C
    USE ZSAT E PS/DS/GK/TS WITH VAPOR PRESSURES, AND ZCRT.
C
    Z = 1 + (ZCRT-1)*PI*F(X)/X/X
    F(X) = 1 + A1^{+}VE + A2^{+}V + A3^{+}V^{+}2
     COMMON/1/AL, BE, GA, DE, EP, DCRT, TCRT, PCRT, DGAT, DTRP, TTRP, PTRP
     COMMON/3/DPDT,D2PDT2,DPSDT,DPMDT,DPDD,DPDR,DTSDR,DTHDR
     COMMON/5/ DDSDT
     COMMON/7/ NFG, GE, AV(6)
     COMMON/13/ ZCRT, ZSAT, DZSDT, ZFX, FRT, DFRTDT
     DATA (GKK = 0.083145)
    1 FORMAT (1HG 9X *T EXCEEDS TO IN DENGASF. * / )
   2 IF(TCRT-T) 3,4,6
    3 PRINT 1 $ STOP
   RETURN
   5 ZSAT = ZCRT $ ZFX = 1
                              $
   6 IF(T.LE. a) 7.9
   7 DENGASF = DDSDT = 0 $ ZSAT = 1 $ DZSDT = 0
   8 \text{ ZFX} = 1 + AV(1) + AV(2) + AV(3)
                                      *
                                         RETURN
   9 ZN = ZCRT - 1 $ PC = PCRT $ TC = TCRT
  18 X = T/TC 8 X2 = X*X 8 V = 1.0 - X
  11 P = PSATF(T)
                  $ PI = P/PC $ PIT = DPSDT/PC
  12 VE = V**GE $ VE1 = -GE*VE/V
  13 ZFX = F = 1 + AV(1) + VE + AV(2) + AV(3) + V + V
  14 F1 = AV(1) *VE1 - AV(2) - 2*AV(3) *V
  15 ZSAT = Z = 1 + ZN*PI*F/X2
  16 DZSDT = DZDT = \{PI^{+}(F1-2^{+}F/X)/TC + F^{+}PIT\}^{+}ZN/X2
  17 DDSDT = (DPSDT - P/T - P*DZDT/Z)/T/Z/GKK
                          $
  18 DENGASF = P/T/Z/GKK
                              RETURN
                                      8
                                          FND
```

```
FUNCTION EDELF(L, M, T, DA, DB, LD)
    GET CHANGE OF E, S, CV WITH DENSITY ALONG ISOTHERMS.
    GET EDELF, DELS, DELCV FROM DA TO DB ON ISOTHERM T.
    ROMBERG NUMERICAL INTEGRATION VIA
    CARNAHAN/LUTHER/WILKES, APPLIED NUMERICAL METHODS, P. 90,
    JOHN WILEY AND SONS, INC., N.Y., 1969.
    SPECIAL REVISION FOR VERY LOW DENSITIES.
    NOTE NK GIVES FINAL, TOTAL SUBDIVISIONS OF INTERVAL DX.
     COMMON/1/AL, BE, GA, DE, EP, DCRT, TCRT, PCRT, DGAT, DTRP, TTRP, PTRP
     COMMON/3/DPDT,D2PDT2,DPSDT, DPMDT, DPDD,DPDR,DTSDR,DTHDR
     COMMON/12/ DELS, DELCV
     COMMON/13/ ZCRT, ZSAT, DZSDT, ZFX, FRT, DFRTDT
     DIMENSION E(20), S(20), C(20)
     DATA (DI = 0.0001), (G = 0.083145)
   1 FORMAT(1H09X*EDELF L =*12,5H, N =13,5H, T = F8.3,6H, DA =E10.4,
    1 6H, DB =E10.4, 6H, LD =I2//
    2 10X 1HN 7X5HEDELF 8X4HDELS 7X5HDELCV )
   2 FORMAT (1HO 9X 6HEDIF =F10.3, 8H, SDIF =F10.5, 9H, CVDIF =F10.3)
   3 FORMAT(6X I5, F12.3, F12.5, F12.3)
    FOR DA=0 AND DB.LE.DI, IDEAL GAS, EDELF=DELS=DELCV=0.
    FOR DA=0 AND DB.GT.DI, START ROMBERG WITH DA = DI,
    TO AVOID INFINITIES IN ORDINATE FUNCTIONS AT DA = 0.
   9 \text{ NMAX} = M \$ \text{ NK} = 0
                          $ ZK = 1.0-1/ZCRT $ RK = 100*G*TCRT/DCRT
  10 IF(L.EQ. 0) 11.14
  11 IF(DB.LE.DI) 12,13
  12 EDELF = DELS = DELCV = 0
                                     RETURN
  13 DA = DI
    GET FIRST TRAPEZOID AREA, E(1) ETC., FROM DA TO DB.
  14 DX = DB - DA $ P = PVTF(T,DA,0) $ IF(DA.LT.DCRT) 16,17
  16 EA = RK*(ZK*ZSAT*ZFX + FRT - T*DFRTDT) $ GO TO 18
  17 EA = 100 + (P-T+DPDT)/DA/DA
  18 IF(L.EQ. 0) 19,20
  19 SA = 100*(G-DPDT/DA)/DA $ GO TO 21
  20 SA = -100 * DPDT/DA/DA
   21 CA = -100 + T + D2PDT2/DA/DA
  22 P = PVTF(T,DB,0) $ IF(DB.LT.DCRT) 23,24
  23 EB = RK*(ZK*ZSAT*ZFX + FRT - T*DFRTDT) $ GO TO 25
  24 EB = 100*(P-T*DPDT)/DB/DB
  25 IF(L.EQ. 0) 26,27
  26 SB = 100*(G-DPDT/DB)/DB $ GO TO 28
  27 SB = -100 * OPDT/DB/DB
  28 CB = -100 + T + D2PDT2/DB/DB
   29 E(1) = (EA + EB) *DX/2 $ S(1) = (SA + SB) *DX/2 $ C(1) = (CA+CB) *DX/2
    INTERVAL HALVING, GET E(N+1), ETC.
   31 JM = 2**N - 1 $ DXN = DX/2**N $ E(K) = S(K) = C(K) = 0
   33 DO 45 J=1,JM,2 $ NK = NK+1 $ DN = DA + J*DXN
   34 P = PVTF(T,DN,0) $ IF(DN.LT.DCRT) 35,36
   35 EB = RK*(ZK*ZSAT*ZFX + FRT - T*DFRTDT) $ GO TO 37
  36 EB = 100 + (P-T+DPDT)/DN/DN
   37 IF(L.EQ. 0) 38,39
  38 SB = 100 + (G-DPDT/DN)/DN $ GO TO 40
   39 SB = -100*DPDT/DN/DN
   40 \text{ CB} = -100 \text{+} \text{T} \text{+} \text{D2PDT2/DN/ON}
   41 E(K) = E(K) + EB    S(K) = S(K) + SB    C(K) = C(K) + CB
   45 CONTINUE
                $
                   E(K) = E(N)/2 + E(K)*DXN
   46 S(K) = S(N)/2 + S(K) + DXN  C(K) = C(N)/2 + C(K) + DXN
C
```

```
TEST FOR CONVERGENCE.
50 ED=ABS(E(K)-E(N)) $ SD=ABS(S(K)-S(N)) $ CD=ABS(C(K)-C(N))
53 IF(ED.LT.0.5/LD) 54,60
54 IF(SD.LT.0.002/LD) 55.60
55 IF (T.EQ. TCRT. AND. DB. GE. DCRT) GO TO 57
56 IF(CD.LT.0.05/LD) 57.60
57 EDELF = E(K) $ DELS = S(K) $ DELCV = C(K) $ RETURN
60 CONTINUE $
              61 PRINT 1, L, N, T, DA, DB, LD
62 PRINT 3, NM, E(NM), S(NM), C(NM) $ PRINT 3, N, E(N), S(N), C(N)
64 PRINT 3, NP, E(NP), S(NP), C(NP) $ PRINT 2, ED, SD, CD
99 STOP
         3
             END
   FUNCTION FINDENF (T,P)
   ON ISOTHERM T, FIND DEN, MOL/L, TO MINIMIZE (P-PC) VIA EQNSTATE.
   COMMON/1/AL,BE,GA,DE,EP, DCRT,TCRT,PCRT, DGAT,DTRP,TTRP,PTRP
   COMMON/3/DPDT.D2PDT2.DPSDT.DPMDT.DPDD.DPDR.DTSDR.DTHDR
   OATA (DM=27.0), (GKK=0.083145)
41 FORMAT(1H0 9X *FINDENF = 0, FAILS TO CONVERGE. * / )
42 FORMAT(1H0 9X *FINDENF = DCRT, DP/DR ZERO OR NEG. * / )
43 FORMAT(1HG 9X *FINDENF = 0, DOUBLE-VALUED AT P = PSAT. * /)
   IF(T.GT. 0.AND.P.GT. 0) 1,35
 1 IF(T-TCRT) 2,5,8
 2 DG=DENGASF(T) $ DL=DENLIQF(T) $ PS=PSATF(T) $ IF(P-PS) 3,32,4
 3 D = DG/2  $ GO TO 11
 4 D = (DL + DTRP)/2  $ GO TO 11
 5 DG=DL=DCRT $ PS=PCRT $ IF(P-PS) 6.33.7
              $ GO TO 11
 6 D = DCRT/2
 7 D = 2*DCRT
               $ GO TO 11
  8 IF(T.LT.300) 9,10
 9 PC = PVTF(T,DCRT,0) $ IF(P-PC) 6,33,7
10 D = DCRT
11 DO 30 J=1.50 $ DP=P-PVTF(T,D,1) $ IF(ABS(DP/P)-1.0E-7) 31,31,12
12 IF (DPDD. GT. 0) 13,34
13 DD = DP/DPDD \$ IF(ABS(DD/D)-1.0E-7) 31,31,14
14 D = 0 + 00
                   IF(D.GT.O.0) 16,15
               $
15 D = P/GKK/T
                $
                     GO TO 30
16 IF (D.GT. DM) 17.18
17 D = DM $ GO TO 30
18 IF(T-TCRT) 19,24,30
19 IF (P.LT.PS) 20,22
20 IF(D.GT.DG) 21.30
 21 D = DG $ GO TO 30
 22 IF(D.LT.DL) 23,30
23 D = DL $ GO TO 30
 24 IF(P.LT. PCRT) 25,27
 25 IF (D.LT.DCRT) 30,26
 26 D = DCRT - 0.02 $ GO TO 30
27 IF (D.GT. DCRT) 30,28
 28 D = DCRT + 0.02
 30 CONTINUE $ PRINT 41
                            STOP
 31 FINDENF = D
                $
                     RETURN
 32 PRINT 43 $ STOP
 33 FINDENF = DCRT $ RETURN
 34 FINDENF = DCRT $ PRINT 42 $ RETURN
 35 FINDENF=DPDT=D2PDT2=û $ DPDD=GKK*T $ OPDR=DPDD*DTRP
 36 RETURN
                END
           35
```

```
FUNCTION DENLIQF(T)
 DEN = DCRT + YNL*(X + (XE-X)*Y), YNL E DTRP - DCRT.
 Y = A1 + A2*EXP(2*(1-1/U)), U = T/TC.
  COMMON/1/AL, BE, GA, DE, EP, DCRT, TCRT, PCRT, DGAT, DTRP, TTRP, PTRP
  COMMON/5/ DDSDT
  COMMON/10/ NFL, EL, AW(6)
1 FORMAT (1HB 9X *DENLIQF = 0, T EXCEEDS TORT. * /)
 2 IF (TCRT-T) 3.4.5
 3 PRINT 1 $ STOP
 4 DENLIQF = DCRT $ DDSDT = -1.0E+100 $ RETURN
 5 XN=TCRT-TTRP $ X=(TCRT-T)/XN $ X2 = X*X $ DXDT = -1.0/XN
 6 XE = X**EL $ V = XE - X $ V1 = EL*XE/X - 1
 8 XP = EXP(ARG) $ XP1T = 2*XP/U/U/TCRT
 9 Y = AW(1) + AW(2)*XP    9 Y = AW(2)*XP1T
10 V1T = V1*DXOT $ YNL = DTRP - DCRT
11 DENLIQF = DCRT + YNL*(X + V*Y)
12 DOSDT = YNL*(DXDT + V*Y1T + V1T*Y)
                                   £
                                         RETURN $
                                                   END
```

FUNCTION FINDTMF(P)

GIVEN P ON THE MELTING LINE, FIND T FOR METHANE.

COMMON/1/AL,BE,GA,DE,EP, DCRT,TCRT,PCRT, DGAT,DTRP,TTRP,PTRP

DATA (QP=1.01325),(E=1.85),(A=1884.43)

1 AQ = A\*QP \$ X = (P-PTRP)/AQ + 1 \$ FINDTMF = TTRP\*X\*\*(1.0/E)

9 RETURN \$ END

FUNCTION FINDTSF(P) GIVEN VAPOR PRESSURE P, ITERATE T TO MINIMIZE (P-PC). COMMON/1/AL, BE, GA, DE, EP, DCRT, TCRT, PCRT, DGAT, DTRP, TTRP, PTRP COMMON/3/DPDT, D2PDT2, DPSDT, DP PDT, DPDD, DPDR, DTSDR, DTHDR 1 FORMAT (1H0 9X \*FINDTSF = 0, FAILS TO CONVERGE. \* / ) 2 FORMAT(1HO 9X \*FINDTSF = 0, P EXCEEDS PCRT. \* / ) 3 IF (P-PCRT) 4,11,12 4 T = 200 \$ 00 9 J=1,50 \$ DP = P - PSATF(T) \$ ADP = ABS (DP) 5 IF(ADP/P-1.0E-6) 10,6,6 6 IF(ADP/DPSDT/T-1.0E-6) 10,7,7 8 T = TCRT9 CONTINUE \$ PRINT 1 \$ STOP 10 FINDTSF = T \$ RETURN 11 FINDTSF = TCRT Б RETURN 12 PRINT 2 \$ STOP \$ END

```
SUBROUTINE GENEOUS
C
     GIVEN P,T FOR THE HOMOGENEOUS DOMAIN -
     GET DEN AND FUNCTIONS AT ANY TEMPERATURE.
      COMMON/3/DPDT, D2PDT2, DPSDT, DPMDT, DPDD, DPDR, DTSDR, DTHDR
      COMMON/8/ IN, IK, P,T, DEN, E, H,S, CV,CP,CSAT, W, WK
      COMMON/12/ DELS. DELCV
      COMMON/19/ KD
      COMMON/99/ TI, EZZ, EZ, SZ, CVZ, HZ, CPZ
      DATA (Q=1.01325), (G=0.083145)
    3 TI = T $ CALL IDEAL $ IF (P.GT.0) 4,10
    4 DEN = DB = FINDENF(T,P) $ N = 11 $ LD = KD $ DA = 0
    5 E = EZZ + EZ + EDELF(0,N,T,DA,DB,LD)   8 H = E + 100*P/DB
    6 S = SZ + DELS - 100*G*ALOG(G*T*DB/Q)
    7 CV = CVZ + DELCV
                         $
                             PX = PVTF(T, DB, 1)
    8 \text{ CP} = \text{CV} + 100 \text{*T/DPDD*(DPDT/DB)**2}
    9 W = SQRT (WK*CP*DPDD/CV) $
                                    RETURN
   10 DEN=S=0 $ E = EZZ + EZ $ H = E + 100 FGFT $ CV=CVZ $ CP=CPZ
   12 W = SQRT(WK*CP*G*T/CV) $ RETURN $ END
```

```
SUBROUTINE GENIUS
C
    SAVES COMPUTER TIME WHEN TABULATING FUNCTIONS ALONG ISOBARS.
    SAVES DEN, E, S, CV ALONG ISOBARS FOR USE IN INTEGRATING TO NEXT
C
    HIGHER ISOBAR. VALID ONLY FOR MONOTONICALLY INCREASING ISOBAR
C
    PRESSURES. AND AT TEMPS. T = INTEGER MULTIPLES OF 10 K.
     COMMON/3/DPDT.D2PDT2.DPSDT.DPMDT.DPDD.DPDR.DTSDR.DTHDR
     COMMON/8/ IN, IK, P,T, CEN, E, H, S, CV, CP, CSAT, W, WK
     COMMON/12/ DELS, DELCV
     COMMON/19/ KD
     DIMENSION DK(70), EK(70), SK(70), CK(70)
   1 FORMAT (1HD 9X *GENIUS T NOT INTEGRAL. * / )
   2 J = T/10 $
                   IF(T - 10*J) 3,4
   3 PRINT 1
              $
                   STOP
    4 IF (IK. EQ. IN) 5.9
   5 KD = LD = 2 $ CALL GENEOUS $ KD = 1
    6 DK(J) = DEN $ EK(J) = E $ SK(J) = S $ CK(J) = CV $ RETURN
    INTEGRATE FROM OLD DEN UP TO NEW DEN ON GIVEN ISOTHERM.
    9 DA = DK(J) $ DK(J) = DEN = DB = FINDENF(?,P) $ N = 10
   11 EK(J) = E = EK(J) + EDELF(1,N,T,DA,DB,LD)    H = E + 100*P/DB
   13 SK(J) = S = SK(J) + DELS $ CK(J) = CV = CK(J) + DELCV
    NOW GET NEW DP/DT, DP/DD, CP, W.
   30 \text{ W} = \text{SQRT}(WK*CP*DPDD/CV)
                              $
                                 RETURN $ END
```

```
FUNCTION HSATF(T)
     NF3 SATLIQ ENTHALPY, J/MOL, RDG/NBS, NOV. 13, 1979.
     BASED ON EZZ = HZZ = 12340.685 J/MOL.
     FOR 35 POINTS, TTRP THRU TCRT, RMSPCT = 0.003.
C
     DEFINE YH = (H-HC)/(HT-HC), X = (TC-T)/(TC-TT), WHEN -
     YH = X + (XE-X)^{+}(A1 + A2^{+}X + A3^{+}X2 + ...)
      DIMENSION AH(8)
      DATA (NFH=8), (TTRP=66.35), (TCRT=234.0)
      DATA (EH=0.35), (HTRP=0.0), (HCRT=15460.422)
      DATA(AH = 0.4046924015, -0.222397394, 1.684556929, -5.424338100,
    1 8.875748786, -7.740104222, 3.181911763, -0.4505783783)
1 FORMAT(1H0 9X 3HT =F10.5, * IN HSATF(T).*/)
    2 IF (TCRT-T) 3,4,5
    3 PRINT 1, T $ STOP
    4 HSATF = HCRT $ RETURN
    5 IF(T.EQ.TTRP) 6,7
    6 \text{ HSATF} = 0.0
                    $
                          RETURN
    7 \times = (TCRT-T)/(TCRT-TTRP) $ V = X**EH - X $ FX = X
    8 DO 9 K=1,NFH $ FX = FX + V + AH(K) + X + + (K-1)
    9 CONTINUE $ HSATF = HCRT*(1 - FX) $ RETURN $ END
```

```
SUBROUTINE IDEAL
  NITROGEN TFIFLUORIDE IDEAL GAS FUNCTIONS, R.D.G., 1/23/79.
  CPZ/R = 4 + (A1 + A2/X + A3/X2 + ...) + EXP(-E/X), X = T/100.
   COMMON/99/ TI, EZZ, EZ, SZ, CVZ, HZ, CPZ
   DIMENSION A(5)
   DATA (NF=5), (E=8.76), (R=8.3145)
   DATA(A=6.1189724,48.162688,228.231405,-249.067052.564.293045)
 1 XI = TI/100 $ XP = EXP(-E/XI)
 4 CP = 4.0 $ DO 5 K=1.NF
 5 CP = CP + A(K) + XP + XI + (1-K)
 NUMERICAL INTEGRATION FOR HZ/RT, SZ/R. START AT T = 300.
 9 SI = 4.184 + 62.378/R $ HI = 4184.0 + (0.024 + 2.832)/300/R
10 H = S = 0 \$ N = ABS(TI-300)/2 + 2 \$ DX = (XI-3)/N
11 DO 20 J=1,N $ X = 3.0 + (J-0.5) + DX $ XP = EXP(-E/X)
15 CPX = 4.0 $ DO 16 K=1,NF
16 \text{ CPX} = \text{CPX} + A(K) + XP + X + + (1 - K)
17 H = H + CPX+DX \$ S = S + CPX+DX/X
20 CONTINUE S = SI + S + H = (H + 3 + HI)/XI
  CONVERT TO JOULES, MOLES, KELVINS.
21 HZ = H*R*TI \$ EZ = HZ - R*TI \$ SZ = R*S
22 CPZ = R*CP $ CVZ = CPZ - R $ RETURN $ END
```

```
FUNCTION PMELTF(T)

C METHANE SOLID-LIQUID MELTING PRESSURE, BAR.

COMMON/1/AL,BE,GA,DE,EP, DCRT,TCRT,PCRT, DGAT,DTRP,TTRP,PTRP

COMMON/3/DPDT,D2PDT2,DPSDT,DPMDT,DPDD,DPDR,DTSDR,DTHDR

DATA (QP=1.01325),(E=1.85),(A=1884.43)

1 X = T/TTRP $ XE = X**E $ AQ = A*QP

2 PMELTF = PTRP + AQ*(XE-1)

3 DPMDT = AQ*E*XE/X/TTRP $ RETURN $ END
```

```
SUBROUTINE JTLOCUS
C
    DERIVE THE J-T INVERSION CURVE. USE ROUTINE DELTAF (T.DI).
     COMMON/1/AL, BE, GA, DE, EP, DCRT, TCRT, PCRT, DGAT, DTRP, TTRP, PTRP
     DIMENSION DK(60), DN(60), TT(60), PP(60)
     DATA (A=1.29079), (B=0.49734)
   1 FORMAT (1H1 16X *THE JOULE-THOMSON INVERSION LOCUS FOR NITROGEN TRI
    1FLUORIDE. * //
    2 17X 3HT,K 8X2HDI 5X5HMOL/L 5X5HP,BAR
      7X3HT,K 8X2HDI 5X5HMOL/L 5X5HP,BAR )
   2 FORMAT(10X I10, 2F10.3, F10.2, I10, 2F10.3, F10.2)
C
    SAVE INITIAL. TRIAL DENSITY. DK(I) = DI.
   5 TA = 180 $
                 NP = 52
   6 PRINT 1 $ DO 25 I=1.NP $ DX = 1.6
   10 IF(T-TCRT) 11,12,12
  11 DL = DENLIQF(T) \$ IF(DI.LT.DL) 23.12
  12 SS = DELTAF(T,DI) $ DO 20 IT=1,20
  14 D=DI-DX $ SL=DELTAF(T,D) $
                                 D=DI+DX $ SP=DELTAF(T.D)
  15 IF (SS-SL) 18,16,16
  16 IF (SP-SL) 19,17,17
  18 IF(SS-SP) 20,20,19
  19 SS = SP $ DI = DI + DX
  20 DX = DX/2    TT(I) = T    DN(I) = DI    PP(I) = PVTF(T,DI,0)
  21 GO TO 25
  23 TT(I) = T    SDK(I) = DN(I) = PP(I) = 0
  25 CONTINUE $ N = NP/2 $ DO 29 J=1.N $ K = J + N
  26 IT = TT(J) $ ITT = TT(K)
  29 PRINT 2, IT, DK(J), DN(J), PP(J), ITT, DK(K), DN(K), PP(K)
  30 RETURN
```

```
FUNCTION DELTAF(T,D)

GET (T*DP/DT - D*DP/DD) FOR THE J-T INVERSION CURVE.
COMMON/1/AL,BE,GA,DE,EP, DCRT,TCRT,PCRT, DGAT,DTRP,TTRP,PTRP
COMMON/3/DPDT,D2PDT2,DPSDT,DPMDT,DPDD,DPDR,DTSDR,DTHDR

IF(T-TCRT) 2,4,4

DL = DENLIQF(T) & IF(D-DL) 3,3,4

DELTAF = 1.0E+100 & RETURN

P = PVTF(T,D,1)

DELTAF = ABS (T*DPDT-D*DPDD) & RETURN & END
```

```
SUBROUTINE PRINTIT
  PRINTOUT ISOCHORES AND ISOTHERMS.
   COMMON/1/AL, BE, GA, DE, EP, DCRT, TCRT, PCRT, DGAT, DTRP, TTRP, PTRP
   COMMON/3/DPDT.D2PDT2.DPSDT.DP 1DT.DPDD.DPDR.DTSDR.DTHDR
   DATA (R = 0.083145)
 1 FORMAT(I5, 2F10.0)
 5 FORMAT(1X)
 6 FORMAT(1H1 25X *NF3 ISOCHORE AT*F7.3, * MOL/L*// 17X 3HT,K
  1 5X5HP,BAR 9X1HZ 5X5HDP/DD 5X5HDP/DT 5X7HD2P/DT2 )
 7 FORMAT(10X 2F10.3, F10.5, F10.3, F10.4, F12.6)
  8 FORMAT(1H1 25X *NF3 ISOTHERM AT*F7.2, * DEG. K*// 15X 5HMOL/L
  1 5X5HP.BAR 9X1HZ 5X5HDP/DD 5X5HDP/DT 5X7HD2P/DT2 )
 9 FORMAT(10X 2F10.3, F10.5, F10.3, F10.4, F12.6)
  PRINTOUT THE ISOCHORES.
20 DO 60 I=1,27 $ IF(I.EQ.1) 21,22
21 ON = 0.5 $ GO TO 30
22 IF(I.EQ.9) 23,24
23 DN = DCRT $ GO TO 30
24 DN = I - 1
30 PRINT 6. DN $ TS = TSATF(DN) $ PS = PVTF(TS.DN.1)
31 Z = PS/DN/R/TS
32 PRINT 7, TS,PS,Z, DPDD,DPDT,D2PDT2
38 IF(I.LT.10) 39,40
39 IT = 8 $ GO TO 50
40 IF(I.LT.14) 41,42
41 IT = 4 $ GO TO 50
42 IF(I.LT.19) 43,44
43 \text{ IT} = 2 \$ 60 \text{ TO } 50
44 \text{ IT} = 1
50 D0 59 J=68.504.IT $ TT = J $ IF(TT-TS) 59.59.52
52 PP = PVTF(TT,DN,1) $ IF(PP.GT.360) 60,55
55 Z = PP/DN/R/TT
58 PRINT 7, TT, PP, Z, DPDD, OPDT, D2PDT2
59 CONTINUE
60 CONTINUE
   PRINTOUT THE ISOTHERMS.
100 DO 130 I=1.99 $ READ 1, IDD, TT,DX $ IF(IDD) 101,999
101 PRINT 8, TT $ PM = PMELTF(TT)
102 IF(TT-TCRT) 103,103,104
103 DG = DENGASF(TT) $ DL = DENLIQF(TT)
104 L = 0 $ DS = DX
105 DO 120 N=1,1500 $ DN = N*DS $ IF(TT-TCRT) 106,106,117
106 IF(DN.GE.DG.AND.DN.LE.DL) 107,117
108 PG = PVTF(T_*DG_*1) $ Z = PG/DG/R/TT
109 PRINT 9, DG,PG,Z, DPDD,DPDT,D2PDT2
110 PRINT 5
111 PL = PVTF(TT,DL,1) SZ = PL/DL/R/TT
112 PRINT 9, DL,PL,Z, DPDD,DPDT,D2PDT2
116 GO TO 120
117 PP = PVTF(TT.DN.1) $ IF(PP.GT.PM.OR.PP.GT.400) 130,118
118 Z = PP/DN/R/TT
119 PRINT 9, DN,PP,Z, DPDD,DPDT,D2PDT2
120 CONTINUE
130 CONTINUE
999 RETURN $ END
```

```
FUNCTION PSATF(T)
C
    LN(P) = P1 + P2/X + P3*X + P4*X2 + P5*X3 + P6*X*(1-X)**EPP.
    WHERE, X E T/TCRT, U E 1/X.
     COMMON/1/AL.BE.GA.DE.EP. DCRT.TCRT.PCRT. DGAT.DTRP.TTRP.PTRP
     COMMON/2/ NFP, EPP, PJ(6)
     COMMON/3/DPDT, D2PDT2, DPSDT, DPMDT, DPDD, DPDR, DTSDR, DTHDR
   1 FORMAT(1H0 9X *T ABOVE TORT IN PSATF(T). * / )
   3 IF(X.LE.0) 4,5
 4 PSATF = DPSDT = 0 $ RETURN
   5 U = 1.0/X  $ U1T = -X1T/X/X
   6 V = 1.0 - X  3 IF(V) 7,8,9
   7 PRINT 1
                 STOP
              3
   8 Z = Z1 = 0 $ GO TO 10
   9 Z = V**EPP $ Z1 = -EPP*Z/V
  10 A=PJ(1) $ B=PJ(2) $ C=PJ(3) $ D=PJ(4) $ E=PJ(5) $ F=PJ(6)
  11 PL = A + 8*U + C*X + D*X2 + E*X3 + F*X*Z
  12 PL1T = B*U1T + (C + 2*D*X + 3*E*X2 + F*(X*Z1+Z))*X1T
  16 PSATF = EXP(PL) $ DPSDT = PL1T*PSATF $ RETURN $ END
```

```
SUBROUTINE PYTDATA
C
     NITROGEN TRIFLUORIDE EQNSTATE, R.D.G. (NBS), SEPT. 24, (1979).
      COMMON GK,GKK, B1,B2,B3,B4,B5, C1,C2,C3, E1,E2,E3, ER,IX
      COMM CN/1 / AL, BE, GA, DE, EP, DCRT, TCRT, PCRT, DGA T, DTRP, TTRP, PTRP
      COMMON/2/ NFP, EPP, PJ(6)
      COMMON/7/ NFG, GE, AV(6)
      COMMON/8/ IN, IK, P,T, DEN, E,H,S, CV,CP,CSAT, W,WK
      COMMON/10/ NFL, EL, AW(6)
      COMMON/13/ ZCRT, ZSAT, DZSDT, ZFX, FRT, DFRTDT
      COMMON/19/ KD
      COMMON/99/ TI, EZZ, EZ, SZ, CVZ, HZ, CPZ
  15 NFP=6 $ EPP=1.75 $ NFG=3 $ NFL=2 $ GE = EL = 1.0/3.0
                       DCRT = 7.92 $ DTRP = 26.32
   17 WM = 71.0019 $
   18 TTRP = 66.35
                   $ TCRT = 234.0 $ GKK = 0.083145 $ GK=GKK*DCRT
   19 PJ(1) = 20.315417602 § PJ(2) = -8.362069370
   20 PJ(3) =-21.398986401 & PJ(4) = 20.162194616
   21 \text{ PJ}(5) = -6.918662727 \text{ } \text{PJ}(6) = 3.677799376
   22 PTRP = PSATF(TTRP) $ PCRT = PSATF(TCRT)
   23 ZCRT = PCRT/DCRT/GKK/TCRT
   25 AV(1) = -0.7109566941 $
                               AV(2) = 0.3800175233
   26 AV(3) = 1.622847586 3 DGAT = DENGASF(TTRP)
   28 AW(1) = 0.754377410 $ AW(2) = 0.027975083
   30 IX=1 $ AL=1 $ GA=1 $ DE=0.5 $ EP=1 $ BE = ER = 0
   31 B1 = 0.55199813920 $ B2 = 0.13268809584 $ B3 = 0.20608495802
   32 E1 = 0.74067409894 $ E2 = 0.29375371520 $ E3 = 0
   33 WK = 103000/WM $ KD = 1 $ EZZ = 12340.685
  99 RETURN $ END
```

```
FUNCTION PVTF(T,D,M)
    NF3 EQNSTATE. PVTF = P.BAR.
    NOTE, M=0 RETURNS DP/DT, D2P/DT2. M=1 RETURNS ALSO DP/DD.
C
C
    P-PSAT = S+GK+(T-TSAT) + S+S+GK+TCRT+F(S,T), WHERE -
    F(S,T) \equiv B(S) * XBF(S,T) + E(S) * XEF(S,T), AND -
C
    B(S) \equiv B1 + B2*S + B3*S2, E(S) \equiv (E1+E2*S)*(S-1)*EXP(-GA*S**IX).
C
            R E DEN/DTRP, S E DEN/DCRT.
    WHERE.
     COMMON GK, GKK, B1, B2, B3, B4, B5, C1, C2, C3, E1, E2, E3, ER, IX
     COMMON/1/AL, BE, GA, DE, EP, DCRT, TCRT, PCRT, DGAT, DTRP, TTRP, PTRP
     COMMON/3/DPDT, D2PDT2, DPSDT, DPMDT, DPDD, DPOR, DTSDR, DTHDR
     COMMON/4/XB1, XB2, XC1, XC2, XE1, XE2, DXBDR, DXCDR, DXEDR
     COMMON/6/ TSAT, THETA, PSAT
     COMMON/13/ ZCRT, ZSAT, DZSDT, ZFX, FRT, DFRTDT
   1 S = D/DCRT $ S2=S*S $ S3=S*S2 $ SN=S-1 $ SX=S**IX
   2 GK = DCRT*GKK $ TC = TCRT $ DSDR = DTRP/DCRT
3 RG = S*GK $ GKT = GK*TC $ TSAT = TS = TSATF(D)
   4 THETA = THETAF(0) $ PSAT = PS = PSATF(TS)
   5 XB = XBF(T,D)
                  XE = XEF(T_0)
   10 SE = E1*S2 + E2*S3 $ SM = SE*SN $ E = SM*XP
  13 PVTF = PS + RG*(T-TS) + GKT*F $ FRT=F/S2 $ DFRTDT=F1/S2/TC
  14 DPDT = RG + GK*F1 $ D2PDT2 = GK*F2/TC
                                           3
                                                IF(M) 15,30
  15 BD = (2*B1 + 3*B2*S + 4*B3*S2)*S*DSDR
  17 ED = (SM*XP1 + SM1)*XP*DSDR
                             E*DXEDR + ED*XE
  20 F1 = B*DXBDR + BD*XB +
  26 DPDR = (DPSDT-RG)*DTSDR + (T-TS)*GK*DSDR + GKT*F1
  27 DPDD = DPDR/DTRP
  30 RETURN
            3
                 END
```

```
FUNCTION QVAPXF(T)

C NITROGEN TRIFLUORIDE, OCT. 16, 1969. NBS/RDG.

C FOR 16 THERMALOOP AND 35 CLAPEYRON DATA, RMSPCT = 0.05.

C QVAP/QTRP = X + (XE-X)*(A + B*X + C*X2), WHERE -

X = (TC-T)/(TC-TT), XE = X**E.

DATA (E=0.38), (QT=14.548), (TTRP=66.35), (TCRT=234.0), (XN=167.65)

DATA (A=0.998247122), (B=0.269536103), (C=-0.405010672)

1 FORMAT(1H0 9X *T EXCEEDS TCRT IN QVAPXF(T). * /)

2 IF(TCRT-T) 3,4,5

3 PRINT 1 $ 'STOP

4 QVAPXF = 0 $ RETURN

5 X = (TCRT-T)/XN $ X2 = X*X $ XE = X**E

6 Q = QT*(X + (XE-X)*(A + B*X + C*X2))

7 QVAPXF = Q*1000 $ RETURN $ END
```

```
FUNCTION SSATF(T)
     NF3 SATLIQ ENTROPY, J/MOL/K, RDG/NBS, NOV. 13, 1979.
     FOR 35 POINTS, TTRP THRU TCRT, RMSPCT = 0.002.
C
C
     SSAT - SCRT = A1*U**ES + A2*LN(X) + A3*U + A4*U2 + A5*U3, WHERE -
     X \equiv T/TCRT, U \equiv (1-X).
C
      DIMENSION AS(7)
      DATA (NFS=7), (ES=0.33), (TCRT=234.0), (SCRT=197.03182)
      DATA(AS = -27.04141165, 168.4875348, 117.5913487,
     1 -16.46287979, 241.1959696, -288.5828349, 230.9162107)
    1 FORMAT(1H0 9X 3HT =F10.5, * IN SSATF(T). * / )
    2 IF(TCRT-T) 3,4,5
    3 PRINT 1, 1 $ STOP
    4 SSATF = SCRT & RETURN
    5 X = T/TCRT $ U = 1.0 - X
    6 SSATF = SCRT + AS(1) *U**ES + AS(2) *ALOG(X) $ DO 7 K=3.NFS
    7 SSATF = SSATF + AS(K) *U**(K-2) $ RETURN $ END
```

```
SUBROUTINE TABLIQ
C
     TABULATE NF3 SATURATED LIQUID FUNCTIONS.
      COMMON/1/AL, BE, GA, DE, EP, DCRT, TCRT, PCRT, DGAT, DTRP, TTRP, PTRP
      COMMON/3/DPDT, D2PDT2, DPSDT, DPMCT, DPDD, DPDR, DTSDR, DTHDR
      COMMON/5/ DDSDT
      COMMON/6/ TSAT. THETA. PSAT
      COMMON/8/ IN, IK, P,T, DEN, E,H,S, CV,CP,CSAT, W,WK
      COMMON/9/DNG, EG, HG, SG, CVG, CPG, WG, DPGDT, DPGDD
      DIMENSION TSA(40), PSA(40)
      DATA (G = 0.083145)
    4 FORMAT(1H1 13X *PROPERTIES OF SATURATED LIQUID NITROGEN TRIFLUORID
    1E. * //
     1 14X 1HT 10X1HP 5X3HDEN 7X1HZ 3X5HV.LIQ 6X5HV.GAS
     2 5X6HDPS/DT 3X6HDDL/DT 3X5HDP/DT 6X5HDP/DD /
     3 10X5HDEG K 8X3HBAR 3X5HMOL/L 8X 3X5HL/MOL 6X5HL/MOL
     4 6X5HBAR/K 2X7HMOL/L/K 3X5HBAR/K 2X9HBAR-L/MOL )
    5 FORMAT (5XF10.3, E11.4, F8.3, F8.5, F8.5, 2E11.4, F9.5, F8.3, E11.4)
   11 FORMAT(1H1 13X *PROPERTIES OF SATURATED LIQUID NITROGEN TRIFLUORID
     15. * //
     1 14X1HT 10X1HP 4X5HQ, VAP 8X1HE 8X1HH 8X1HS
     2 6X2HCV 6X2HCS 6X2HCP 6X1HW /
     3 10X5HDEG K 8X3HBAR 4X5HJ/MOL 4X5HJ/MOL 4X5HJ/MOL 2X7HJ/MOL/K
     4 1X7HJ/MOL/K 1X7HJ/MOL/K 1X7HJ/MOL/K 2X5HM/SEC )
   12 FORMAT(5X F10.3, E11.4, 3F9.1, F9.3, 3F8.2, I7)
     FOR PAGE ONE OF TABLIQ.
     REPLACE T = 145 BY BOILING-POINT AT J = 17.
  130 PRINT 4
              \$ NP = 37
  131 00 150 J=1,NP $ IF(J.EQ.1) 132,133
  132 T = TTRP $ GO TO 139
  133 IF (J.EQ.17) 134,135
  134 T = FINDTSF(1.01325)
                           $ GO TO 139
  135 IF(J.EQ.NP) 136,138
  136 T = TCRT \$ DG = DL = DCRT \$ DDLDT = 0
  137 VG = VL = 1.0/DCRT $ GO TO 141
  138 T = 60 + 5*J
      IF(J.EQ.35)
                   T = 232
      IF(J_{\bullet}EQ_{\bullet}36) T = 233
  139 DL = DENLIQF(T) $ DDLDT = DDSDT
  140 DG = DENGASF(T) $ VG = 1/DG $ VL = 1/DL
  141 TSA(J) = T    PX = PVTF(T,DL,1)
  147 PSA(J) = PS = PSAT    Z = PS/DL/G/T
  150 PRINT 5, T,PS,DL,Z, VL,VG, DPSDT,DDLDT, DPDT,DPDD
     FOR PAGE TWO OF TABLIQ.
     USE COEXIST AT ALL TEMPS.
  160 PRINT 11 $ DO 170 J=1, NP $ P = PSA(J)
                                                 T = TSA(J)
  164 CALL COEXIST $ IW = W $
                                   QX = QVAPXF(T)
  170 PRINT 12, T,P,QX, E,H,S, CV,CSAT,CP, IW
```

999 RETURN

3

END

```
SUBROUTINE THERMO
     THERMO IS FOR COMPUTATION AT ANY, RANDOM (P,T) POINT.
C
     THERMO ASSUMES AN ISOBAR IN SINGLE-PHASE ONLY.
     GIVEN (P,T), RETURNS DEN, E,H,S, CV,CP,W, DPDT,DPDD.
C
     ENTRIES BELOW FOR PHASE BOUNDARIES ASSUME A GIVEN ISOBAR P.
     NITROGEN TRIFLUORIDE ROUTINES, RDG/NBS, NOV. 13, 1979.
     COMMON/1/AL, BE, GA, DE, EP, DCRT, TCRT, PCRT, DGAT, DTRP, TTRP, PTRP
      COMMON /3 /DPDT, D2PDT2, DPSDT, DPMDT, DPDD, DPDR, DTSDR, DTHDR
      COMMON/8/ IN, IK, P,T, DEN, E,H,S, CV,CP,CSAT, W,WK
      COMMON/9/ DNG, EG, HG, SG, CVG, CPG, WG, DPGDT, DPGDD
    1 FORMAT(1H0 9X *THERMO T =* F8.3, 5H, P = E12.5/
     1 10X *T BELOW TTRP, NOT DEFINED. * / )
    2 FORMAT(1H0 9X *THERMO T = F F8.3, 5H. P = E12.5/
     1 10X *P ABOVE MELTING LINE, NOT DEFINED. * / )
    3 FORMAT(1HG 9X *THERMO T =* F8.3, 5H, P = E12.5/
     1 10X *DOUBLE-VALUED AT COEXISTENCE. * / )
    4 FORMAT (1H0 9X *THERMO T = * F8.3, 5H, P = E12.5/
    1 10X *CP, CV, W UNAVAILABLE AT TCRT AND P.GT.PCRT. * / )
   10 IF(T.LT.TTRP) 11,13
   11 DEN=E=H=S=CV=CP=W=DPDT=DPDD=0 $ PRINT 1, T,P $
   13 IF (T.LT. TTRP+20) 14.20
   14 PM = PMELTF(T) $ IF(P.GT.PM) 15,20
   15 DEN=E=H=S=CV=CP=W=DPDT=DPDD=0 $ PRINT 2, T,P $ RETURN
   20 IF(P-PCRT) 21,30,35
     SUBCRITICAL ISOBARS.
   21 TS = FINDTSF(P) \$ IF(T-TS) 22,23,25
                       RETURN
   22 CALL COMPRLQ $
   23 DEN=E=H=S=CV=CP=W=DPDT=DPDD=Q $ PRINT 3, T,P $ RETURN
   25 CALL GENEOUS & RETURN
     THE CRITICAL ISOBAR.
   30 IF(T.LE.TCRT) 31,32
   31 CALL COMPRLQ
                   $ RETURN
   32 CALL GENEOUS
                        RETURN
                    3
     SUPERCRITICAL ISOBARS.
   35 IF(T-TCRT) 36,37,39
   36 CALL COMPRLQ $ RETURN
   37 CALL COMPRLQ $ CP=CV=W=0 $ PRINT 4, T,P $ RETURN
   39 CALL GENEOUS
                    3
                         RETURN
      ENTRY THERMOM
C
     THERMOM FOR GIVEN ISOBAR AT THE MELTING LINE, GET T.
     RETURNS T.DEN. E.H.S. CV.CP.W. DPMDT, DPDT, DPDD.
   40 T = FINDTMF(P) $ CALL COMPRLQ
                                      $
                                            RETURN
      ENTRY THERMOL
C
     THERMOL FOR GIVEN ISOBAR AT SATURATED LIQUID LINE, GET T.
     RETURNS T, DEN, E, H, S, CV, CP, CSAT, W, DPSDT, DDSDT, DPDT, DPDD.
   43 T = FINDTSF(P) $ CALL COEXIST $ RETURN
      ENTRY THERMOV
     THERMOV FOR GIVEN ISOBAR AT THE SATURATED VAPOR LINE, GET T.
     RETURNS T, DEN, E, H, S, CV, CP, W, DPSDT, DDSDT, DPDT, DPDD.
   45 T = FINDTSF(P) $ CALL COEXIST $ DEN=DNG $ E=EG $ H=HG $ S=SG
   47 CV=CVG $ CP=CPG $ W=WG $ DPDT=DPGDT $ DPDD=DPGDD
   50 RETURN
                   END
```

```
FUNCTION THETAF(DEN)
     THETA = TSAT*EXP(U(S)).
C
     LET Q = (S-1)/(ST-1), WHERE ST = DTRP/DCRT, THEN -
C
     IF S < 1, U = AL^{+}Q^{++}3,
                              IF S > 1. U = -AL+Q+3.
      COMMON/1/AL, BE, GA, DE, EP, DCRT, TCRT, PCRT, DGAT, DTRP, TTRP, PTRP
      COMMON/3/DPDT, D2PDT2, DPSDT, DPMDT, DPDD, DPDR, DTSDR, DTHDR
      COMMON/6/ TSAT, THETA, PSAT
    1 S = DEN/DCRT $ DSDR = DTRP/DCRT $ C = DSDR-1
    2 Q = {S-1}/C    Q2 = Q+Q    U = AL+Q+Q2
    3 U1 = AL + 3 + Q2 + DSDR/C
                            3
                                IF(Q) 5,9,4
    4 U = -U
             $ U1 = -U1
    5 XP = EXP(U)
                    $ THETAF = TSAT + XP
    6 DTHOR = (TSAT*U1 + DTSDR)*XP
                                     $
                                            RETURN
    9 THETAF = TCRT & DTHDR = 0
                                    $
                                           RETURN
                                                  $
                                                        END
```

```
FUNCTION TSATF(DEN)
    ITERATE T TO MINIMIZE (DEN-DCALC) VIA DENGASF(T). DENLIGF(T).
    IF ITERATION FAILS, PRINTOUT ONCE ONLY AND STOP AT K = 2.
     COMMON/1 /AL, BE, GA, DE, EP, DCRT, TCRT, PCRT, DGAT, DTRP, TTRP, PTRP
     COMMON/3/DPDT, D2PDT2, DPSDT, DPMDT, DPDD, DPDR, DTSDR, DTHDR
     COMMON/5/ DDSDT
     DATA (Q= 2.0) (FN=6.3890561)
C
    NOTE.
           FN E EXP(Q) - 1.0.
   1 FORMAT (1H1 14X *TSATF (DEN) FAILS AT DEN =* E15.7//
    1 15X 5HD CALC 13X2HDD 10X5HDDSDT 13X2HDT 12X3HT,K )
   2 FORMAT(5X 4E15.7, E16.8)
     K = 0 % D = DEN % IF(D.LE.0) 3,4
   3 TSATF = 0 $ DTSDR = 1.0E+100 $
                                        RETURN
   5 ST=DGAT/DCRT $ F=ALOG(S)/ALOG(ST)*((1-S)/(1-ST))**2 $ GO TO 7
   6 ST=DTRP/DCRT S = ((S-1)/(ST-1))**3 F = (EXP(Q*U)-1)/FN
     T = TCRT/(YN*F+1)
   8 DO 20 J=1,50 $ IF(D-DCRT) 9,30,10
   9 DC = DENGASF(T) $ GC TO 11
  10 DC = DENLIQF(T)
  11 DD = D - DC $ IF(ABS(DD/D).LT.1.0E-7) 25.12
  12 DT = DD/DDSDT $ IF(ABS(DT/T).LT.1.0E-7) 25.13
  13 T = T + OT $ IF(T) 14,14,15
  14 T = TTRP $ GO TO 18
  15 IF (T.LT. TCRT) 18.16
  16 T = TCRT - 0.00001
  18 IF(K.EQ.1) PRINT 2, DC, DD, DDSDT, DT, T
  20 CONTINUE \$ K = K+1 \$ IF(K.NE.1)
                       GO TO 4
  21 PRINT 1, DEN
                  3
  25 TSATF = T $ DTSDR = DTRP/DDSDT $ RETURN
  30 TSATF = TCRT $ DTSDR = 0 $ RETURN $ END
```

```
FUNCTION XBF(T.D)
    XBF = SQRT(T/TC) + LN(T/TS) = Q(T) + Z(R,T),
C
     COMMON/1/AL, BE, GA, DE, EP, DCRT, TCRT, PCRT, DGAT, DTRP, TTRP, PTRP
     COMMON/3/DPDT, D2PDT2, DPSDT, DPMDT, DPDD, DPDR, DTSDR, DTHDR
     COMMON/4/XB1, XB2, XC1, XC2, XE1, XE2, DXBDR, DXCDR, DXEDR
     COMMON/6/ TSAT, THETA, PSAT
   1 TC = TCRT $ TS = TSAT $ X = T/TC
   2 U = T/TS $ U1X = TC/TS $ U1R = -U*DTSDR/TS
   3 Z = ALOG(U)
                  $ Z1R=U1R/U $ Z1X=U1X/U $ Z2X=-Z1X*Z1X
                   $Q1 = 0.5/Q $Q2 = -Q1/2/X
   4 Q = SQRT(X)
   6 \times B2 = Q \times Z2X + Q1 \times 2 \times Z1X + Q2 \times Z
                                        RETURN $ END
```

```
FUNCTION XEF(T.D)
C
    THIS H-FORM FROM NBS J.RES. 73A(6), 585, DEC. (1969).
C
    XEF = PSI - PSISAT, PSI = A*F(T) + B*H(R,T), WHERE -
C
    F(T) \equiv EXP(C*(1-X)),
                       W E (1-TH/T). WE E W**EX. AND -
    H(R,T) \equiv 1 - (W - WE/E)/(1-1/E).
     COMMON/1/AL, BE, GA, DE, EP, DCRT, TCRT, PCRT, DGAT, DTRP, TTRP, PTRP
     COMMON/3/DPDT, D2PDT2, DPSDT, DPMDT, DPDD, DPDR, DTSDR, DTHDR
     COMMON/4/XB1, XB2, XC1, XC2, XE1, XE2, DXBDR, DXCDR, DXEDR
     COMMON/6/ TSAT, THETA, PSAT
     DATA (EX = 1.10)
   1 A=DE $ B=1-A $ C=EP $ E=EX $ TC=TCRT $ TS=TSAT $ TH=THETA
   2 EK = E/(E-1)
                     $ X=T/TC $ XS=TS/TC $ XS1=DTSDR/TC
   3 W = 1.0 - TH/T $ IF(W) 30,30,4
   5 W1R = -DTHDR/T $ W1X = TH/T/X $ W2X = -2*W1X/X
   6 WE = W**E $ WE1 = E*WE/W $ WE1R = WE1*W1R
   7 WE1X = WE1*W1X $ WE2X = WE1*W2X + (E-1)*WE1/W*W1X*W1X
   8 H = 1 - EK^{+}(W-WE/E)  8 H1R = -EK^{+}(W1R-WE1R/E)
   9 H1X = -EK*(W1X-WE1X/E)
                         $ H2X = -EK+(W2X-WE2X/E)
  10 P = A*F + B*H $ P1R = B*H1R
  12 \text{ WS} = 1.0 - \text{TH/TS} $ IF(WS) 13,13,14
  13 FS = HS = 1 $ FS1 = HS1 = 0 $ GO TO 22
  14 WS1 = (TH*DTSDR/TS - DTHDR)/TS
  15 WSE = WS**E $ WSE1 = E*WSE*WS1/WS
  20 FS = EXP(C*(1-XS)) $ FS1 = -C*XS1*FS
  22 PS = A*FS + B*HS $ PS1 = A*FS1 + B*HS1
  $
                                         RETURN
  30 XEF = XE1 = XE2 = DXECR = 0 $ RETURN $ END
```

```
PROGRAM ZIEGLER (OUTPUT)
C
              ESTIM. V.P. AND QVAP FROM TRIPLE- TO BOILING-POINTS.
    USING ENTHALPY AND ENTROPY CLOSED LOOPS.
     COMMON/1/ TA, TB, PB, QB, DELH, DELS
     COMMON/2/ EZA, HZA, SZA, HGB, SGB, DHLAB, DSLAB
      COMMON/3/DPDT,D2PDT2,DPSDT:DPMDT,DPDD,DPDR,DTSDR,DTHDR
     COMMON/9/ PZIP, BZ, DBZDT, DPZDT, DZDD
      COMMON/99/ TI, EZZ, EZ, SZ, CVZ, HZ, CPZ
      DIMENSION QK(2),TK(150),DK(150),PIK(150),PK(150),QJ(150)
    1 FORMAT(I5, F1J.3, E15.6)
    2 FORMAT(I5, F10.3, F10.3)
    3 FORMAT(1H1 11X *NF3 ESTIM. V.P., BAR, AND QVAP, KJ/MOL, RDG/NBS.*//
     1 12X 4HTB =F10.5, 6H, PB =F8.5, 6H, DB =F9.6/
    2 12X5HEZB =F7.1, 7H, EGB =F7.1, 7H, HZB =F8.1, 7H, HGB =F8.1/
     3 12X 5HSZB =F9.4, 7H, SGB =F9.4, 6H, QB =F8.1/ )
    4 FORMAT(7X 3HT,K 8X2HPI 6X5HP,BAR 5X5HMOL/L 6X3HHZA 6X3HHGA
     1 6X3HSZA 6X3HSGA 4X5HDHGAB 4X5HDHLAB 4X5HDSGAB 4X5HDSLAB
     2 5X3HQAH 5X3HQAS )
    5 FORMAT(2XF8.2, E10.4, E11.5, E10.4, 2F9.1, 2F9.3, 2F9.1, 2F9.3, 2F8.3)
    6 FORMAT (12X 3HT, K 4X5H100/T 7X5HP, EQN 7X5HP, BAR 6X5HLN(P)
    1 4X8HDG, MOL/L 3X5HQ, EQN 3X5HQ, VAP )
    7 FORMAT(5X F10.2, F9.5, 2E12.5, F11.5, E12.5, 2F8.3)
    8 TTRP = 66.36 $ PB = 1.01325 $ TB = 144.10
    NF3 QVAP, J/MOL VIA PIERCE/AEROJET AT BP = 144.10 K.
C
    9 QK(1) = QK(2) = 11587.0
     GET HGB, SGB FOR SATVAPOR AT THE BOILING POINT.
   10 TI = TB
              $ CALL IDEAL $ EZB=EZ $ HZB=HZ
   11 DNB = FINDENF(TB,PB) $ EGB = EZ + EDELF(TB,DNB)
   12 SG8 = SZ + DELS $ HG3 = EGB + 100*PB/DNB
                 QB = QK(I)
   14 I = 1 B
   15 PRINT 3, TB, PB, DNB, EZB, EGB, HZB, HGB, SZB, SGB, QB $
                                                            PRINT 4
     DO TEMPERATURES FROM TRIPLE- TO BOILING-POINTS -
   20 DO 50 J=1,78 $ IF(J.EQ.1) 21,22
   21 TA = T = TTRP $ GO TO 23
   22 TA = T = 66 + J
     GET EZA, HZA, SZA AT T = TA.
   23 TI = TA & CALL IDEAL & EZA=EZ & HZA=HZ & SZA=SZ
C
     GET DHLAB, DSLAB FOR THE SATDLIQUID FROM TA TO TB.
   24 CALL CSATSUM $ DHLA3 = DELH $ DSLAB = DELS
     NOW ITERATE P (T=TA) TO MINIMIZE (QAH - QAS).
   36 P = PI = PSATF(T) \$ DP = P/2 \$ SS = DELTAF(T,P)
   31 DO 40 IT=1,15 $ PL = P-DP $ SL = DELTAF(T,PL)
   32 PP = P+DP \$ SP = DELTAF (T,PP)
   35 IF(SL-SS) 36,36,38
   36 IF(SL-SP) 37,37,39
   37 SS = SL
              $ P = P - DP $ GO TO 40
   38 IF(SP-SS) 39,40,40
   39 SS = SP \$ P = P + DP
                     DNA = FINDENF(T,P)
   40 DP = DP/2
                 8
     USE FINAL P TO GET DNA, HGA, SGA, DHGAB, DSGAB,
     AND THEN, VIA LOOP, GET QAH, QAS.
   42 EGA = EZA + EDELF(T, DNA) $ SGA = SZA + DELS
   43 HGA = EGA + 100*P/DNA $ DHGAB=HGB-HGA $ DSGAB=SGB-SGA
   44 QAH = QB + DHLAB - DHGAB $ QAS = TA*(QB/TB + DSLAB - DSGAB)
   45 QAH = QAH/1000 $ QAS = QAS/1000 $ PIK(J) = PI
   46 TK(J)=TA $ DK(J)=DNA $ PK(J)=P $ QJ(J) = (QAH+QAS)/2
   50 PRINT 5, TA, PI, P, DNA, HZA, HGA, SZA, SGA, DHGAB, DHLAB,
     1 DSGAB, DSLAB, QAH, QAS
```

```
C     PRINT T,1/T, PEQN,P,LN(P), DNA, QEQN,Q, FOR PUBLICATION.
61 PRINT 3, TB,PB,DNB, EZB,EGB, HZB,HGB, SZB,SGB, QB $ PRINT 6
62 DO 99 J=1,78
C 63 IF(J.EQ.50.OR.J.EQ.99) 67,70
C 67 PRINT 3, TB,PB,DNB, EZB,EGB,HZB,HGB,SZB,SGB, QB $ PRINT 6
70 T = TK(J) $ AT = 100/T $ P = PK(J) $ GP = ALOG(P)
71 QE = QVAPXF(T)/1000
C 75 PRINT 7, T,AT, PIK(J),P,GP, DK(J), QE,QJ(J)
80 IDX = 40 $ IF(J.EQ.1) 90,81
81 IT = T/5 $ IF(T-5*IT) 99,90
90 QCALC = 1600*QJ(J)
91 PRINT 7, T,AT, PIK(J),P,GP, DK(J), QE,QJ(J)
C 92 PUNCH 1, IDX,T,P $ PUNCH 1, IDX,T,DK(J) $ PUNCH 2, IDX,T,QCALC
99 CONTINUE $ STOF - $ END
```

SUBROUTINE CSATSUM

GET DELH, DELS ALONG SATDLIQ FROM TA TO TB.

COMMON/1/ TA,TB,PB,QB, DELH,DELS

COMMON/3/DPDT,D2PDT2,DPSDT,DPMDT,DPDD,DPDR,DTSDR,DTHDR

1 E = H = S = 0

2 TR = TB - TA \$ N = ABS(TR)/2 + 2 \$ DT = TR/N

3 DO 8 J=1,N \$ TJ = TA + (J-0.5)\*DT

4 CS = CSATXF(TJ) \$ PS = PSATF(TJ) \$ DS = DENLIQF(TJ)

5 H = H + CS\*DT + 100\*DPSDT\*DT/DS \$ \$ = S + CS\*DT/TJ

8 CONTINUE

9 DELF = H \$ DELS = S \$ RETURN \$ END

FUNCTION DELTAF(T,P) GET DNA, EGA, HGA, SGA FOR SATDVAPOR AT T, P, (T=TA), C GET DHGAB = HGB-HGA, DSGAB = SGB-SGA, C GET QAH, QAS VIA CLOSED LOOPS, THEN, DELTAF E ABS(QAH-QAS). COMMON/1/ TA, TB, PB, QB, DELH, DELS COMMON/2/ EZA, HZA, SZA, HGB, SGB, DHLAB, DSLAB COMMON/99/ TI, EZZ, EZ, SZ, CVZ, HZ, CPZ 1 IF(P.GT.0) 2.9 2 DNA = FINDENF(T,P) \$ EGA = EZA + EDELF(T,DNA) 3 SGA = SZA + DELS & HGA = EGA + 100\*P/DNA 5 DHGAB = HGB - HGA & DSGAB = SGB - SGA 6 QAH = Q8 + DHLAB - DHGAB \$ QAS = T\*(QB/TB + DSLAB - DSGAB) \$ RETURN 8 DELTAF = ABS(QAH-QAS) 9 DELTAF = 1.0E+100 \$ RETURN \$ END

```
FUNCTION DENLIQF(T)
    FOR NITROGEN TRIFLUORIDE, RDG/NBS, 1/23/79.
C
    DEN = DCRT + YNL*(X + (XE-X)*Y), YNL \equiv DTRP - DCRT.
C
C
    Y = A1 + A2*X + A3*X2 + A4*X3.
     COMMON/5/ DDSDT
     DIMENSION AW(4)
     DATA (NFL=4) . (EL=0.35)
     DATA (DCRT=7.92), (DTRP=26.20), (TTRP=66.36), (TCRT=233.90)
     DATA(AW = 0.740994164, 0.129520773, -0.021108622, -0.096307220)
    1 FORMAT(1HG 9X *DENLIQF = 0, T EXCEEDS TCRT. * / )
    2 IF(TCRT-T) 3,4,5
    3 PRINT 1 $ STOP
   4 DENLIGF = DCRT $ DDSDT = -1.0E+10 $ RETURN
   6 XE = X**EL $ V = XE - X $ V1 = EL*XE/X - 1
    8 Y = AW(1) + AW(2) + X + AW(3) + X2 + AW(4) + X + X2
   9 Y1 = AW(2) + 2*AW(3)*X + 3*AW(4)*X2 $ YNL = DTRP - DCRT
   11 DENLIQF = DCRT + YNL*(X + V*Y)
   12 DOSDT = YNL*(1 + V*Y1 + V1*Y)*DXDT $ RETURN $ END
     FUNCTION EDELF (T.D)
     CHANGE OF E.S ON ISOTHERM T FROM DEN = 0 TO DEN = D.
C
    USE VIRIAL EQNSTATE. NOTE DCZ = 7.92 FOR NF3.
C
     DELE = EDELF = -R*(D/DCZ)*T*T*DB(T)/DT,
C
     DELS = -R*LN(D*R*T/P1) - R*(D/DCZ)*(B(T) + T*DB(T)/DT).
     COMMON/1/ TA, TB, PB, QB, DELH, DELS
     COMMCN/9/ PZIP, BZ, DBZDT, DPZDT, DZDD
     DATA (Q=1.01325), (R=0.0831450), (DCZ=7.92)
    1 Z = ZIPF(T,D) \delta EDELF = -100*R*(D/DCZ)*T*T*DBZDT
    2 DELS = ALOG(D*R*T/Q) + (D/DCZ)*(BZ + T*DBZDT)
    9 DELS = -100*R*DELS & RETURN & END
      SUBROUTINE IDEAL
     NITROGEN TRIFLUORIDE IDEAL GAS FUNCTIONS, R.D.G., 1/23/79.
     CPZ/R = 4 + (A1 + A2/X + A3/X2 + ...) + EXP(-E/X), X = T/100.
```

```
COMMON/99/ TI, EZZ, EZ, SZ, CVZ, HZ, CPZ
   DIMENSION A(5)
  DATA (NF=5), (E=8.76), (R=8.3145)
  DATA(A=6.1189724,48.162688,228.231405,-249.067052,564.293045)
 1 NK = NF 3 XI = TI/100 3 XP = EXP(-E/XI)
 2 CP = 4.0  3 CP = 4.0 
 3 \text{ CP} = \text{CP} + A(K) + XP + XI + + (1 - K)
4 SI = 4.184 + 62.378 / R SI = 4.184 + 0 + (0.024 + 2.832) / 300 / R
 NUMERICAL INTEGRATION FOR HZ/R. SZ/R -
5 H = S = 0   S N = ABS(TI-300)/2 + 2   S DX = (XI-3)/N
6 00 10 J=1.N 3 X = 3.0 + (J-0.5) + DX $ XP = EXP(-E/X)
7 CPX = 4.0 $ DO 8 K=1,NK
 8 CPX = CPX + A(K) + XP + X + (1 - K)
                  S = S + CPX*DX/X
9 H = H + CPX*DX
10 CONTINUE 3 H = (HI*3 + H)/XI $ S = SI + S
 CONVERT TO JOULES, MOLES, KELVINS.
11 HZ = R*TI*+ \$ EZ = HZ - R*TI \$ SZ = R*S
12 CPZ = R*CF & CVZ = CPZ - R &
                                       RETURN & END
```

```
FUNCTION FINDENF(T,P)
    GIVEN P,T IN VIRIAL EQN., SOLVE QUADRATIC FOR DEN, MOL/L.
C
    USE VIRIAL EQNSTATE. NOTE DCZ = 7.92 FOR NF3.
     DATA (DCRT=7.92), (TCRT=234.0), (R=0.083145)
     DATA (B1=0.49382731), (B2=-1.30972686), (B3=-0.38983811)
    1 X = T/TCRT  8 B = B1 + B2/X + B3/X/X/X
    2 Q = SQRT(1.0 + 4*P*B/R/T/DCRT)
    3 FINDENF = DCRT*(Q-1)/2/B $ RETURN $ END
      FUNCTION PSATF(T)
     FOR NITROGEN TRIFLUORIDE, RDG/NBS, 1/23/79.
C
C
     LN(P) = P1 + P2*U + (P3 + P4*X + P5*X2 + ...)*(1-X)**EPP.
C
     WHERE, X \equiv T/TCRT, U \equiv (1-1/X).
      COMMON/3/DPDT, D2PDT2, DPSDT, DPMDT, DPDD, DP DR, DTSDR, DTHDR
      DIMENSION PJ(4)
      DATA (NFP=4), (EPP=1.95), (TCRT=233.90)
      DATA(PJ = 3.81146639, 6.28921982, -1.95516249, 4.51743327)
    1 FORMAT(1HO 9X *T ABOVE TORT IN PSATF(T). * / )
    2 X = T/TCRT $ X2 = X*X $ X1T = 1.0/TCRT
    3 U = 1.0 - 1/X  5 U1T = 1.0/X/T
    4 V = 1.0 - X  3 IF(V) 7.8.9
    7 PRINT 1
              3
                 STOP
    8 Z = Z1 = 0  $ GO TO 10
    9 Z = V**EPP $ Z1 = -EPP*Z/V
   10 S = S1 = 0 $ D0 13 K=3,NFP $ L = K-3 $ XL = X^{**}L
   13 CONTINUE
   14 PL = PJ(1) + PJ(2)*U + S*Z
   15 PL1T = PJ(2)*U1T + (S*Z1 + S1*Z)*X1T
   16 PSATF = EXP(PL) $ DPSDT = PL1T*PSATF $ RETURN $ END
     FUNCTION QVAPXF(T)
C
    NF3 AEROJET FORMULA, J/MOL.
     DATA (EM=0.354), (EN=0.456), (TC=233.9)
     DATA (A=3323.72) . (B=623.265)
    1 X = 1.0 - T/TC & Q = A*X**EM + B*X**EN
    2 QVAPXF = 4.184*Q $
                           RETURN $ END
     FUNCTION ZIPF (T,D)
    ISOBUTANE VIRIAL EQN., R.D.G., SEPT., 1978.
C
    CRITICAL CONSTS. FOR NF3.
C
    Z(T,D) = 1 + B(X)*S, X \equiv T/TCRT, S \equiv DEN/DCRT.
                               DEN IN MOL/L.
    B(X) = B1 + B2/X + B3/X3.
     COMMON/9/ PZIP, BZ, DBZDT, DPZDT, DZDD
     DATA (CCRT=7.92), (TCRT=234.0), (R=0.083145)
     DATA (81=0.49382731), (82=-1.30972686), (83=-0.38983811)
   1 S = D/DCRT $ X = T/TCRT $ X2 = X*X $ X3 = X*X2
   2 BZ = B = B1 + B2/X + B3/X3
   3 ZIPF = 1.0 + 8*S $ PZIP = D*R*T*ZIPF
   5 DPZDT = D*R*(S*T*D8ZDT + ZIPF) $ RETURN $ END
```

```
PROGRAM COMPAR(INPUT, OUTPUT, PUNCH)
       READS P,T,DENSITY,ENTHALPY,ENTROPY,SPECIFIC HEATS, CALCULATES SAME
C
C
       FROM BWR EQN AND COMPARES VALUES
C
      PROCESSES ONE POINT AT A TIME. BLANK CARD AT END OF RUN EXCEPT END
      COMMON F.Y.NFUN.RESS
      COMMON/HJM/ EPSI, CPCV, RRR, AKT
      COMMON/CRIT/ EM, EOK, RM, TC, DC, X , PC, SIG
      COMMON/14/TL, DWK, PSIG, TDWG, BHMM, TBRM, PH, PBAR, PDWG, PLOAD, TUBN
      COMMON/15/TVALVE
      COMMON/16/TBB, PBB, DPBOT, VB, DVBOT
      COMMON/17/ IPRINT
      COMMON/G/ RG
      DIMENSION ET(10).HI(4).CLK(10).ID(4).TT(10).HE(4).KD(4)
      DIMENSION F (40)
      CALL DATANES
      DTP=26.32
      P=0.00000185 $ T=66.350
      HO = ENTHAL (P,DTP,T)
    1 READ 2,P,T,RG,HG,SG,CVG,CPG
    2 FORMAT(F10.4.F10.3.F11.4.F 9.1.F10.3.F10.2.F10.2)
      IF(T.EQ.0) GO TO 4
      P=P/1.01325 $ RBWR=FINDO(P.T)
      HBHR=ENTHAL (P.RBHR.T) -HD
      SBWR=ENTROP(RBWR.T)
      CVBWR=CV(RBWR,T) $ CPBWR=CP(RBWR,T)
      DR=(RBWR-RG) *100/RG $ DH=HBWR-HG
      DS=SBWR-SG $ DCV=(CVBWR-CVG)*100/CVG $ DCP=(CPBWR-CPG)*100/CPG
      P=P*1.01325
      V=1.0/RG
C
      PRINT 6.P.T.V.HBWR.SBWR
    6 FORMAT(2F10.3, F9.1, F9.3)
      PRINT 3, P, T, V, DR, DH, DS, DCV, DCP
    3 FORMAT(2F10.1,E13.4,F8.3,F9.1,F9.3,2F8.2)
      PUNCH 7,P,T,DR,DH,DS,DCV,DCP
    7 FORMAT(2F10.1, F8.3, F9.1, F9.3, 2F8.2)
      GO TO 1
    4 CONTINUE
      CALL EXIT
      END
```

```
SUBROUTINE DATANF3
       PARAMETERS FOR NITROGEN TRIFLUORIDE
C
      DIMENSION G(32). VP(9). GI(11)
      DIMENSION GV(9), GT(9), FV(4), FT(4), EV(8), ET(8)
      COMMON/CRIT/ EM, EOK, RM, TC, DC, X , PC, SIG
      COMMON/DATA1/GV,GT,FV,FT,EV, ET
      COMMON/SEN/BETA, XO, DELTA, E1, E2, AGAM
      COMMON/DATA/G.R.GAMMA.VP.DTP
      COMMON/CPID/GI
      COMMON/ISP/N, NW, NWW
      NWW=0 $ N=0 $ NW=1
      TC=234.0 $ EM=71.019 $ DC=0.5625
      PC=44.607/1.01325 $ GAMMA=-0.0056
      T0=100.0 $ H0=3334.6 $ S0=215.69
      VP(1)=20.315417602 $ VP(2)=-8.362069370
      VP(3) = -21.398986401 \$ VP(4) = 20.162194616
      VP(5)=-6.918662727 $ VP(6)=3.677799376
      VP(7) = 1.75
      DTP=26.20
      R=0.0820568
      G(1) =
                             .1751151116E-01
      G(2) =
                            -.5338642406E+00
```

```
G(3) =
                      .3924633078E+01
                     -.5141353757E+03
G(4) =
G(5) =
                     -.3243348520E+05
G(6) =
                     -.5912181013E-03
G(7) =
                      .9096990477E+00
G(8) =
                     -.4785568295E+03
G(9) =
                     -.4180501052E+07
G(10) =
                     -.9695778991E-05
                      .5361200088E-01
G(11) =
G(12) =
                     -.1443265236E+02
G(13) =
                     -. 3322161796E-02
G(14) =
                      .2764741771E+00
G(15) =
                      .8324982578E+01
G(16) =
                     -.1307102346E-01
G(17) =
                      -1851077599E-03
G(18) =
                      .2920941516E+00
G(19) =
                     -.6918309272E-02
G(20) =
                      •4308730236E+07
G(21) =
                     -.1096864087E+08
G(22) =
                      .2380327276E+05
G(23) =
                      •3137563559E+07
G(24) =
                      .6086206849E+02
G(25) =
                      .4205136659E+02
G(26) =
                       .1076337320E+00
G(27) =
                     -. 3297262333E+02
G(28) =
                      .8485003350E-04
G(29) =
                      •1224321948E-02
                      .1269404637E-06
6(30) =
G(31) =
                     -.8824183840E-06
G(32) =
                      .3309207594E-04
DTP=26.32
RETURN & END
SUBROUTINE PROPS(PP, DD, TT)
DIMENSION X(33)
```

CALCS P. DP/DRHO. DPDT. AND NECESSARY INTEGRALS FOR H.S.G ETC C DIMENSION B(33),G(32) EQUIVALENCE (B, X) COMMON/DATA/G, R, GAMMA COMMON/1/8 DATA(ID=1) DATA(IZ=1) 1 CONTINUE IF(IZ.LE.0)GO TO 2 IZ=0 2 CONTINUE 0=00 P=PP T=TT GM=GAMMA D2=D\*D 03=02\*0 04=D3\*D 05=D4\*D D6=D5\*D D7=06\*D D8=D7\*D D9=D8\*D D10=09\*0 D11=010\*D D12=D11\*D

D13=D12\*D

```
TS=SQRT (T)
      T2=T+T
      T3=T2*T
      T4=T3+T
      T5=T4*T
      F=EXP (GM*D2)
      GO TO (100,200,300,400,500,600,700),K
      ENTRY PRESS
      ENTRY FOR PRESSURE, INPUT IS DENSITY
C
C
      AND TEMP. IN MOL/L AND K, OUTPUT IS IN ATM.
      K=1
      GO TO 1
  100 CONTINUE
      B( 1)=D2*T
      B( 2) = D2 + TS
      B(3) = D2
      B( 4)=D2/T
      B( 5) = D2/T2
      B( 6)=D3*T
      B(7) = 03
      B( 8) = D3/T
      B( 9) = D3/T2
      B(10)=D4*T
      B(11) = D4
      B(12) = D4/T
      B(13)=05
      B(14) = D6/T
      B(15) = D6/T2
      B(16) = D7/T
      B(17) = D8/T
      B(18) = D8/T2
      B(19)=D9/T2
      B(20) = D3*F/T2
      B(21) = D3 + F/T3
      B(22)=D5*F/T2
      B(23) = D5 + F/T4
      B(24) = D7#F/T2
      B(25)=D7*F/T3
      B(26)=09*F/T2
      B(27) = 09*F/T4
      B(28) = D11 + F/T2
      B(29) = D11*F/T3
      B(30) = D13*F/T2
      B(31) = D13 + F/T3
      B(32) = D13 F/T4
      IF (ID.GT.0)GO TO 102
      B(33) = P - R + D + T
      RETURN
  102 P=0
      M=32
      DO 101 I=1.M
  101 P=P+B(I)*G(I)
      P=P+R*D*T
      PP=P
      RETURN
      ENTRY DPDD
      PARTIAL OF PRESSURE WITH RESPECT TO
C
      DENSITY - SEE PRESSURE
C
      ENTRY FOR UNITS
      K=2
      GO TO 1
  200 CONTINUE
      F1=2.00*F*GM*D
       F21=3.000*F*D2 +F1*D3
      F22=5.000*F*D4 +F1*D5
      F23=7.000*F*D6 +F1*D7
```

```
F24=9.000 +F+D8 +F1+D9
    F25=11.00*F*D10+F1*D11
    F26=13.88*F*D12+F1*D13
    B( 1) = 2.00*D*T
    B( 2)=2.00*D*T$
    B(3)=2.00*D
    B(4)=2.00*D/T
    B( 5) = 2.00 * D/T2
    B(6) = 3.00 * D2 * T
    B( 7)=3.00*D2
    B(8)=3.00*D2/T
    B(9) = 3.00 + D2/T2
    B(10)=4.00*D3*T
    B(11)=4.00*D3
    B(12) = 4.00 + D3/T
    B(13)=5.00*D4
    B(14) = 6.00 + D5/T
    B(15) = 6.00 + D5/T2
    B(16) = 7.00 + D6/T
    B(17) = 8.00 + D7/T
    B(18) = 8.00 + D7/T2
    B(19) = 9.00 + D8/T2
    B(20) = F21/T2
    B(21)=F21/T3
    B(22) = F22/T2
    B(23) = F22/T4
    B(24)=F23/T2
    B(25) = F23/T3
    B(26) = F24/T2
    B(27) = F24/T4
    B(28) = F25/T2
    B(29) = F25/T3
    B(30) = F26/T2
    B(31)=F26/T3
    B(32)=F26/T4
    M = 32
    IF (ID.GT.0)GO TO 202
    B (33) = P-R+T
    RETURN
202 P=0
    DO 201 I=1, M
201 P=P+B(I)+G(I)
    P=P+R+T
    PP=P
    RETURN
    ENTRY OPDT
    PARTIAL OF PRESSURE WITH RESPECT
    TO TEMPERATURE - SEE PRESSURE
    ENTRY FOR UNITS
    K = 3
    GO TO 1
300 CONTINUE
    X(1) = D2
    X(2) = 02/(2.00 * TS)
    X(3)=0
    X(4) = -02/T2
    X(5) = -2.00 + D2/T3
    X(6) = D3
    X(7) = 0
    X(8) = -D3/T2
    X(9) = -2.00 + D3/T3
    X(10) =04
    X(11) = 0
    X(12) = -04/T2
```

C

C

```
X(26) = 2.00 + G4/T3
       X(27) = 4.00 + G4/T5
       X(28) = 2.00 + G5/T3
       X(29) = 3.00 + G5/T4
      X(30) = 2.00 + G6/T3
       X(31)=3.00 + G6/T4
       X(32) = 4.00 = G6/T5
       IF (ID.GT. 0) GO TO 402
       RETURN
  402 P=0
       DO 401 I=1,32
  401 P=P+G(I) *X(I)
       PP=P
       RETURN
       ENTRY DUDN
C
       TERMS NEEDED FOR ENTHALPY CALCULATION
       K = 5
       GO TO 1
  500 CONTINUE
       H=H0+(T*DSDN(D)-DSDN(Q))*101.325+(DUDN(D-DUDN(G))*101.325+CPOH(T)
C
C
       +(P/D-R*T)*101.325
       G1=F/(2.00*GM)
       G2=(F*D2-2.00*G1)/(2.00*GM)
       G3=(F*D4-4.00*G2)/(2.00*GM)
       G4=(F*D6-6.00*G3)/(2.00*GM)
       G5 = (F + D8 - 8 - 00 + G4) / (2 - 00 + GM)
       G6=(F*D10-10.00*G5)/(2.00*GM)
       X(1)=D+T
       X(2)=0*TS
       X(3)=0
       X ( 4) = D/T
       X(5) = D/T2
       X(6) = D2 + T/2 \cdot 00
       X(7) = D2/2 \cdot 00
       X(8) = D2/(2.06*T)
       X(9) = D2/(2.00 + T2)
       X(10) = D3 + T/3.00
       X(11) = 03/3.00
       X(12) = 03/(3.00 + T)
       X(13) = 04/4.00
       X(14) = 05/(5.00 + T)
       X(15) = 05/(5.00 + T2)
       X(16) = D6/(6.00 + T)
       X(17) = 07/(7.00 + T)
       X(18) = D7/(7.00 + T2)
       X(19) = D8/(8.00 + T2)
       X(20) = G1/T2
       X(21) = G1/T3
       X(22) = G2/T2
       X(23) = G2/T4
       X(24) = G3/T2
       X(25) = G3/T3
       X(26) = G4/T2
       X(27) = G4/T4
       X(28) = G5/T2
       X(29) = G5/T3
       X(30) = G6/T2
       X(31) = G6/T3
       X(32) = G6/T4
       IF (ID.GT.0)GO TO 502
       RETURN
  502 P=0
       DO 501 I=1.32
  501 P=P+G(I)*X(I)
```

```
Appendix D.
                                    Continued.
    PP=P
    RETURN
    ENTRY TOSOT
    TEMP. TIMES THE PARTIAL OF
    ENTROPY WITH RESPECT TO TEMP.
    K=6
    GO TO 1
600 CONTINUE
    CV=CV0+(TDSDN(/)-TDSDN(D))+101.325
    G1=F/(2.00+GM)
    G2=(F*D2-2.00*G1)/(2.00*GM)
    G3 = (F + D4 - 4 \cdot 0.0 + G2) / (2 \cdot 0.0 + GM)
    G4=(F*D6-6.00*G3)/(2.00*GM)
    G5=(F+D8-8.00+G4)/(2.00+GM)
    G6=(F*D10-10.00*G5)/(2.00*GM)
    X(1) = 0
    X(2) = -D/(4.00 + TS)
    X(3) = 0
    X(4)=2.00*D/T2
    X(5) = 6.00 + D/T3
    X(6) = 0
    X(7) = 0
    X(8) = D2/T2
    X(9) = 3.00 + D2/T3
    X(10) = 0
    X(11) = 0
    X(12) = (2.00 + D3)/(3.00 + T2)
    X(13) = 0
    X(14) = (2.00 + 05)/(5.00 + T2)
    X(15) = (6.00 + 05)/(5.00 + T3)
    X(16) = D6/(3.00 + T2)
    X(17) = (2.00 + 07)/(7.00 + T2)
    X(18) = (6.00 \pm 0.7) / (7.00 \pm 7.3)
    X(19) = (3.00 + D8)/(4.00 + T3)
    X(20) = 6.000 + G1/T3
    X(21) = 12.00 + G1/T4
    X(22) = 6.000 = G2/T3
    X(23) = 20.00 + G2/T5
    X(24) = 6.000 + G3/T3
    X(25) =12.00+G3/T4
    X(26) = 6.000 + G4/T3
    X(27) = 20.00 + G4/T5
    X(28) = 6.000 + G5/T3
    X(29) = 12.00 + G5/T4
     X(30) = 6.000 + G6/T3
    X(31)=12.00 = G6/T4
     X(32) = 20.00 + G6/T5
     IF (ID.GT.0)GO TO 602
     RETURN
602 P=0
     DO 601 I=1,32
601 P=P+G(I) *X(I)
     PP=P
     RETURN
     ENTRY DP202
     SECOND PARTIAL OF PRESSURE WITH
     RESPECT TO DENSITY SQUARED
     K = 7
     GO TO 1
700 CONTINUE
     F1=2. FF GM FD
     F12=2.*F1*GM*D+2.*F*GM
     F212=3.*F1*D2+3.*2.*D*F+F12*D3+F1*3.*D2
     F222=5.*F1*D4 +5.*4.*D3*F+5.*D4*F1+F12*D5
     F232=7.*F1*D6+7.*6.*D5*F+7.*D6*F1+F12*D7
     F242=9.*F1*D8+9.*8.*D7*F+9.*D8*F1*F12*D9
```

```
F252=11.*F1*D10+10.*11.*D9*F+11.*010*F1+F12*D11
    F262=13.*F1*D12+13.*12.*D11*F+13.*D12*F1+F12*D13
    B(1) = 2. *T $B(2) = 2. *TS $ B(3) = 2.
    B(4)=2./T $ B(5)=2./T2 $ B(6)=6.*D*T
    B(7)=6.*D $ B(8)=6.*D/T $ B(9)=6.*D/T2
    B(18)=12.*D2*T $ B(11)=12.*D2 $ B(12)=12.*D2/T
    B(13)=20.*D3 $ B(14)=30.*D4/T
                                      $ B(15)=30.*D4/T2
   B(16) = 42. *D5/T $ B(17) = 56. *D6/T $ B(18) = 56. *D6/T2
    B(19)=72.*D7/T2 $ B(20)=F212/T2 $ B(21)=F212/T3
    B(22) = F222/T2
                  $ B(24)=F232/T2 $ B(25)=F232/T3
    B(23) = F222/T4
    B(26) = F242/T2 $ B(27) = F242/T4 $ B(28) = F252/T2
    B(29) = F252/T3 $ B(30) = F262/T2 $ B(31) = F262/T3
    B(32)=F262/T4
    M=32
    IF (ID. GT. 0) GO TO 702
    B (33) = PP
    RETURN
702 P=0
    DO 701 I=1.H
701 P = P + B(I) + G(I)
    PP=P
    RETURN
    END
```

FUNCTION DPDTVP(T)

C VAPOR PRESSURE DP/DT
DIMENSION G(32),VP(9)
COMMON/DATA/G,R,GAMMA,VP
COMMON/CRIT/ EM, EOK, RM, TC, DC, X, PC, SIG
T2=T+0.001 \$ P2=VPN(T2)
T1=T-0.001 \$ P1=VPN(T1)
DPDTVP=(P2-P1)/0.002
RETURN \$ END

FUNCTION VPN(T) C VAPOR PRESSURE IN ATM DIMENSION G(32), VP(9) COMMON/DATA/G,R,GAMMA,VP COMMON/CRIT/ EM, EOK, RM, TC, DC, X , PC, SIG VP(1)=20.315417602 \$ VP(2)=-8.362069370 VP(3) = -21.398986401 \$ VP(4) = 20.162194616 VP(5)=-6.918662727 \$ VP(6)=3.677799376 VP(7)=1.75 TC=234.0 IF (T. GT. TC) 18,19 18 VPN=PC+(1.245/1.01325)\*(T-TC) PRINT 30 30 FORMAT(1H \*T GREATER THAN TC, VP EXTENSION USED\*) GO TO 17 19 CONTINUE X=T/TC P=VP(1)+VP(2)/X+VP(3)\*X+VP(4)\*X\*\*2+VP(5)\*X\*\*3+VP(6)\*X\*(1.0-X)\*\*VP 1 (7) VPN=EXP(P)/1.01325 17 CONTINUE RETURN & END

```
FUNCTION FIND D(P.T)
      DIMENSION G(32), VP(9)
      COMMON/DATA/G, R, GAMMA, VP, DTP
      COMMON/CRIT/ EM, EOK, RM, TC, DC, XX, PC, SIG
      COMMON/G/ RG
      ITTERATES EQUATION OF STATE
C
      FOR DENSITY. GIVEN PRESSURE
      AND TEMP. IN ATM. AND KELVIN.
C
                                       IF
      ITTERATION FAILS TRY USING
C
C
      FUNCTION CALLED FIND M
      TT=T
      IF(TT.GT.TC) GO TO 100
      IF( P.GT. VPN(TT)) GO TO 101
      X=P+(.8-1.)/PC+1.0
      DD=P/(R*T*X)
      GO TO 102
  100 X=(1.1/(9.*PC))*P+.7/9.
      DD=P/(R*T*X)
      IF(P/PC.GT.20..AND.T/ TC .LT.2.5)DD=DTP
      GO TO 102
  101 DD=DTP
  102 CONTINUE
      DO 10 I=1,50
      CALL PRESS(PP,DD,TT)
      P2=PP
      IF (ABS (P-P2) -1 .E-7*P) 20,20,1
    1 CALL DPDD (PP.DD.TT)
      DP=PP
      CORR=(P2-P)/DP
      0=00
      IF(ABS(CORR)-0.00005*D) 20,20,10
   10 DD=DD-CORR
      FIND D=0
      RETURN
   20 FIND D=DD
      IF(D.LT.0) 25,26
   25 DD=RG
      GO TO 102
   26 CONTINUE
      RETURN
      END
```

```
FUNCTION CV(D.T)
C
      CALCULATES SPECIFIC HEAT CAPACITY
C
      AT CONSTANT VOLUME FOR AN INPUT
C
      OF DENSITY AND TEMPERATURE IN MOL/L AND K
      DATA (R=8.31434)
      DD=D
      11=11
      CALL TOSDT(CD,DD,TT)
      DD = 0
      CALL TDSDT(CO,DD,TT)
      CV=CPI(TT)+(C0-CD)*101.325
      CV=CV-R
      RETURN
      END
```

```
FUNCTION CP(D,T)

C CALCULATES SPECIFIC HEAT CAPACITY

C AT CONSTANT PRESSURE FOR INPUT OF

C DENSITY AND TEMPERATURE IN MOL/L AND K

C CP IS IN JOULES/MOL-K
```

```
CVEE=CV(D,T)

CALL DPDT(DPT,0,T)

CALL DPDD(DPD,0,T)

CP=CVEE+(T/(D**2)*(DPT**2)/DPD)*101.325

RETURN
END
```

FUNCTION ENTHAL (P,D,T) CALCULATES ENTHALPY FOR INPUT OF C PRESSURE, DENSITY AND TEMP. IN C ATM., MOL/L AND K. OUTPUT IS IN C JOULES/HOL R=0.0820568 DD=D TT=T CALL DSDN(SD, DD, TT) CALL DUON (UD, DD, TT) 00=0 CALL DSDN(S0,DD,TT) CALL DUDN(U0,DD,TT) CALL HI (HSI, T) ENTHAL=T\*(SD-S0)\*101.325+(UD-U0)\*101.325+ HSI +(P/D-R\*T)\*101.325 RETURN END

FUNCTION ENTROP(D.T) C CALCULATES ENTROPY C FOR AN INPUT OF DENSITY AND C TEMP. IN MOL/L AND K. OUTPUT IS IN C JOULES/MOL-K R=0.0820568 00=0 TT=T CALL DSDN(SD, DD, TT) DD = 0CALL DSDN(SO, DD, TT) CALL SI(HSI.T) ENTROP=(SD-S0) +101.325-R+ALOG(D+R+T)+101.325+HSI RETURN END

FUNCTION SOUND(D,T)

C CALCULATES THE SPEED OF SOUND

C FOR AN INPUT OF DENSITY AND TEMP.

C IN MOL/L AND KELVIN. OUTPUT IS IN

C METERS/SECOND.

COMMON/CRIT/W

CALL DPDD(DP,D,T)

SOUND=((CP(D,T)/CV(D,T))\*DP\*101325./W)\*\*.5

RETURN
END

FUNCTION CPI(T)

C IDEAL GAS SPECIFIC HEAT, CP, IN J/MOL-K
DIMENSION Q(5)
DATA((Q(I), I=1,5)=6.1189724, 48.162688, 228.231405, -249.067052,

```
564.293045)
      X=T/100.
      CPI=0.0
      DO 1 I=1.5
    1 CPI=CPI+Q(I) *X**(1-I)
      CPI=(CPI*EXP(-8.76/X)+4.0)*8.31441
      RETURN
      END
      SUBROUTINE HI(HSI,T)
C
       IDEAL GAS ENTHALPY IN J/HOL AND ENTROPY IN J/HOL-K
      T0=100.0 & H0=3334.6
      DT=(T-T0)/50.0
      HSI=HO
      DO 1 I=1,50
      CP=CPI(T0+(I-0.5) *DT)
    1 HSI=HSI+CP*DT
      RETURN
      ENTRY SI
      T0=100.0
      DT = (T - T0) / 50.0
      HSI=215.69
      DO 2 I=1,50
      CP=CPI(T0+(I-0.5) *DT)
    2 HSI=HSI+CP*DT/(T0+(I-0.5)*)T)
      RETURN
      END
```

## Appendix E. Explanations for Table Headings

In many tables we have included values of parameters, constants and coefficients in the headings to ensure that correct values have been transcribed into the manuscript. These include -

Table 1, EPP, exponent in eq. (1)

TTRP, triple-point temperature, K

TCRT, critical-point temperature, K

PTRP, triple-point pressure, bar

PCRT, critical-point pressure, bar

DPSDT, vapor-pressure slope at the C.P., bar/K

list of coefficients for eq. (1)

Table 2, EL, exponent in eq. (2)

DTRP, triple-point liquid density, mol/L

DCRT, critical-point density, mol/L

list of coefficients for eq. (2)

Table 3, EG, exponent in eq. (3),

EGX, exponent for last term in eq. (3)

DGAT, triple-point vapor density, mol/L

list of coefficients for eq. (3)

Table 4, EV, highest exponent in eq. (5)

list of coefficients for eq. (5)

## Table 6

TBLP, boiling-point temperature, K

DGBP, vapor density at the B.P., mol/L

DLBP, liquid density at the B.P., mol/L

DPS/DTB, vapor-pressure slope at the B.P., bar/K

QVAPB, heat of vaporization at the B.P., kJ/mol

IX thru EP, non-linear parameters in eq. (6)

Bl thru C3, coefficients in eq. (6)

B,C are B( $\rho$ ), C( $\rho$ ) in eq. (6)

## Table 7

TC, critical temperature, K

DC, critical density, mol/L

PC, critical pressure, bar

DPS/DT, vapor pressure slope at the C.P, bar/K

DP/DT, slope of the critical isochore at the C.P., bar/K

## Table 10, NF, number of coefficients,

E, exponent in eq. (8),

OT, triple-Point heat of vaporization, kJ/mol

list of coefficients for eq. (8)

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